## **NFPA 15**

Standard for

Water Spray Fixed Systems for Fire Protection

2001 Edition

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This edition of NFPA 15, Standard for Water Spray Fixed Systems for Fire Protection, was prepared by the Technical Committee on Water Spray Fixed Systems and acted on by NFPA at its May Association Technical Meeting held May 13–17, 2001, in Anaheim, CA. It was issued by the Standards Council on July 13, 2001, with an effective date of August 2, 2001, and supersedes all previous editions.

This edition of NFPA 15 was approved as an American National Standard on August 2, 2001.

## Origin and Development of NFPA 15

The Standard for Water Spray Fixed Systems for Fire Protection, formerly Water Spray Nozzles and Extinguishing Systems, first prepared by the Committee on Manufacturing Hazards, was tentatively adopted in 1939, with final adoption in 1940. Subsequently, this standard was placed under the jurisdiction of the Committee on Special Extinguishing Systems, and a new edition was adopted in 1947. In 1959 the committee organization was further changed to place primary responsibility in the hands of the Committee on Water Spray, under the general supervision of the General Committee on Special Extinguishing Methods. In 1966 the General Committee on Special Extinguishing Methods was discontinued, and the Committee on Water Spray was constituted as an independent committee. Revised editions were presented in 1969, 1973, 1977, 1979, and 1982.

The 1985 edition incorporated several technical changes concerning special piping provisions. The format of the document was also changed to more closely follow the NFPA *Manual of Style*.

Given the limited changes in water spray technology over the past few years, it was apparent that the 1985 edition could be reconfirmed with referenced publications being updated.

The 1996 edition represented a complete reorganization of the standard. Information was rearranged in a more functional and concise format to improve the usability of the document.

Other major changes included a new chapter on high-speed systems, and revised requirements for spray nozzles, piping protection, spacing of pilot sprinklers, discharge densities, and design calculations.

The 2001 edition represents a complete reorganization of the standard to conform to the requirements of the 2000 edition of the NFPA *Manual of Style*.

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**Committee Scope:** This Committee shall have primary responsibility for documents on the design, construction, installation, and test of fixed water spray systems for fire protection purposes.

This list represents the membership at the time the Committee was balloted on the final text of this edition. Since that time, changes in the membership may have occurred. A key to classifications is found at the back of the document.

NOTE: Membership on a committee shall not in and of itself constitute an endorsement of the Association or any document developed by the committee on which the member serves.

# NFPA 15 Standard for Water Spray Fixed Systems for Fire Protection 2001 Edition

NOTICE: An asterisk (\*) following the number or letter designating a paragraph indicates that explanatory material on the paragraph can be found in Annex A.

Changes other than editorial are indicated by a vertical rule in the margin of the pages on which they appear. These lines are included as an aid to the user in identifying changes from the previous edition. Where one or more complete paragraphs have been deleted, the deletion is indicated by a bullet between the paragraphs that remain.

Information on referenced publications can be found in Chapter 2 and Annex C.

# **Chapter 1 Administration**

## 1.1 Scope.

- **1.1.1** This standard provides the minimum requirements for the design, installation, and system acceptance testing of water spray fixed systems for fire protection service and the minimum requirements for the periodic testing and maintenance of ultra high-speed water spray fixed systems.
- **1.1.2\*** Water spray fixed systems shall be specifically designed to provide for effective fire control, extinguishment, prevention, or exposure protection.
- **1.1.3\*** This standard shall not apply to water spray protection from portable nozzles, sprinkler systems, monitor nozzles, water mist suppression systems, explosion suppression, or other means of application covered by other standards of NFPA.

## 1.2 Purpose.

The purpose of this standard shall be to provide the minimum requirements for water spray fixed systems based upon sound engineering principles, test data, and field experience.

## 1.3 Application.

- **1.3.1** Water spray is applicable for protection of specific hazards and equipment and shall be permitted to be installed independently of, or supplementary to, other forms of fire protection systems or equipment.
- **1.3.2** Water spray protection is acceptable for the protection of hazards involving each of the following groups:
  - (1) Gaseous and liquid flammable materials
  - (2) Electrical hazards such as transformers, oil switches, motors, cable trays, and cable runs
  - (3) Ordinary combustibles such as paper, wood, and textiles
  - (4) Certain hazardous solids such as propellants and pyrotechnics

## 1.4 Retroactivity.

The provisions of this standard reflect a consensus of what is necessary to provide an acceptable degree of protection from the hazards addressed in this standard at the time the standard was issued. Unless otherwise specified, the provisions of this standard shall not apply to facilities, equipment, structures, or installations that existed or were approved for construction or installation prior to the effective date of the standard. Where specified, the provisions of this standard shall be retroactive. In those cases where the authority having jurisdiction determines that the existing situation presents an unacceptable degree of risk, the authority having jurisdiction shall be permitted to apply retroactively any portions of this standard deemed appropriate. The retroactive requirements of this standard shall be permitted to be modified if their application clearly would be impractical in the judgment of the authority having jurisdiction, and only where it is clearly evident that a reasonable degree of safety is provided.

## 1.5 Equivalency.

Nothing in this standard is intended to prevent the use of systems, methods, or devices of equivalent or superior quality, strength, fire resistance, effectiveness, durability, and safety over those prescribed by this standard. Technical documentation shall be submitted to the authority having jurisdiction to demonstrate equivalency. The system, method, or device shall be approved for the intended purpose by the authority having jurisdiction.

## 1.6 Units and Formulas.

**1.6.1** Metric units of measurement in this standard are in accordance with the modernized metric system known as the International System of Units (SI). Two units (liter and bar), outside of but recognized by SI, are commonly used in international fire protection. These units are listed in Table 1.6.1, with conversion factors.

Table 1.6.1 Unit Conversions

Conversions			
Name	Unit	Conve	
of	Symb	rsion	
Unit	ol	Factor	
Liter	L	1 gal =	
		3.785	
		L	
Liter	(L/min	1	
per	$)/m^{2}$	gpm/ft	
minute	,	$2 \equiv$	
per		40.746	
square		(L/min	
meter		$)/m^{2}$	
Cubic	$dm^3$	1 gal =	
decim		3.785	
eter		$dm^3$	
Pascal	Pa	1  psi =	
		6894.7	
		57 Pa	
Bar	bar	1  psi =	
		0.0689	
		bar	
Bar	bar	1 bar =	
		$10^5  \mathrm{Pa}$	

Note: For additional conversions and information see ASTM E 380, Standard Practice for Use of the International System of Units (SI).

- **1.6.2** If a value for measurement as given in this standard is followed by an equivalent value in another unit, the first stated shall be regarded as the requirement. A given equivalent value might be approximate.
- **1.6.3** The conversion procedure for the SI units has been to multiply the quantity by the conversion factor and then to round the result to the appropriate number of significant digits.

# **Chapter 2 Referenced Publications**

#### 2.1 General.

The documents or portions thereof listed in this chapter are referenced within this standard and shall be considered part of the requirements of this document.

## 2.1.1 NFPA Publications.

National Fire Protection Association, 1 Batterymarch Park, P.O. Box 9101, Quincy, MA 02269-9101.

NFPA 13, Standard for the Installation of Sprinkler Systems, 1999 edition.

NFPA 16, Standard for the Installation of Deluge Foam-Water Sprinkler and Foam-Water Spray Systems, 1999 edition.

NFPA 18, Standard on Wetting Agents, 1995 edition.

NFPA 20, Standard for the Installation of Stationary Pumps for Fire Protection, 1999 edition.

NFPA 22, Standard for Water Tanks for Private Fire Protection, 1998 edition.

NFPA 24, Standard for the Installation of Private Fire Service Mains and Their Appurtenances, 1995 edition.

NFPA 25, Standard for the Inspection, Testing, and Maintenance of Water-Based Fire Protection Systems, 1998 edition.

NFPA 51B, Standard for Fire Prevention During Welding, Cutting, and Other Hot Work, 1999 edition.

NFPA 70, National Electrical Code®, 1998 edition.

NFPA 72®, National Fire Alarm Code®, 1999 edition.

NFPA 214, Standard on Water-Cooling Towers, 2000 edition.

#### 2.1.2 Other Publications.

## 2.1.2.1 ANSI Publications.

American National Standards Institute, Inc., 11 West 42nd Street, New York, NY 10036.

ANSI/ASME B1.20.1, Pipe Threads, General Purpose, 1983.

ANSI B16.1, Cast Iron Pipe Flanges and Flanged Fittings, 1989.

ANSI B16.3, Malleable Iron Threaded Fittings, 1992.

ANSI B16.4, Gray Iron Threaded Fittings, 1992.

ANSI B16.5, Pipe Flanges and Flanged Fittings, 1988.

ANSI B16.9, Factory-Made Wrought Steel Buttwelding Fittings, 1993.

ANSI B16.11, Forged Fittings, Socket-Welding and Threaded, 1991.

ANSI B16.18, Cast Copper Alloy Solder Joint Pressure Fittings, 1984.

ANSI B16.22, Wrought Copper and Copper Alloy Solder Joint Pressure Fittings, 1989.

ANSI B16.25, Buttwelding Ends, 1992.

ANSI B36.10M, Welded and Seamless Wrought Steel Pipe, 1985.

ANSI B36.19M, Stainless Steel Pipe, 1985.

ANSI C2, National Electrical Safety Code, 1993.

## 2.1.2.2 ASTM Publications.

American Society for Testing and Materials, 100 Barr Harbor Drive, West Conshohocken, PA 19428-2959.

ASTM A 53, Standard Specification for Pipe, Steel, Black and Hot-Dipped, Zinc-Coated, Welded and Seamless, 1995.

ASTM A 135, Standard Specification for Electric-Resistance-Welded Steel Pipe, 1993.

ASTM A 182, Standard Specification for Forged or Rolled Alloy-Steel Pipe Flanges,

Forged Fittings, and Valves and Parts for High-Temperature Service, 1995.

ASTM A 234, Standard Specification for Piping Fittings of Wrought Carbon Steel and Alloy Steel for Moderate and Elevated Temperatures, 1995.

ASTM A 312, Standard Specification for Seamless and Welded Austenitic Stainless Steel Pipes, 1994.

ASTM A 536, Standard Specification for Ductile Iron Castings, 1984.

ASTM A 795, Standard Specification for Black and Hot-Dipped Zinc-Coated (Galvanized) Welded and Seamless Steel Pipe for Fire Protection Use, 1995.

ASTM B 75, Standard Specification for Seamless Copper Tube, 1995.

ASTM B 88, Standard Specification for Seamless Copper Water Tube, 1995.

ASTM B 251, Standard Specification for General Requirements for Wrought Seamless Copper and Copper-Alloy Tube, 1993.

ASTM D 2996, Standard Specification for Filament-Wound "Fiberglass" (Glass-Fiber-Reinforced Thermosetting-Resin) Pipe, 2000.

ASTM E 380, Standard Practice for Use of the International System of Units (SI), 1992.

ASTM F 1173, Standard Specification for Thermosetting Resin "Fiberglass" Pipe and Fittings to be Used for Marine Applications, 1995.

## 2.1.2.3 AWS Publications.

American Welding Society, 550 N. W. LeJeune Road, Miami, FL 33126.

AWS A5.8, Specification for Filler Metals for Brazing and Braze Welding, 1992.

AWS B2.1, Specification for Qualification for Welding Procedures and Welders for Piping and Tubing, 1998.

# **Chapter 3 Definitions**

#### 3.1 General.

The definitions contained in this chapter shall apply to the terms used in this standard. Where terms are not included, common usage of the terms shall apply.

#### 3.2 NFPA Official Definitions.

- **3.2.1\* Approved.** Acceptable to the authority having jurisdiction.
- **3.2.2\* Authority Having Jurisdiction.** The organization, office, or individual responsible for approving equipment, materials, an installation, or a procedure.
- **3.2.3\* Listed.** Equipment, materials, or services included in a list published by an organization that is acceptable to the authority having jurisdiction and concerned with evaluation of products or services, that maintains periodic inspection of production of listed equipment or materials or periodic evaluation of services, and whose listing states that either the equipment, material, or service meets appropriate designated standards or has been tested and found suitable for a specified purpose.
- **3.2.4 Shall.** Indicates a mandatory requirement.
- **3.2.5** Should. Indicates a recommendation or that which is advised but not required.

#### 3.3 General Definitions.

- **3.3.1 Automatic Detection Equipment.** Equipment that will automatically detect heat, flame, smoke, flammable gases, or other conditions likely to produce fire or explosion and cause automatic actuation of alarm and protection equipment.
- **3.3.2 Flammable Gas Detection Equipment.** Equipment that will automatically detect a percent volume concentration of a flammable gas or vapor relative to a predetermined level.
- **3.3.3 Combined System.** A system of piping that connects both sprinklers and water spray nozzles in a common fire area, and is supplied by a single riser and system actuation valve.
- **3.3.4 Control of Burning.** Application of water spray to equipment or areas where a fire can occur to control the rate of burning and thereby limit the heat release from a fire until the fuel can be eliminated or extinguishment effected.
- **3.3.5 Deflagration.** Propagation of a combustion zone at a velocity that is less than the speed of sound in the unreacted medium.
- **3.3.6 Density.** The unit rate of water application to an area or surface expressed in gpm/ft<sup>2</sup> [(L/min)/m<sup>2</sup>].
- **3.3.7 Detonation.** Propagation of a combustion zone at a velocity that is greater than the speed of sound in the unreacted medium.
- **3.3.8 Electrical Clearance.** The air distance between the water spray equipment, including

piping and nozzles, and unenclosed or uninsulated live electrical components at other than ground potential.

- **3.3.9 Exposure Protection.** Absorption of heat through application of water spray to structures or equipment exposed to a fire, to limit surface temperature to a level that will minimize damage and prevent failure.
- **3.3.10\* Fire Area.** An area that is physically separated from other areas by space, barriers, walls, or other means in order to contain fire within that area.
- **3.3.11 Flammable and Combustible Liquids.** Flammable liquids shall be or shall include any liquids having a flash point below 100°F (37.8°C) and having a vapor pressure not exceeding 40 psi (276 kPa) (absolute) at 100°F (37.8°C). Flammable liquids shall be subdivided as follows: Class I liquids shall include those having flash points below 100°F (37.8°C) and shall be subdivided as follows: (1) Class IA liquids shall include those having flash points below 73°F (22.8°C) and having a boiling point below 100°F (37.8°C); (2) Class IB liquids shall include those having flash points at or above 100°F (37.8°C); (3) Class IC liquids shall include those having flash points at or above 73°F (22.8°C) and below 100°F (37.8°C). Combustible liquids shall be or shall include any liquids having a flash point at or above 100°F (37.8°C). They shall be subdivided as follows: (1) Class II liquids shall include those having flash points at or above 100°F (37.8°C) and below 140°F (60°C); (2) Class IIIA liquids shall include those having flash points at or above 140°F (60°C) and below 200°F (93.3°C); (3) Class IIIB liquids shall include those having flash points at or above 140°F (60°C) and below 200°F (93.3°C).
- **3.3.12 Impingement.** The striking of a protected surface by water droplets issuing directly from a water spray nozzle.

## 3.3.13 Insulation.

- **3.3.13.1\* Insulated.** Refers to equipment, structures, or vessels provided with an encapsulating material that, for the expected duration of fire exposure, will limit steel temperatures to a maximum of 850°F (454°C) for structural members or 650°F (343°C) for vessels. The insulation system shall be: (1) Noncombustible and fire retardant; (2) Mildew and weather resistant; (3) Resistant to the force of hose streams; and (4) Secured by fire and corrosion-resistant fastenings.
- **3.3.13.2 Uninsulated.** Refers to equipment, structures, or vessels not provided with an encapsulating material that meets the requirements defined as "insulated."
- **3.3.14 Net Rate.** The total rate of water discharge density, less water wastage due to factors such as wind effects and inaccuracies in nozzle angles of spray.
- **3.3.15\* Nonabsorbing Ground.** Earth or fill that is not readily permeable or absorbent to large quantities of flammable or combustible liquid or water, or both.
- **3.3.16 Pilot Sprinkler.** An automatic sprinkler or thermostatic fixed temperature release device used as a detector to pneumatically or hydraulically release the system actuation valve.
- **3.3.17 Rundown.** The downward travel of water along a surface, caused by the momentum of the water or by gravity.
- 3.3.18 Ultra High-Speed Water Spray System. A type of automatic water spray system

where water spray is rapidly applied to protect specific hazards where deflagrations are anticipated.

- **3.3.18.1 Ultra High-Speed Water Spray System Area Application.** The application of ultra high-speed water spray over a specific floor area or over the surface area of a specific object.
- **3.3.18.2 Ultra High-Speed Water Spray System** Local Application. The application of ultra high-speed water spray on a specific point or points of ignition, such as cutting, mixing or grinding operations.

#### 3.3.19 Valve.

- **3.3.19.1 Deluge Valve.** A type of system actuation valve that is opened by the operation of a detection system installed in the same areas as the spray nozzles or by remote manual operation supplying water to all spray nozzles.
- **3.3.19.2 System Actuation Valve.** The main valve that controls the flow of water into the water spray system.
- **3.3.20 Water Spray.** Water in a form having a predetermined pattern, particle size, velocity, and density discharge from specially designed nozzles or devices.
- 3.3.21 Water Spray Nozzle.
- **3.3.21.1 Automatic Water Spray Nozzle.** A nozzle intended to open automatically by operation of a heat responsive element that maintains the discharge orifice closed by means such as the exertion of force on a cap (button or disc), that when discharging water under pressure, will distribute the water in a specific, directional pattern.
- **3.3.21.2\* Open Water Spray Nozzle.** An open water discharge device that, when discharging water under pressure, will distribute the water in a specific, directional pattern. **3.3.22\* Water Spray System.** An automatic or manually actuated fixed pipe system connected to a water supply and equipped with water spray nozzles designed to provide a
- specific water discharge and distribution over the protected surfaces or area.

  3.3.23\* Water Wastage. That discharge from water spray nozzles that does not impinge on the surface being protected.

# **Chapter 4 General Requirements**

## 4.1\* Design Objectives.

In general, water spray shall be considered effective for any one of or a combination of the following objectives (see Chapter 7):

- (1) Extinguishment of fire
- (2) Control of burning
- (3) Exposure protection
- (4) Prevention of fire

## 4.2 Special Considerations.

**4.2.1** A study shall be made of the physical and chemical properties of the materials for which the water spray protection is being considered to determine the advisability of its

use.

- **4.2.2** The flash point, specific gravity, viscosity, miscibility, and solubility and permeability of the material, temperature of the water spray, and the normal temperature of the hazard to be protected are among the factors that shall be given consideration.
- **4.2.3**\* Where water spray can encounter confined materials at a high temperature or with a wide distillation range, the slopover or frothing hazard shall be evaluated.

## 4.2.4 Water Soluble Materials.

- **4.2.4.1** Where protecting water soluble materials, such as alcohol, systems shall be permitted to be designed for extinguishment by control, extinguishment by dilution, or extinguishment by an adequate application rate and coverage.
- **4.2.4.2** Each water soluble material shall be tested under the conditions of use to determine the applicability of a water spray system, unless design supportive data is available.
- **4.2.5\*** Water spray shall not be used for direct application to materials that react with water, such as metallic sodium or calcium carbide, which produce violent reactions or increase hazardous products as a result of heated vapor emission.
- **4.2.6** Water spray shall not be used for applications involving liquefied gases at cryogenic temperatures (such as liquefied natural gas), which boil violently when heated by water.
- **4.2.7** An evaluation shall be conducted, given the possibility of damage, distortion, or failure of equipment operating at high temperatures due to water spray application.

## 4.3\* Workmanship.

Water spray system design, layout, and installation shall be entrusted to fully experienced and responsible parties only.

## 4.4 Control of Runoff.

- **4.4.1\*** Water discharge from water spray systems shall be controlled or contained to prevent the spread of fire where flammable or combustible liquids are present.
- **4.4.2** Where flammable or combustible liquids are not present and the potential for water damage to adjacent areas is minimal, water discharged from water spray systems shall not be required to be controlled or contained.
- **4.4.3**\* The control or containment system shall utilize any one of the following:
  - (1) Curbing and grading
  - (2) Underground or enclosed drains
  - (3) Open trenches or ditches
  - (4) Diking or impoundment
  - (5) Any combination of 4.4.3(1) through (4)
- **4.4.4\*** Where the protected hazard involves the possible release of flammable or combustible liquids, the drainage system shall be designed to safely handle burning liquids.
- **4.4.5** Enclosed drain systems shall be fitted with traps or other means to prevent the entrance of flames or burning liquids into the system.
- **4.4.6** Open trenches and ditches shall be routed so as not to expose fire fighters, critical equipment and piping, other important structures, or property of others.
- **4.4.7** The control or containment system shall be designed to accommodate the total combined flow from all of the following:
  - (1)\* All water spray systems intended to operate simultaneously within the fire area (where the actual discharge will exceed the design flow rate, the actual flow rate shall be used).

- (2) Supplemental hose streams and monitor nozzle devices likely to be used during the fire.
- (3) The largest anticipated spill or accidental release of process liquids where applicable.
- (4) Any normal discharge of process liquids or cooling water into the drainage system.
- (5)\* Rain water, provided local conditions warrant inclusion.
- **4.4.8\*** The control or containment system shall be designed to accommodate the total combined flow for the fire's expected duration.
- **4.4.9** Where approved, the system shall be permitted to be designed to accommodate the total combined flow for a period less than the fire's expected duration.
- **4.4.10** The water and liquids drained from protected areas shall be collected and treated as required by local regulations.
- **4.4.11** Hazardous chemicals and contaminated water shall not be discharged to open waterways or onto the property of others.

# **Chapter 5 System Components**

#### 5.1 General.

**5.1.1** All component parts shall be coordinated to provide complete systems.

#### 5.1.2 Materials.

- **5.1.2.1** Only listed materials and devices shall be used in the installation of water spray systems.
- **5.1.2.2** Components that do not affect system operation, such as drain valves and signs, shall not be required to be listed.
- **5.1.2.3** Only new materials and devices shall be employed in the installation of new water spray systems.
- **5.1.2.4** The use of reconditioned valves and devices, other than automatic water spray nozzles, as replacement equipment in existing systems shall be permitted.
- **5.1.3** System components shall be rated for the maximum working pressure to which they are exposed, but not less than 12.1 bar (175 psi).
- **5.1.4 Corrosion Protection.** System components installed outside, or in the presence of a corrosive atmosphere, shall be constructed of materials that will resist corrosion or be suitably protected from corrosion.

## 5.2 Water Spray Nozzles.

Water spray nozzles shall be of a type listed for use in water spray systems with the following discharge characteristics:

- (1) K factor
- (2) Spray patterns at various pressures, distances, and orientation angles

- (3) Uniformity of water distribution over its spray pattern
- **5.2.1** Water spray nozzles shall be permanently marked with their characteristics according to their listing.
- **5.2.2** Standard temperature ratings and color code designations of automatic water spray nozzles shall be as required for automatic sprinklers in NFPA 13, *Standard for the Installation of Sprinkler Systems*.

## 5.2.3 Special Coatings.

**5.2.3.1** Listed corrosion-resistant spray nozzles shall be installed in locations where chemicals, moisture, or other corrosive vapors sufficient to cause corrosion of such devices exist.

## **5.2.3.2** Corrosion-Resistant Coatings.

- **5.2.3.2.1** Corrosion-resistant coatings shall be applied by the manufacturer of the spray nozzle.
- **5.2.3.2.2** Any damage to the protective coating occurring at the time of installation shall be repaired immediately, using only the coating of the manufacturer of the spray nozzle in the approved manner so that no part of the spray nozzle will be exposed after installation.
- **5.2.3.3\* Painting.**
- **5.2.3.3.1** Unless applied by the manufacturer, spray nozzles shall not be painted.
- **5.2.3.3.2** Any spray nozzles that have been painted by other than the manufacturer or after installation shall be replaced with spray nozzles of the same characteristics, including K factor, thermal response (automatic nozzles), and water distribution.
- **5.2.4 Guards.** Automatic water spray nozzles subject to mechanical damage shall be protected with listed guards.

## 5.2.5\* Stock of Spare Automatic Water Spray Nozzles and Pilot Sprinklers.

- **5.2.5.1** A supply of automatic water spray nozzles and pilot sprinklers shall be maintained on the premises so that any automatic water spray nozzles or pilot sprinklers that have operated or been damaged in any way can be promptly replaced.
- **5.2.5.2** These automatic water spray nozzles and pilot sprinklers shall correspond to the types and temperature ratings of the automatic water spray nozzles and pilot sprinklers on the property.
- **5.2.5.3** The automatic water spray nozzles and pilot sprinklers shall be kept in a cabinet where the ambient storage temperature does not exceed 38°C (100°F).
- **5.2.5.4** Where required by the manufacturer, a special automatic water spray nozzle and/or pilot sprinkler wrench shall be provided to be used in the removal and installation of automatic water spray nozzles and pilot sprinklers.
- **5.2.5.5** The stock of spare automatic water spray nozzles and pilot sprinklers shall include as a minimum 1 of each type of automatic water spray nozzle and pilot sprinkler present on the property and shall in no case be less than the following total quantities based on the total number of automatic water spray nozzles and pilot sprinklers on the property:
  - (1) For properties with less than 300 automatic water spray nozzles or pilot sprinklers, not less than 6 automatic water spray nozzles or pilot sprinklers
  - (2) For properties with 300 to 1000 automatic water spray nozzles or pilot sprinklers, not less than 12 automatic water spray nozzles or pilot sprinklers
  - (3) For properties with over 1000 automatic water spray nozzles or pilot sprinklers,

## 5.3 Pipe and Tube.

**5.3.1** Pipe or tube used in water spray systems shall meet or exceed one of the standards in Table 5.3.1 or be in accordance with 5.3.4. In addition, steel pipe shall be in accordance with 5.3.2 and 5.3.3, and copper tube shall be in accordance with 5.3.4.

<b>Table 5.3.1</b>
Pipe or
Tube
<b>Specificatio</b>

Specificatio				
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Mater	Stand			
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and				
Dimen				
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Ferro				
us				
Piping				
(Weld				
ed and				
Seaml				
ess) Stainle	ANSI			
Stanne	B36.1			
Steel	9M			
Pipe	)1VI			
Standa	ASTM			
rd	A 312			
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Seaml				
ess				
and				
Welde				
d				
Austen				
itic				
Stainle				
SS Cu 1				
Steel				
Pipes				

Standa ASTM rd A 795

Specifi

cation

for

Black

and Hot-

Dippe

d

Zinc-

Coated

(Galva

nized)

Welde d and

Seaml

ess

Steel

Pipe

for Fire

Protect

ion

Use<sup>†</sup>

Standa ASTM rd A 53

Specifi

cation

for

Pipe, Steel,

Black

and

Hot-

Dippe

d,

Zinc-Coated

Welde

d and

Seaml

ess†

Welde ANSI B36.1 d and Seaml 0M

ess

Wroug

ht

Steel

Pipe

Standa ASTM rd A 135

Specifi cation

for

Electri

c-

Resist

ance-

Welde d Steel

Pipe

Coppe

Tube

(Draw

n,

Seaml

ess)

Standa ASTM B 75 rd

Specifi cation

for

Seaml

ess

Coppe

Tube<sup>†</sup>

Standa ASTM rd B 88

Specifi

cation

for

Seaml

ess

Coppe

Water

Tube<sup>†</sup>

```
Standa ASTM
        B 251
rd
Specifi
cation
for
Gener
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ements
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r and
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Tube
Specifi AWS
cation A5.8
for
Filler
Metals
for
Brazin
g and
Braze
Weldi
(Classi
ficatio
BCuP-
3 or
BCuP-
4)
   †Denote
   s pipe or
    tubing
   suitable
      for
   bending
   accordin
     g to
    ASTM
   standard
      S.
```

**5.3.2\*** Where steel pipe listed in Table 5.3.1 is used and joined by welding or by roll grooved pipe and fittings, the minimum nominal wall thickness for pressures up to 20.7 bar (300 psi) shall be in accordance with Schedule 10 for pipe sizes up to 127 mm (5 in.); 3.40 mm (0.134 in.) for 152-mm (6-in.) pipe; and 4.78 mm (0.188 in.) for 203-mm and 254-mm

(8-in. and 10-in.) pipe.

- **5.3.2.1** Pressure limitations and wall thickness for steel pipe listed in accordance with 5.3.5 shall be in accordance with the listing requirements.
- **5.3.3** When steel pipe listed in Table 5.3.1 is joined by threaded fittings or by fittings used with pipe having cut grooves, the minimum wall thickness shall be in accordance with Schedule 30 [in pipe sizes 203 mm (8 in.) and larger] or Schedule 40 [in pipe sizes less than 203 mm (8 in.)] for pressures up to 20.7 bar (300 psi).
- **5.3.4** Copper tube shall be permitted in water-filled water spray systems where system pressures do not exceed 12.1 bar (175 psi). Copper tube specified in the standards listed in Table 5.3.1 shall have wall thicknesses of Type K, L, or M.
- **5.3.5\*** Other types of pipe or tube investigated for suitability in automatic water spray installations and listed for this service, including but not limited to steel differing from that provided in Table 5.3.1, shall be permitted where installed in accordance with their listing limitations, including installation instructions. Bending of pipe shall be permitted as allowed by the listing.

## 5.3.6 Steel Piping.

- **5.3.6.1** Steel pipe used in manual and open systems shall be galvanized on its internal and external surfaces in accordance with Table 5.3.1.
- **5.3.6.2** The threaded ends of galvanized pipe shall be protected against corrosion.
- **5.3.6.3** Water-filled steel piping shall be permitted to be black steel.
- **5.3.6.4** Stainless steel pipe shall not be required to be galvanized.
- **5.3.7 Corrosion Protection.** Where no other piping material will provide the required corrosion resistance for a particular corrosive application, listed coated pipe or an approved corrosion resistance system applied to piping shall be permitted.
- **5.3.8 Minimum Pipe Size.** The minimum pipe size shall be 25 mm (1 in.) for steel and galvanized steel, and in. 19 mm ( $\frac{3}{4}$  in.) for copper and stainless steel.

## 5.3.9 Pipe Bending.

- **5.3.9.1** Bending of steel piping of wall thickness equal to or greater than Schedule 10 and Types K and L copper tube shall be permitted where bends are made with no kinks, ripples, distortions, reductions in internal diameter, or any noticeable deviations from round.
- **5.3.9.2** For Schedule 40 steel piping and Types K and L copper tubing, the minimum radius of bend shall be 6 pipe diameters for pipe sizes 51 mm (2 in.) and smaller, and 5 pipe diameters for pipe sizes 64 mm (2½ in.) and larger.
- **5.3.9.3** For all other types of steel pipe, the minimum radius of bend shall be 12 pipe diameters for all pipe sizes.

## 5.3.10 Pipe Identification.

- **5.3.10.1** All pipe, including specially listed pipe allowed by 5.3.5, shall be marked continuously along its length by the manufacturer in such a way as to properly identify the type of pipe.
- **5.3.10.2** This identification shall include the manufacturer's name, model designation, or schedule.

## 5.4 Fittings.

**5.4.1** Fittings used in water systems shall meet or exceed the standards in Table 5.4.1.

Table 5.4.1
Fittings Materials and Dimensions

and	Dimensions
Mater	Stand
ials	ard
and	
Dimen	
sions	
Cast	
Iron	
Gray	ANSI
Iron	B16.4
	D10.4
Thread	
ed	
Fitting	
S,	
Class	
125	
and	
250	
Cast	ANSI
Iron	B16.1
Pipe	
Flange	
s and	
Flange	
d	
Fitting	
s	
Malle	
able	
Iron	
Mallea	ANSI
ble	B16.3
Iron	
Thread	
ed	
Fitting	
S,	
Class	
150	
and	
300	
Steel	
Factor	ANICI
	ANSI B16.9
y-	В10.9
Made	
Wroug	
ht	
Steel	
Buttw	
elding	
Fitting	
S	_

Buttw elding Ends Standa rd Specification for Piping Fitting s of Wroug ht Carbo n Steel and Alloy		ANSI B16.2 5 ASTM A 234
Steel for Moder ate and Elevat ed		
Tempe ratures Pipe Flange s and Flange d		ANSI B16.5
Fitting s Forged Fitting s, Socket		ANSI B16.1
Weldi ng and Thread ed Coppe		
r Wroug ht Coppe r and Coppe r Alloy Solder Joint		ANSI B16.2 2
Pressu re Fitting s	_	_

Cast **ANSI** B16.1 Coppe r Alloy 8 Solder Joint Pressu re Fitting S **Ductil** e Iron **ASTM** Standa A 536 rd Specifi cation for Ductil e Iron Castin gs Stainl ess Steel Standa **ASTM** A 182 rd Specifi cation for Forged or Rolled Alloy-Steel Pipe Flange Forged Fitting s, and Valves and Parts for High-Tempe rature Servic e

**5.4.2** In dry sections of the piping exposed to possible fire or in self-supporting systems, ferrous fittings shall be of steel, malleable iron, or ductile iron.

**5.4.3** Galvanized fittings shall be used where galvanized pipe is used.

**5.4.4** Other types of fittings investigated for suitability in water spray system installations and listed for this service, including but not limited to fiberglass and steel differing from

that provided in Table 5.4.1, shall be permitted when installed in accordance with their listing limitations, including installation instructions.

- **5.4.5** Fittings shall be extra heavy pattern where pressures exceed 12 bar (175 psi).
- **5.4.6** Standard weight pattern malleable iron fittings 152 mm (6 in.) in size or smaller shall be permitted where pressures do not exceed 20.7 bar (300 psi).
- **5.4.7** Listed fittings shall be permitted for system pressures up to the limits specified in their listings.
- 5.4.8 Couplings and Unions.
- **5.4.8.1** Screwed unions shall not be used on pipe larger than 51 mm (2 in.).
- **5.4.8.2** Couplings and unions of other than screwed type shall be of types listed specifically for use in water spray or sprinkler systems.

## 5.4.9 Reducers and Bushings.

- **5.4.9.1** A one-piece reducing fitting shall be used wherever a change is made in the size of pipe.
- **5.4.9.2** Hexagonal or face bushings shall be permitted for use in reducing the size of openings of fittings where standard fittings of the required size and material are not available from the manufacturer.
- **5.4.10\*** Rubber-gasketed fittings shall be permitted to be used to connect pipe in fire exposed areas where the water spray system is automatically controlled.
- **5.4.11** Fire exposed areas where rubber-gasketed fittings are located shall be protected by automatic water spray systems or other approved means.

## 5.5 Joining of Pipe and Fittings.

## 5.5.1 Threaded Pipe and Fittings.

- **5.5.1.1** All threaded pipe and fittings shall have threads cut in accordance with ANSI/ASME B1.20.1, *Pipe Threads, General Purpose*.
- **5.5.1.2\*** Steel pipe with wall thicknesses less than Schedule 30 [in pipe sizes 203 mm (8 in.) and larger] or Schedule 40 [in pipe sizes less than 203 mm (8 in.)] shall not be joined by threaded fittings.
- **5.5.1.3** Where wall thicknesses are less than those required in 5.5.1.2, pipes shall be permitted to be threaded where the threaded assembly is investigated and listed for this service.
- **5.5.1.4** Joint compound or tape shall be applied only to male threads.

## 5.5.2\* Welded Pipe and Fittings.

- **5.5.2.1** Field welding shall be permitted.
- **5.5.2.2** Safe welding and cutting practices shall be followed in accordance with NFPA
- 51B, Standard for Fire Prevention During Welding, Cutting, and Other Hot Work.
- **5.5.2.2.1** Where outlets are welded to pipe using listed welding outlet fittings, partial joint penetration (groove/fillet) welds are acceptable when performed in accordance with the standard. Where slip-on flanges are welded to pipe, fillet welds are acceptable where such welds are used along both circumferences where the flange contacts the pipe.
- **5.5.2.3** Welding methods shall meet or exceed the requirements of AWS B2.1,
- Specification for Qualification for Welding Procedures and Welders for Piping and Tubing.

- **5.5.2.4** Fittings used to join pipe shall be listed fabricated fittings or manufactured in accordance with Table 5.4.1.
- **5.5.2.5** Manufactured fittings joined in conformance with a qualified welding procedure as set forth in this section shall be permitted to be an acceptable product under this standard, provided that materials and wall thickness are compatible with other sections of this standard.
- **5.5.2.6** Fittings shall not be required where pipe ends are butt-welded with full root penetration welds.
- **5.5.2.7** No welding shall be performed if there is impingement of rain, snow, sleet, or high wind on the weld area of the pipe product.
- **5.5.2.8** Welding shall be performed in accordance with the following:
  - (1)\* Holes cut in piping for outlets shall be cut to the full inside diameter of fittings prior to welding in place of the fittings.
  - (2) Discs shall be retrieved.
  - (3) Openings cut into piping shall be smooth bore, and all internal slag and welding residue shall be removed.
  - (4) Fittings shall not penetrate the internal diameter of the piping.
  - (5) Steel plates shall not be welded to the ends of piping or fittings.
  - (6) Fittings shall not be modified.
  - (7) Nuts, clips, eye rods, angle brackets, or other fasteners shall not be welded to pipe or fittings.
- **5.5.2.9** Where longitudinal earthquake braces are provided, tabs welded to pipe for longitudinal earthquake braces shall be permitted.
- **5.5.2.10** When reducing the pipe size in a run of piping, a reducing fitting designed for that purpose shall be used.
- **5.5.2.11** Where welded piping is to be galvanized, pipe shall be fabricated into spooled sections and shall be galvanized after fabrication.
- **5.5.2.12** Torch cutting and welding shall not be permitted as a means of modifying or repairing water spray systems.

## 5.5.2.13 Qualifications.

- **5.5.2.13.1** Successful procedure qualification of complete joint penetration groove welds shall qualify partial joint penetration (groove/fillet) welds and fillet welds in accordance with the provisions of the standard.
- **5.5.2.13.1.1** Welding procedures qualified under standards recognized by previous editions of this standard shall be permitted to be continued in use.
- **5.5.2.13.2** Qualification of the welding procedure to be used and the performance of all welders and welding operators shall be required and shall meet or exceed the requirements of American Welding Society Standard AWS B2.1, *Specification for Qualification for Welding Procedures and Welders for Piping and Tubing.*
- **5.5.2.13.3** Contractors or fabricators shall be responsible for all welding they produce.

**5.5.2.13.4** Each contractor or fabricator shall have available to the authority having jurisdiction an established written quality assurance procedure ensuring compliance with the requirements of 5.5.2.5.

## 5.5.2.14 Records.

- **5.5.2.14.1** Contractors or fabricators shall maintain certified records of the welding procedures used and the welders or welding machine operators employed by them.
- **5.5.2.14.2** Records shall show the date and the results of procedure and performance qualifications and shall be available to the authority having jurisdiction.

## **5.5.3** Groove Joining Methods.

- **5.5.3.1** Pipe joined with grooved fittings shall be joined by a listed combination of fittings, gaskets, and grooves.
- **5.5.3.2** Grooves cut or rolled on pipe shall be dimensionally compatible with the fittings.
- **5.5.4\*** Joints for the connection of copper tube shall be brazed using the brazing material in Table 5.3.1.
- **5.5.5 Other Types.** Other joining methods investigated for suitability in water spray sprinkler installations and listed for this service shall be permitted where installed in accordance with their listing limitations, including installation instructions.
- **5.5.6** End Treatment. Pipe ends shall have burrs and fins removed after cutting.
- **5.5.6.1** Pipe used with listed fittings and its end treatment shall be in accordance with the fitting manufacturer's installation instructions and the fitting's listing.

## 5.6 Hangers.

- **5.6.1 General.** The types of hangers used shall be in accordance with the requirements of NFPA 13, *Standard for the Installation of Sprinkler Systems*.
- **5.6.2** Hangers used outdoors or in locations where corrosive conditions exist shall be galvanized, suitably coated, or fabricated from corrosion-resistive materials.

#### 5.7 Valves.

#### 5.7.1 Control Valves.

- **5.7.1.1** All valves controlling connections to water supplies and to supply pipes to water spray nozzles shall be listed indicating valves.
- **5.7.1.2** Listed underground gate valves equipped with listed indicator posts shall be permitted in underground applications.
- **5.7.1.3** Where approved, replacement or installation of a nonindicating valve, such as a T-wrench-operated roadway box, shall be permitted to be installed.
- **5.7.1.4** Control valves shall not close in less than 5 seconds when operated at maximum possible speed from the fully open position.
- **5.7.1.5** Wafer-type valves with components that extend beyond the valve body shall be installed in a manner that does not interfere with the operation of any system components.

## **5.7.2 System Actuation Valves.**

- **5.7.2.1\*** System actuation valves shall be listed.
- **5.7.2.2\*** Accessories used to operate the actuation valve shall be listed and compatible.
- **5.7.2.3\*** System actuation valves shall be provided with manual means of actuation independent of the automatic release system and detection devices.
- **5.7.2.4** Alarm check valves shall not require an independent means of activation.
- **5.7.2.5** Manual controls of actuation valves shall not require a pull of more than 178 N (40 lbf) or a movement of more than 356 mm (14 in.) to secure operation.
- 5.7.3 Drain Valves and Test Valves. Drain valves and test valves shall be approved.

## 5.7.4 Identification of Valves.

- **5.7.4.1** All control, drain, and test connection valves shall be provided with permanently marked weatherproof metal or rigid plastic identification signs.
- **5.7.4.2** The identification sign shall be secured with corrosion-resistant wire, chain, or other approved means.

## 5.8 Pressure Gauges.

Required pressure gauges shall be listed and shall have a maximum limit not less than twice the normal working pressure where installed.

#### 5.9 Strainers.

- **5.9.1\*** Pipeline strainers shall be specifically listed for use in water supply connections.
- **5.9.2** Strainers shall be capable of removing from the water all solids of sufficient size to obstruct the spray nozzles [normally 3.2-mm ( $^{1/8}$ -in.) perforations are suitable].
- **5.9.3** Pipeline strainer designs shall incorporate a flushing connection.
- **5.9.4** Individual or integral strainers for spray nozzles, where required, shall be capable of removing from the water all solids of sufficient size to obstruct the spray nozzle they serve.

## 5.10 Fire Department Connections.

- **5.10.1** Fire department connections shall be listed and shall have internal threaded swivel fittings having threads compatible with those of the local fire department.
- **5.10.2** Connections shall be equipped with listed plugs or caps.

## 5.11 Alarms.

- **5.11.1** Waterflow alarm apparatus shall be listed for this service.
- **5.11.2** An alarm unit shall include a listed mechanical alarm or horn or a listed electric device, bell, speaker, horn, or siren.
- **5.11.3\*** Outdoor water-motor-operated or electrically operated bells shall be protected from the weather and shall be provided with guards.
- **5.11.4** Piping to the water-motor-operated devices shall have corrosion resistance equal to or better than galvanized ferrous pipe and fittings and shall be of a size not less than 19 mm

 $(\frac{3}{4} \text{ in.}).$ 

- **5.11.5** Drains from alarm devices shall be sized and arranged to prevent water overflow at the drain connection when system drains are open wide and under system pressure.
- **5.11.6** Electrical alarm devices used outdoors shall be listed for this purpose.
- **5.11.7** Electrical fittings and devices listed for use in hazardous locations shall be used where required by NFPA 70, *National Electrical Code*<sup>®</sup>.

## **5.12 Detection Systems.**

- **5.12.1** Automatic detection equipment, release devices, and system accessories shall be listed for the intended use.
- **5.12.2** The detection systems shall be automatically supervised in accordance with NFPA 72<sup>®</sup>, *National Fire Alarm Code*<sup>®</sup>.

# **Chapter 6 Installation Requirements**

## 6.1 Basic Requirements.

**6.1.1 Hazardous Locations.** Components of the electrical portions of water spray systems that are installed in classified locations as defined in Article 500 of NFPA 70, *National Electrical Code*, shall be listed for such use.

## 6.1.2\* Electrical Clearances.

- **6.1.2.1** All system components shall be located so as to maintain minimum electrical clearances from live parts.
- **6.1.2.2** The electrical clearances in Table 6.1.2.2 shall apply to altitudes of 1000 m (3300 ft) or less.

Table 6.1.2.2 Electrical Clearance from Water Spray Equipment to Live Uninsulated Electrical Components

			Minimum* Clearance	
Nomi nal Syste m Voltag	Maxi mum Syste m Voltag	Desig n BIL (kV)	mm	in.
e (kV)	e (kV)			
То	14.5	110	178	7
13.8				
23.0	24.3	150	254	10
34.5	36.5	200	330	13
46.0	48.3	250	432	17
69.0	72.5	350	635	25
115.0	121.0	550	1067	42
138.0	145.0	650	1270	50

161.0	169.0	750	1473	58
230.0	242.0	900	1930	76
		1050	2134	84
345.0	362.0	1050	2134	84
		1300	2642	104
500.0	550.0	1500	3150	124
		1800	3658	144
765.0	800.0	2050	4242	167

NOTE: BIL values are expressed as kilovolts (kV), the number being the crest value of the full wave impulse test that the electrical equipment is designed to withstand. For BIL values that are not listed in the table, clearances may be found by interpolation.

\*For voltages up to 161 kV, the clearances are taken from NFPA 70, *National Electrical Code*. For voltages 230 kV and above, the clearances are taken from Table 124 of ANSI C2, *National Electrical Safety Code*.

- **6.1.2.3** At altitudes in excess of 1000 m (3300 ft), the electrical clearance shall be increased at the rate of 1 percent for each 100 m (330 ft) increase in altitude above 1000 m (3300 ft).
- **6.1.3** Where the design BIL is not available and where nominal voltage is used for the design criteria, the highest minimum clearance listed for this group shall be used.

## 6.2 Water Spray Nozzles.

#### **6.2.1\* Selection.**

- **6.2.1.1** Open water spray nozzles shall be used.
- **6.2.1.2** Automatic nozzles shall be permitted when positioned and located so as to provide satisfactory performance with respect to activation time and distribution.
- **6.2.1.3** The selection of the type and size of spray nozzles shall be made with proper consideration given to such factors as discharge characteristics, physical character of the hazard involved, ambient conditions, material likely to be burning, and the design objectives of the system.
- **6.2.1.4** Where acceptable to the authority having jurisdiction, sprinklers shall be permitted to be used in water spray systems and installed in positions other than anticipated by their listing to achieve specific results where special situations require.
- **6.2.2 Temperature Rating.** The temperature rating for automatic nozzles shall be based on the maximum ambient temperature and determined in accordance with NFPA 13, *Standard for the Installation of Sprinkler Systems*.
- **6.2.3** Water spray nozzles shall be permitted to be placed in any position, within its listing limitations, necessary to obtain proper coverage of the protected area.
- **6.2.4** The positioning of water spray nozzles shall include an evaluation of all the following factors:

- (1) The shape and size of the area to be protected
- (2) The nozzle design and characteristics of the water spray pattern to be produced
- (3) The effect of wind and fire draft on very small drop sizes or on large drop sizes with little initial velocity
- (4) The potential to miss the target surface and increase water wastage
- (5) The effects of nozzle orientation on coverage characteristics
- (6) The potential for mechanical damage

## **6.3 Piping Installation.**

#### **6.3.1 Valves.**

- **6.3.1.1 Water Supply Control Valves.** Each system shall be provided with a control valve located so as to be accessible during a fire in the area the system protects, or any adjacent areas, or, in the case of systems installed for fire prevention, during the existence of the contingency for which the system is installed.
- **6.3.1.2 Valve Supervision.** Valves controlling the water supply to water spray systems shall be supervised open by one of the following methods:
  - (1) Central station, proprietary, or remote station alarm service
  - (2) Local alarm service that will cause the sounding of an audible signal at a constantly attended point
  - (3) Locking valves open
  - (4) Sealing of valves and approved weekly recorded inspection where valves are located within fenced enclosures under the control of the owner
- **6.3.1.3** Underground gate valves with roadway boxes shall not be required to be supervised.

## **6.3.1.4 Location of System Actuation Valves.**

- **6.3.1.4.1** System actuation valves shall be as close to the hazard protected as accessibility during the emergency will permit.
- **6.3.1.4.2** The location of system actuation valves shall include an evaluation of all the following factors:
  - (1) Radiant heat from exposing fire
  - (2) Potential for explosions
  - (3) The location and arrangement of drainage facilities including dikes, trenches, and impounding basins
  - (4) Potential for freezing and mechanical damage
  - (5) Accessibility
  - (6) System discharge time

## 6.3.2 Pipe Support.

- **6.3.2.1** System piping shall be supported to maintain its integrity under fire conditions.
- **6.3.2.2** Piping shall be supported from steel or concrete structural members or pipe stands.
- **6.3.2.2.1\*** Pipe stands used to support piping shall be in accordance with Table 6.3.2.2.1 to determine maximum heights for pipe stands supporting various diameters of looped piping.

Table 6.3.2.2.1 Maximum Pipe Stand Heights

			_		
Pipe Stand Diameter					
Diame ter of Pipe	1½ in.	2 in.	2½ in.	3 in.	4 in.
1½ in.	10 ft	14 ft	18 ft	28 ft	30 ft
2 in.	8 ft	12 ft	16 ft	26 ft	30 ft
$2\frac{1}{2}$ in.	6 ft	10 ft	14 ft	24 ft	30 ft
3 in.	_	8 ft	12 ft	22 ft	30 ft
>3 in.	<u> </u>				10 ft

**6.3.2.2.2\*** Distance between pipe stands exceeding those in Table 6.3.2.2.2 shall be permitted where a 45 degree diagonal is attached between the pipe stand and the loop piping. (See Figure A.6.3.2.2.2.) For piping of other than Schedule 40, pipe stand shall be spaced in accordance with the hanger references of NFPA 13.

Table 6.3.2.2.2 Pipe Stand

Distance				
Loop Size		Betwe	tance en Pipe inds	
in.	mm	ft	mm	
1	25	10	3048	
$1\frac{1}{2}$	40	12	3658	
2	50	14	4267	
$2\frac{1}{2} - 8$	65	_ 15	4572	

- **6.3.2.2.3** Pipe stands shall be constructed of Schedule 40 threaded pipe, malleable iron flange base, and shall have a threaded cap top.
- **6.3.2.2.4\*** Pipe stands shall be anchored to a concrete pier or footing with either drop-in anchors, quik bolts, or cast-in-place J hooks.
- 6.3.2.2.5\* Piping shall be attached to the pipe stand with U-bolts or equivalent attachment.
- **6.3.2.3** Piping support shall be permitted to be attached directly to vessels or other equipment, provided the equipment is capable of supporting the system and the design is certified by a registered professional engineer.
- **6.3.2.4** Tapping and drilling of load-bearing structural elements shall only be permitted where the design of the structural members takes the drilling or tapping into account, where the design includes the additional loads created by the water spray system, and where the design is certified by a registered professional engineer.
- **6.3.2.5** Where welding of supports directly to vessels or equipment is necessary, it shall be done in a safe manner in conformance with the provisions of all safety, structural, and fire

codes and standards.

- **6.3.2.6\*** Hangers shall be installed and located in accordance with NFPA 13, *Standard for the Installation of Sprinkler Systems*.
- **6.3.2.7\*** Where the pipe support methods outlined in this standard or NFPA 13, *Standard for the Installation of Sprinkler Systems*, cannot be used, water spray system piping shall be supported in such a manner equivalent to the performance requirements of this standard or NFPA 13 and the design certified by a registered professional engineer.
- **6.3.2.8** Piping shall be supported and braced to restrict movement due to nozzle reaction and water surges so that system performance and integrity is maintained.

## **6.3.3 Piping Drainage.**

- **6.3.3.1** All water spray system pipe and fittings shall be installed so that the system can be drained.
- **6.3.3.2** Drains shall discharge to a safe location, and drain valves, where provided, shall be accessible.
- **6.3.3.3** Drains shall not be directly interconnected with any sewer systems.
- **6.3.3.4** The drain discharge shall conform to any health or water department regulations.
- **6.3.3.5** Means shall be provided to verify water flow through the drain.
- **6.3.3.6\* System or Main Drain Connections.** Each system shall be provided with drain connections for system risers, mains, and actuation valves.
- **6.3.3.7** Drain connections shall be sized as shown in Table 6.3.3.7.

**Table 6.3.3.7** 

Draii	n Size	
Riser	Size of	
or	Drain	
Main	Conne	
Size	ction	
(in.)	(in.)	
Up to	3/4 or	
2	larger	
$2\frac{1}{2}$ , 3,	$1\frac{1}{4}$ or	
$3\frac{1}{2}$	larger	
4 and	2 only	
larger		
Note:		

For SI

units, 1 in. =

25.4

mm.

## 6.3.3.8 Auxiliary Drains.

- **6.3.3.8.1** Auxiliary drains shall be provided where a change in piping direction prevents drainage of system piping through either the main drain valve or open water spray nozzles.
- **6.3.3.8.2** The sizing of auxiliary drains for water spray systems shall be in accordance with

Table 6.3.3.8.2
Minimum
Auxiliary Drain
Size for Trapped
Water Spray
Pining

riping			
Volume of		Drain	
Trapped		Size	
Pip	ing	(in.)	
gal	L		
< 5	< 18.9	1/2	
5 to 50	18.9 to	3/4	
	189.3		
> 50	>	1.0	
	189.3		
N	ote: For S	SI	

units, 1 gal = 3.8 L; 1 in. = 25.4 mm.

## **6.3.4 Protection Against Freezing.**

- **6.3.4.1** Where used, valve rooms shall be lighted and heated.
- **6.3.4.2** The source of heat shall be of a permanently installed type and shall be capable of maintaining a room temperature at a minimum of 4°C (40°F).
- **6.3.4.3** Where water-filled supply pipes, risers, system risers, or feed mains pass through open areas, cold rooms, passageways, or other areas exposed to freezing, the pipe shall be protected against freezing by insulating coverings, frostproof casing, or other means capable of maintaining a minimum temperature of 4°C (40°F).
- **6.3.4.4** Unheated areas shall be permitted to be protected by antifreeze systems in accordance with NFPA 13, *Standard for the Installation of Sprinkler Systems*, if acceptable to the authority having jurisdiction.
- **6.3.5 Protection Against Damage Where Subject to Earthquakes.** Protection of piping against damage where subject to earthquakes shall be in accordance with NFPA 13, *Standard for the Installation of Sprinkler Systems*.

## 6.3.6\* Protection of Piping Against Damage Where Explosion Potential Exists.

**6.3.6.1** Where water spray systems are installed in areas having an explosion potential, they shall be installed in a manner that will minimize damage to the piping and system control and actuation valves.

## 6.4 System Attachments.

#### **6.4.1 Alarms.**

- **6.4.1.1** All automatic water spray systems shall be provided with a local alarm.
- **6.4.1.2** Any flow from a single automatic nozzle of the smallest orifice size installed on the system or flow from any group of nonautomatic nozzles, shall result in an audible alarm on the premises within 90 seconds after flow begins.

- **6.4.1.3** Where a separate detection system is used to activate the water spray system, the alarm shall be actuated independently of system water flow to indicate operation of the detection system.
- **6.4.1.4** Waterflow alarms shall be installed in accordance with NFPA 13, *Standard for the Installation of Sprinkler Systems*.
- **6.4.1.5** Electrically operated alarm attachments shall be installed in accordance with NFPA 72, *National Fire Alarm Code*.
- **6.4.1.6** Water spray system waterflow alarm systems that are not a part of a required protective signaling system shall not be required to be supervised, but shall be installed in accordance with NFPA 70, *National Electrical Code*, Article 760.

## 6.4.2 Remote Manual Actuation.

- **6.4.2.1** At least one manual actuation device independent of the manual actuation device at the system actuation valve shall be installed for all automatic systems.
- **6.4.2.2** Where the manual release at the systems actuation valve meets the requirements of
- 6.4.2.2 a separate remote manual activation device shall not be required.
- **6.4.2.3** Systems that protect normally unoccupied areas shall not require a separate manual activation means.
- **6.4.2.4** Remote manual actuation devices shall be located so as to be accessible during an emergency.
- **6.4.2.5** Remote manual actuation devices shall be identified with a permanently marked weatherproof metal or rigid plastic sign identifying the system(s) controlled.

## 6.4.3\* Fire Department Connections.

- **6.4.3.1\*** One or more fire department connections shall be provided as described in this section.
- **6.4.3.2** Fire department connections shall not be required for the following installations:
  - (1) Systems located in remote areas that are inaccessible for fire department support shall not require a fire department connection.
  - (2) Large capacity systems exceeding the pumping capacity of the fire department shall not require a fire department connection.
  - (3) Ultra high-speed water spray systems shall not require a fire department connection.
- **6.4.3.3** Size. The number of outlets and size of the outlets and piping in the fire department connection shall be sufficient to supply the water spray system demand.
- **6.4.3.4** The arrangement and other installation features of fire department connections shall be in accordance with NFPA 13, *Standard for the Installation of Sprinkler Systems*.

## **6.4.4 Gauges.**

- **6.4.4.1** Pressure gauges shall be installed as follows:
  - (1) Below the system actuation valve
  - (2) Above and below alarm check valves
  - (3) On the air or water supply to pilot lines

- **6.4.4.2** Pressure gauges shall be installed so as to permit removal.
- **6.4.4.3** Pressure gauges shall be located where they will not be subject to freezing.
- **6.4.4.4** Provisions shall be made for test gauges at or near the highest or most remote nozzle on each separate section of the system.
- **6.4.4.5** At least one gauge connection shall be provided at or near the nozzle calculated as having the least pressure under normal flow conditions.
- **6.4.5 Alarm Test Connection for Wet Pipe Systems.** An alarm test connection shall be provided for all wet pipe systems in accordance with NFPA 13, *Standard for the Installation of Sprinkler Systems*.

#### 6.4.6 Strainers.

- **6.4.6.1\*** Main pipeline strainers shall be provided for all systems utilizing nozzles with waterways less than 9.5 mm ( $\frac{3}{8}$  in.) and for any system where the water is likely to contain obstructive material.
- **6.4.6.2** Mainline pipeline strainers shall be installed so as to be accessible for flushing or cleaning.
- **6.4.6.3** Individual or integral strainers shall be provided at each nozzle where waterways smaller than 3.2 mm ( $\frac{1}{8}$  in.) are used.

## 6.5 Automatic Detection Equipment.

#### 6.5.1 Protection.

- **6.5.1.1 Corrosion Protection.** Detection equipment installed outdoors or in the presence of possible corrosive vapors or atmospheres shall be protected from corrosion by suitable materials of construction or by suitable protection coatings applied by the equipment manufacturer.
- **6.5.1.2 Protective Canopy.** Detection equipment requiring protection from the weather shall be provided with a canopy, hood, or other suitable protection.
- **6.5.1.3\* Mechanical Damage.** Detection equipment shall be located so as to be protected from mechanical damage.
- **6.5.1.4 Mounting.** Detectors shall, in all cases, be supported independently of their attachment to wires or tubing.
- **6.5.1.5** Pilot type automatic sprinklers shall be permitted to be supported by their piping or tubing.
- 6.5.2 Selection, Location, and Spacing of Detectors.
- **6.5.2.1** The selection, location, and spacing of automatic fire detectors for the actuation of fixed water spray systems shall meet or exceed the applicable requirements of NFPA 72, *National Fire Alarm Code*, and be consistent with the following:
  - (1) Data obtained from field experience
  - (2) Tests
  - (3) Engineering surveys

- (4) Manufacturer's recommendations
- (5) Detectors' listing criteria
- (6) Nature of the hazard being protected
- (7) Both normal and abnormal air velocities
- (8) Range of anticipated temperatures
- (9) Maximum expected rates of temperature change under nonfire conditions
- (10) Number and height of structural levels
- (11) Effects of precipitation (rain and snow)
- (12) Presence and magnitude of electromagnetic interference
- (13) Presence of obstructions that might retard or mitigate timely detection
- (14) Other conditions that might affect the efficacy of the fire detection employed
- **6.5.2.2** Detectors shall be located so as to promptly respond to a fire, flammable gas release, or other design condition.
- **6.5.2.2.1** The detection system shall be capable of detecting a fire up to the elevation of the highest level of protected equipment surface.
- **6.5.2.2.2** Detectors shall be located so that no portion of the hazard being protected extends beyond the perimeter line of detectors.

## 6.5.2.3\* Outdoor Detector Spacing.

- **6.5.2.3.1** When located out of doors or in the open, the spacing of fixed temperature or rate-of-rise detectors shall be reduced by at least 50 percent from the listed spacings under smooth ceilings.
- **6.5.2.3.2** Where testing has demonstrated acceptable performance at other spacings, those spacings shall be permitted.
- **6.5.2.3.3** Pilot sprinklers spaced in accordance with 6.5.2.4 shall not require reduced spacing.
- **6.5.2.3.4** Where specific guidance is provided in the listing, detectors specifically listed for outdoor installation shall be installed in accordance with the listing requirements.

## **6.5.2.4 Pilot-Type Sprinklers.**

- **6.5.2.4.1** The temperature rating of pilot-type sprinklers shall be selected in accordance with NFPA 13, *Standard for the Installation of Sprinkler Systems*.
- **6.5.2.4.2** Where located under a ceiling, pilot sprinklers shall be positioned in accordance with the requirements for automatic sprinklers in NFPA 13, *Standard for the Installation of Sprinkler Systems*.
- **6.5.2.4.3** Maximum horizontal spacing for indoor locations shall not exceed 3.7 m (12 ft).
- **6.5.2.4.4** The obstruction to water distribution rules for automatic sprinklers shall not be required to be followed where pilot sprinklers are used.
- **6.5.2.4.5** Pilot sprinklers shall be permitted to be spaced more than 559 mm (22 in.) below a ceiling or deck where the maximum spacing between pilot sprinklers is 3 m (10 ft) or less.
- **6.5.2.4.6** Other maximum horizontal pilot sprinkler spacings differing from those required

- in 6.5.2.4.2 and 6.5.2.4.3 shall be permitted where installed in accordance with their listing.
- **6.5.2.4.7** Pilot sprinklers located outdoors, such as in open process structures, shall be spaced such that the elevation of a single level of pilot sprinklers and between additional levels of pilot sprinklers shall not exceed 5.2 m (17 ft).
- **6.5.2.4.8** The horizontal distance between pilot sprinklers installed outdoors shall not exceed 2.5 m (8 ft).
- **6.5.2.4.9** The horizontal distance between pilot sprinklers installed outdoors on a given level shall be permitted to be increased to 3 m (10 ft) when the elevation of the first level does not exceed 4.6 m (15 ft), the distance between additional levels does not exceed 3.7 m (12 ft), and the pilot sprinklers are staggered vertically.
- **6.5.2.4.10** Other vertical pilot sprinkler spacings differing from those required in 6.5.2.4.7 and 6.5.2.4.8 shall be permitted where installed in accordance with their listing.

## **6.5.2.5 Special Situations.**

## 6.5.2.5.1 Open-Sided Buildings.

- **6.5.2.5.1.1** Detectors located in open-sided buildings shall follow the indoor spacing rules.
- **6.5.2.5.1.2** A line of detectors in accordance with the outdoor detector spacing rules shall be located along the open sides of open-sided buildings.
- **6.5.2.5.2 Under Open Gratings.** Detectors located under open gratings shall be spaced in accordance with the outdoor rules.
- **6.5.2.6 Two or More Systems.** Where there are two or more adjacent water spray systems in one area controlled by separate detection systems, the detectors on each system shall be spaced independently as if the dividing line between the systems were a wall or draft curtain.

## 6.5.2.7\* Flammable Gas Detectors.

- **6.5.2.7.1** The location of flammable gas detectors shall take into consideration the density of the flammable gas and its temperature and proximity to equipment where leakage is more likely to occur.
- **6.5.2.7.2** Access for testing, calibration, and maintenance of flammable gas detectors shall be provided.
- **6.5.2.8 Radiant Energy Sensing Fire Detectors.** Radiant energy sensing fire detectors shall be spaced and located in accordance with their listings and manufacturer's recommendations

## 6.5.3 Arrangement and Supervision of Systems.

## 6.5.3.1 Electrical Systems.

- **6.5.3.1.1** Water spray systems that depend on electric thermostats, relay circuits, flammable gas detectors, or other similar equipment shall be so arranged that such equipment is normally energized or completely supervised in a manner that will result in positive notifications on an abnormal condition in accordance with NFPA 72, *National Fire Alarm Code*, unless failure of the detection system results in the operation of the water spray system.
- **6.5.3.1.2** Supervision shall include, but not be limited to, the tripping device, solenoid valve, and any connecting wiring.

**6.5.3.2 Pneumatic and Hydraulic Systems.** Pneumatically and hydraulically operated systems shall be supervised in a manner such that failure will result in positive notification of the abnormal condition, unless the failure results in operation of the water spray system.

# **Chapter 7 Design Objectives**

## 7.1 System Design.

- **7.1.1** Systems shall be arranged for automatic operation with supplementary manual tripping means provided.
- **7.1.2** Manual operation shall be permitted where automatic operation of the system presents a hazard to personnel.
- **7.1.3** Manual operation of the system shall be permitted where a system is isolated and attended by trained personnel at all times.
- **7.1.4** Systems shall be designed to accomplish at least one of the design objectives defined in Section 4.1 and in accordance with Sections 7.2 through 7.5, as applicable.
- **7.1.5** Systems shall be permitted to have other design objectives requiring different protection where approved by the authority having jurisdiction.
- **7.1.6\*** The system and water supplies shall be designed to admit water into the piping and to discharge effective water spray from all open nozzles without delay.
- **7.1.7** The design shall ensure that the nozzle spray patterns meet or overlap.
- **7.1.8** Nozzle spacing (vertically or horizontally) shall not exceed 3 m (10 ft).
- **7.1.9** Nozzles shall be permitted to exceed the spacing requirements of 7.1.8 where listed for spacing exceeding 3 m (10 ft).

## 7.1.10 Size of System and Water Demand.

- **7.1.10.1\*** A single system shall not protect more than one fire area.
- **7.1.10.2\*** The number of systems expected to operate simultaneously shall be determined by evaluating the following factors:
  - (1) Possible flow of burning liquids between areas before or during operation of the water spray systems
  - (2) Possible flow of hot gases between fire areas that could actuate adjoining systems, thereby increasing demand
  - (3) Flammable gas detection set to automatically actuate systems
  - (4) Manual operation of multiple systems
  - (5) Other factors that would result in operation of systems outside of the primary fire area
- **7.1.10.3** The hydraulically designed discharge rate for a single system or multiple systems designed to operate simultaneously shall not exceed the available water supply. (See 9.2.1.)

## 7.2 Extinguishment.

#### **7.2.1** General.

**7.2.1.1 Design Objective.** Systems shall be designed so that extinguishment shall be accomplished and all protected surfaces shall be cooled to prevent flashback occurring after

the system is shut off.

- **7.2.1.2\* Extinguishment Methods.** Extinguishment of fires by water spray shall be accomplished by one or a combination of the following methods:
  - (1) Surface cooling
  - (2) Smothering by produced steam
  - (3) Emulsification
  - (4) Dilution
- (5) Other factors
- **7.2.1.3\* Design Density.** A general range of water spray application rates that shall apply to most ordinary combustible solids or liquids shall be from 6.1 (L/min)/m<sup>2</sup> to 20.4 (L/min)/m<sup>2</sup> (0.15 gpm/ft<sup>2</sup> to 0.50 gpm/ft<sup>2</sup>) of protected surface.
- **7.2.1.4** The specific design density for extinguishment shall be based on test data or knowledge concerning conditions similar to those that will apply in the actual installation.
- 7.2.2 Cable Trays and Cable Runs.
- **7.2.2.1\*** Where insulated wire and cable or nonmetallic tubing is to be protected by an automatic water spray (open nozzle) system designed for extinguishment of fire that originates within the cable or tube, the system shall be hydraulically designed to impinge water directly on each tray or group of cables or tubes at a net rate of 6.1 (L/min)/m² (0.15 gpm/ft²) on the projected plane containing the cable or tubing tray or run.
- **7.2.2.2** Cable trays and cable runs shall be permitted to be protected by other water spray densities and methods of application where verified by tests and where acceptable to the authority having jurisdiction.
- **7.2.2.3\*** Automatic detection devices shall detect smoldering or slow-to-develop flames.
- **7.2.2.4** Where it is likely that spills of flammable liquids or molten materials will expose cables, nonmetallic tubing, and tray supports, the design of protection systems shall be in accordance with that specified for exposure protection. (*See 7.4.3.8.*)

#### 7.2.3 Belt Conveyors.

#### **7.2.3.1** General.

- **7.2.3.1.1** Open nozzles shall be located to direct water spray onto the surfaces to extinguish fire in hydraulic oil, the belt, the contents on the belt, or the drive unit.
- **7.2.3.1.2** Water spray impingement on structural elements shall provide exposure protection against radiant heat or impinging flame.
- **7.2.3.1.3** Interlocks shall be provided between the detection system and the machinery to shut down belt conveyor operation, including upstream feed. (See Sections 6.5 and 7.7.)
- **7.2.3.1.4** The water supply shall be capable of supplying both the design flow rate and 946 L/min (250 gpm) for hose streams for a minimum duration of 1 hour.

#### 7.2.3.2\* Drive Unit.

- **7.2.3.2.1** The water spray system shall be installed to protect the drive rolls, the take-up rolls, the power units, and the hydraulic-oil unit.
- **7.2.3.2.2** The net rate of water application for the drive unit shall be not less than 10.2

 $(L/min)/m^2$  (0.25 gpm/ft<sup>2</sup>) of roll and belt.

### 7.2.3.3 Conveyor Belt.

- **7.2.3.3.1\*** The water spray system shall be installed to automatically wet the top belt, its contents, and the bottom return belt.
- **7.2.3.3.2** Discharge patterns of water spray nozzles shall envelop, at a net rate of not less than 10.2 (L/min)/m<sup>2</sup> (0.25 gpm/ft<sup>2</sup>), the top and bottom belt surface area, conveyor surfaces where combustible materials are likely to accumulate, the structural parts, and the idler-rolls supporting the belt.
- **7.2.3.3.3** Water spray system protection for belt conveyors shall accomplish either of the following:
  - (1) Extend onto transfer belts, transfer equipment, and transfer building
  - (2) Interlock in such a manner that the water spray system protecting the feeding belt will automatically actuate the water spray system protecting the first segment of the downstream equipment

### 7.3 Control of Burning.

#### **7.3.1** General.

- **7.3.1.1\*** A system for the control of burning shall operate as intended until there has been time for the burning material to be consumed, for steps to be taken to shut off the flow of leaking material, or until the burning material can be otherwise extinguished.
- **7.3.1.2** Nozzles shall be positioned to impinge water directly on the areas of the source of fire and where spills are likely to spread or accumulate.
- **7.3.1.3** The water application rate shall be at a net rate of not less than 20.4 (L/min)/m<sup>2</sup> (0.50 gpm/ft<sup>2</sup>) of protected area.
- **7.3.2\* Pumps, Compressors, and Related Equipment.** Pumps or other devices that handle flammable liquids or gases shall have the shafts, seals, and other critical parts enveloped by directed water spray at a net rate of not less than 20.4 (L/min)/m<sup>2</sup> [0.50 gpm/ft<sup>2</sup>] of projected surface area of the equipment.
- **7.3.3 Flammable and Combustible Liquid Pool Fires.** Water spray systems designed to control pool fires resulting from a flammable or combustible liquid spill fire shall be designed to apply a net rate of not less than 12.2 (L/min)/m<sup>2</sup> (0.30 gpm/ft<sup>2</sup>) of protected area.
- **7.3.3.1** Subsection 7.3.3 shall apply to the control of pool fires resulting from a flammable or combustible liquid spill.
- **7.3.3.2** The water spray system shall be designed to apply a net rate of not less than 12.2  $(L/min)/m^2$  (0.30 gpm/ft<sup>2</sup>) of protected area.

#### 7.4 Exposure Protection.

### 7.4.1\* General.

**7.4.1.1\*** A system for exposure protection shall operate as intended for the anticipated duration of the exposure fire.

### 7.4.2\* Vessels.

- **7.4.2.1** Water spray shall be applied to vessel surfaces (including top and bottom surfaces of vertical vessels) at a net rate of not less than 10.2 (L/min)/m<sup>2</sup> (0.25 gpm/ft<sup>2</sup>) of exposed surface.
- **7.4.2.2\*** Where rundown is contemplated, the distance between nozzles at different levels or elevations, protecting vertical or inclined surfaces, shall not exceed 3.7 m (12 ft) as measured along the surface.
- **7.4.2.3\*** The horizontal distance between nozzles shall be such that spray patterns meet or overlap at the protected surface.
- **7.4.2.4** Spherical or horizontal cylindrical surfaces below the vessel equator shall not be considered wettable from rundown.
- **7.4.2.5** Where projections (manhole flanges, pipe flanges, support brackets, relief valves, etc.) will obstruct water spray coverage, including rundown on vertical surfaces, additional nozzles shall be installed around the projections to maintain the wetting pattern that otherwise would be seriously interrupted.
- **7.4.2.6** All uninsulated vessel skirts and any uninsulated steel saddles greater than 305 mm (12 in.) high at the lowest point shall have water spray applied on one exposed (uninsulated) side, at a net rate of not less than 10.2 (L/min)/m<sup>2</sup> (0.25 gpm/ft<sup>2</sup>).

### 7.4.3 Structures and Miscellaneous Equipment.

**7.4.3.1\* Horizontal Structural Steel.** Horizontal, stressed (primary) structural steel members shall be protected by nozzles and piping of such size and arrangement to discharge a net rate of not less than 4.1 (L/min)/m<sup>2</sup> (0.10 gpm/ft<sup>2</sup>) over the wetted area, as per Figure 7.4.3.1.



### FIGURE 7.4.3.1 Wetted surface of a structural member (a beam or column).

- **7.4.3.2** Horizontal structural steel that has been encased in fire-resistant insulating material to provide a level of fire resistance acceptable to the authority having jurisdiction shall not require water spray protection.
- **7.4.3.3 Alternative Engineering Analysis for Horizontal Structural Steel.** Horizontal structural steel shall not require water spray exposure protection where all of the following are met:
  - (1) Horizontal structural steel shall be analyzed and determined, through calculations certified by a registered professional engineer, to withstand the worst case postulated fire.
  - (2) Calculations shall verify that the temperature of the steel members does not exceed that which would compromise structural integrity.
  - (3) The calculation methodology shall be approved and acceptable to the authority having jurisdiction.
- 7.4.3.4\* Vertical Structural Steel. Vertical structural steel members shall be protected by

nozzles and piping of such size and arrangement as to discharge a net rate of not less than 10.2 (L/min)/m<sup>2</sup> (0.25 gpm/ft<sup>2</sup>) over the wetted area. (See Figure 7.4.3.1.)

- **7.4.3.5** Vertical structural steel that has been encased in fire-resistant insulating material to provide a level of fire resistance acceptable to the authority having jurisdiction shall not require water spray protection.
- **7.4.3.6 Alternative Engineering Analysis for Vertical Structural Steel.** Vertical structural steel shall not require water spray exposure protection where all of the following are met:
  - (1) Vertical structural steel shall be analyzed and determined, through calculations certified by a registered professional engineer, to withstand the worst case postulated fire.
  - (2) Calculations shall verify that the temperature of the steel members does not exceed that which would compromise structural integrity.
  - (3) The calculation methodology shall be approved and acceptable to the authority having jurisdiction.

### 7.4.3.7 Metal Pipe, Tubing, and Conduit.

- **7.4.3.7.1** Water spray intended to protect metal pipe, tubing, and conduit in racks shall be directed toward the underside of the pipes, tubes, and conduit.
- **7.4.3.7.2** Water spray protection shall be permitted to be applied to the top of pipes on racks where water spray piping cannot be installed below the rack due to the potential of physical damage or where space is inadequate for proper installation.
- **7.4.3.7.3** The levels protected and the densities required shall be in accordance with Table 7.4.3.7.3.

Table 7.4.3.7.3 Protection of Metal Pipe, Tubing, and Conduit

Numb er of Rack Levels	Plan View Density at Lowest Level			Plan Dens Up Lev	Levels Requi ring Nozzle s		
gpm /ft <sup>2</sup>	(L/mi n) /m <sup>2</sup>		gpm /ft <sup>2</sup>	(L/mi n) /m <sup>2</sup>			
1	0.25	10.2		N/A	N/A	All	
2	0.20	8.2		0.15	6.1	All	
3, 4, or 5	0.20	8.2		0.15	6.1	Altern ate	
6 or more	0.20	8.2		0.10	4.1	Altern ate	

\*The table values contemplate exposure from a spill fire.

- **7.4.3.7.4** Water spray shall be applied to the underside of the top level even if located immediately above a protected level.
- **7.4.3.7.5** Nozzles shall be selected and positioned such that spray patterns meet or overlap at the protected surface for the entire width of the rack.

- **7.4.3.7.6** Nozzles shall be positioned no more than ft 0.8 m ( $2\frac{1}{2}$  ft) below the bottom of the level being protected.
- **7.4.3.7.7** Where the rack horizontal support members create an obstruction to the spray pattern, nozzles shall be spaced within the bays.
- **7.4.3.7.8** Vertical structural supports shall be protected in accordance with 7.4.3.4.
- **7.4.3.7.9** Vertically stacked piping shall be protected by water spray directed at one side (vertical plane) of the piping at a net rate of not less than 6.1 (L/min)/m<sup>2</sup> (0.15 gpm/ft<sup>2</sup>).

### 7.4.3.8 Cable Trays and Cable Runs.

- **7.4.3.8.1** Where insulated wire, cable, or nonmetallic tubing in open trays or runs is to be protected by water spray from a spill fire exposure, a net rate of not less than 12.2 (L/min)/m<sup>2</sup> (0.30 gpm/ft<sup>2</sup>) of projected horizontal or vertical plane area containing the cables or tubes shall be provided.
- **7.4.3.8.2** Water spray nozzles shall be arranged to supply water at this rate both over and under (or to the front and rear of) cable or tubing runs and to the racks and supports. **7.4.3.8.3 Flame Shield Use.**
- **7.4.3.8.3.1** Where flame shields equivalent to 1.6-mm ( $^{1}_{16}$ -in.) thick steel plate are mounted below cable or tubing runs, the water density requirements shall be permitted to be reduced to a net rate of not less than 6.1 (L/min)/m<sup>2</sup> (0.15 gpm/ft<sup>2</sup>) over the upper surface of the cable or rack.
- **7.4.3.8.3.2** The steel plate or equivalent flame shield shall be wide enough to extend at least 152 mm (6 in.) beyond the side rails of the tray or rack in order to deflect flames or heat emanating from spills below cable or conduit runs.
- **7.4.3.8.4** Where other water spray nozzles are arranged to extinguish, control, or cool exposing liquid surfaces, the water spray density shall be permitted to be reduced to a net rate of not less than 6.1 (L/min)/m<sup>2</sup> (0.15 gpm/ft<sup>2</sup>) over the upper surface, front, or back of the cable or tubing tray or run.

#### 7.4.4 Transformers.

- **7.4.4.1\*** Transformer protection shall provide complete water spray impingement on all exposed exterior surfaces.
- **7.4.4.2** Where there is insufficient space to install water spray nozzles underneath transformers such that the water spray cannot directly impinge upon the bottom surfaces, it shall be permitted to protect the surfaces underneath the transformer by horizontal projection or by nozzles directed to cool the area below the transformer projections.
- 7.4.4.3 Application and Protection.
- **7.4.4.3.1** The water shall be applied at a net rate not less than 10.2 (L/min)/m² (0.25 gpm/ft²) of projected area of rectangular prism envelope for the transformer and its appurtenances, and not less than 6.1 (L/min)/m² (0.15 gpm/ft²) on the expected nonabsorbing ground surface area of exposure.
- **7.4.4.3.2** The water shall be applied at a net rate of not less than  $6.1(L/min)/m^2$  (0.15 gpm/ft<sup>2</sup>) on the expected nonabsorbing ground surface area of exposure.
- **7.4.4.3.3** Water spray application as specified in 7.4.4.3.1 and 7.4.4.3.2 shall be provided for special configurations, conservator tanks, pumps, and so forth.

- **7.4.4.3.4** Where transformer components create spaces greater than 305 mm (12 in.) in width, the surfaces shall be individually protected.
- **7.4.4.3.5** Where there is insufficient clearance to achieve direct impingement, it shall be permitted to protect the surfaces underneath the transformer by horizontal projection or by nozzles directed to cool the area below the transformer projections.
- **7.4.4.3.6** The water supply shall be capable of supplying both the design flow rate and 946 L/min (250 gpm) for hose streams for a minimum duration of 1 hour.
- **7.4.4.4** Water spray piping shall not be routed across the top of the transformer tank or across the face of the transformer cabinet.
- **7.4.4.5** Piping shall be permitted to be routed across the top of the transformer tank or across the face of the transformer cabinet, where impingement cannot be accomplished with any other configuration and the required distance from live electrical components is maintained. (See 6.1.2.)
- **7.4.4.6** Nozzles shall be positioned such that the water spray does not envelop energized bushings or lightning arresters by direct impingement.
- **7.4.4.7** Direct impingement of water spray on energized bushings and/or lightning arresters shall only be permitted when authorized by the manufacturer or manufacturer's literature and the owner.

### 7.5\* Prevention of Fire.

- **7.5.1** The system shall operate as intended for the time necessary to dissolve, dilute, disperse, or cool flammable vapor, gases, or hazardous materials.
- **7.5.2** The duration of release of the flammable materials shall be included in the determination of the water spray duration time.
- **7.5.3** The minimum net rate of application shall be based upon field experience with the product or upon actual test data.

#### 7.6 Combined Systems.

#### 7.6.1\* General.

- **7.6.1.1** The sprinkler system portion of combined systems shall be designed and installed in accordance with NFPA 13, *Standard for the Installation of Sprinkler Systems*.
- **7.6.1.2** The water spray portion of any combined system shall be designed and installed in accordance with this standard.

#### 7.6.2\* Design.

- **7.6.2.1** The system demand shall include the simultaneous hydraulic demand from all sprinklers and water spray nozzles on the system.
- **7.6.2.2** The water spray component of the combined demand shall not reduce the minimum required sprinkler discharge density.

#### 7.7 Automatic Detection Equipment.

**7.7.1\* General.** Detection systems providing an actuation signal to fixed water spray systems shall be designed in accordance with NFPA 72, *National Fire Alarm Code*.

- **7.7.2** The spacing, location, and position of detectors shall be in accordance with 6.5.2.
- 7.7.3\* The following shall be evaluated when selecting and adjusting detection equipment:
  - (1) Normally changing conditions
- (2) Non-fire temperature changes

### 7.7.4\* Response Time.

- **7.7.4.1** The detection system shall be designed to cause actuation of the system actuation valve to operate without delay.
- **7.7.4.2** Where ambient conditions exist that cause false system operations, detection systems shall be permitted to include delays that would override these conditions.

# **Chapter 8 Plans and Hydraulic Calculations**

#### 8.1 General.

- **8.1.1\*** Hydraulic calculations shall be conducted as part of the design of the piping system to determine that the required pressure and flow is available at each nozzle.
- **8.1.2\*** Minimum operating pressure of any nozzle protecting outdoor hazard shall be 1.4 bar (20 psi).
- **8.1.3** Nozzles protecting interior hazards shall have minimum operating pressures in accordance with their listing.
- **8.1.4\*** Correction for velocity pressure shall be included in the calculations.
- **8.1.5** The calculations shall be permitted to ignore velocity pressure corrections where the velocity pressure does not exceed 5 percent of the total pressure at each junction point.

### 8.2 Working Plans.

### **8.2.1** General.

- **8.2.1.1** Working plans shall be submitted to the authority having jurisdiction before any equipment is installed or remodeled.
- **8.2.1.2** Deviation from approved plans shall require permission of the authority having jurisdiction.
- **8.2.1.3** Working plans, including elevations, shall be drawn to an indicated scale, show all essential details, and include the following pertinent data as a minimum:
  - (1) The dates of initial submission and revisions.
  - (2) The name of the owner and occupant.
  - (3) The name and address of the contractor and layout technician.
  - (4) The location, including the street address.
  - (5) The point of the compass.
  - (6) The full height cross section.
  - (7) The structural features.
  - (8) The relative elevations of nozzles, junction points, and supply or reference points.
  - (9) Full information concerning water supplies, including such items as pumps,

- underground mains, earthquake protection, and flow test results.
- (10) The make, type, size, location, position, and direction of spray nozzles.
- (11) The make, type, model, and size of the system actuation valve, control valve, or special system valve. The method of control valve supervision shall be indicated on the plans.
- (12) The type and location of alarm devices to be provided. The type and location of the control panel.
- (13) The number of each size and type of spray nozzles on each system.
- (14) The type of pipe and schedule of wall thickness, lengths of pipe, and whether center to center or cutting lengths are shown.
- (15) The size and type of all fittings; the dimensions and locations of shop welded sections.
- (16) The sensing devices for detection, including the type, arrangement, and location.
- (17) The hydraulic reference points shown on the plan shall correspond with comparable reference points on the hydraulic calculation sheets.
- (18) The calculated system demand at a reference point.
- (19) The total designed water demand with the number of systems designed to operate simultaneously at a reference point, preferably the source of supply, including hose streams and other fire protection equipment.
- (20) The density requirements and hazard surface calculation, where applicable.
- (21) The design objective of the system.
- (22) The make, type, and location of hangers, supports, sleeves, sway bracing, and inserts.
- (23) All control and check valves, strainers, drain pipes, and test pipes.
- (24) A graphic representation of the scale used on all plans.
- (25) The weight or class, lining, and size of underground pipe and the depth that the top of the pipe is to be laid below grade.
- (26) Provisions for flushing underground pipe.
- (27) Accurate and complete layout of the hazard to be protected.
- **8.2.1.4** The working plan submittal shall include manufacturer's installation instructions for any specially listed equipment, including descriptions, applications, and limitations for any nozzles, devices, piping, fittings, supports and bracing materials.
- **8.2.1.5** When the equipment to be installed is an addition or change to an existing system, details of the existing system shall be indicated on the working plans to allow for review of the design and supporting hydraulic calculations.

### 8.3\* Hydraulic Calculations.

- **8.3.1** Hydraulic calculations shall be prepared on forms that include a summary sheet, detailed worksheet, and a graph sheet.
- **8.3.2\* Summary Sheet.** The summary sheet *[for sample summary sheet, see Figure B.1(a)]* shall contain all of the following information where applicable:
  - (1) The date
  - (2) The location
  - (3) The name of the owner and occupant
  - (4) The building or plant number
  - (5) The description of the hazard
  - (6) The name and address of the contractor and calculator
  - (7) The name of the authority having jurisdiction
  - (8) The design purpose
  - (9) The rates of the water application (density) and applied areas in (L/min)/m<sup>2</sup> (gpm/ft<sup>2</sup>)
  - (10) The total system water requirements as calculated, including allowance for hose streams
  - (11) The total designed water demand with number of systems designed to operate simultaneously at a reference point, preferably the source of supply, including hose streams and other fire protection equipment
  - (12) Water supply information
- **8.3.3\* Detailed Worksheets.** Detailed worksheets or computer printout sheets *[for sample worksheet, see Figure B.1(b)]* shall contain all of the following information:
  - (1) Sheet number, date, job number, and identification of calculations covered
  - (2) Description of discharge constant (K) (or provide the discharge curve or tabulation) for each nozzle type
  - (3) Hydraulic reference points
  - (4) Flow in L/min (gpm)
  - (5) Pipe size in mm (in.)
  - (6) Pipe lengths, center to center of fittings (or cut lengths) in m (ft)
  - (7) Equivalent pipe lengths for fittings and devices in m (ft)
  - (8) Friction loss in bar (psi) between reference points
  - (9) Total friction loss in bar (psi) between reference points
  - (10) Elevation head in bar (psi) between reference points
  - (11) Required pressure in bar (psi) at each reference point

- (12) Velocity pressure and normal pressure if included in calculations
- (13) Notes to indicate starting points, reference to other sheets, or to clarify data shown
- (14) Combined *K*-factor calculations for nozzles on drops, armovers, or sprigs where calculations do not begin at a nozzle
- (15) When extending existing equipment, hydraulic calculations are to be furnished indicating the previous design, volume, and pressure at points of connection, and adequate additional calculations to indicate effect on existing systems.

### 8.3.4\* Graph Sheet.

**8.3.4.1** The graph sheet shall be plotted on semi-logarithmic graph paper ( $O^{1.85}$ ).

**8.3.4.2** Water supply curves and system requirements, plus hose demand if required, shall be plotted to present a graphic summary of the complete hydraulic calculation.

### 8.4 Water Supply Information.

The following information shall be included on the plans and calculations:

- (1) Location and elevation of static and residual test gauge, with relation to the system actuation valve reference point
- (2) Flow location
- (3) Static pressure, bar (psi)
- (4) Residual pressure, bar (psi)
- (5) Flow, L/min (gpm)
- (6) Date
- (7) Time
- (8) Source of water flow test information
- (9) Other sources of water supply, with pressure or elevation

### **8.5 Hydraulic Calculation Procedures.**

#### 8.5.1 Formulae.

**8.5.1.1 Friction Loss Formula.** Pipe friction losses shall be determined on the basis of the Hazen and Williams formula,

$$p = \frac{4.52Q^{1.85}}{C^{1.85}d^{4.87}}$$

where:

p = frictional resistance in psi per foot of pipe

Q = flow in gpm

d = actual internal diameter of pipe in inches

C =friction loss coefficient

or in SI units,

$$P_{w} = 6.05 \times \frac{Q_{w}^{1.85}}{C^{1.85} d_{m}^{4.87}} \times 10^{5}$$

where:

 $P_m$  = frictional resistance in bars per meter of pipe

 $Q_m = \text{flow in L/min}$ 

 $d_m$  = actual internal diameter in mm

C =friction loss coefficient

**8.5.1.2\* Velocity Pressure Formula.** The velocity pressure shall be determined on the basis of the formula,

$$P_v = \frac{0.001123Q^2}{D^4}$$

where:

 $P_v$  = velocity pressure in psi

Q = flow in gpm

D =inside diameter in inches

**8.5.1.3 Normal Pressure Formula.** Normal pressure shall be determined on the basis of the formula,

$$P_n = P_t - P_v$$

where:

 $P_n$  = normal pressure in bar (psi)

 $P_t$  = total pressure in bar (psi)

 $P_v$  = velocity pressure in bar (psi)

8.5.1.4 Hydraulic Junction Points.

**8.5.1.4.1** Hydraulic junction point calculations shall be balanced within 0.03 bar (0.5 psi).

**8.5.1.4.2** The highest pressure at the junction point, and the total flows as adjusted, shall be carried into the calculations.

**8.5.1.4.3** Hydraulic junction point calculations, except for loops, shall be balanced to the higher pressure by the formula, (corrected for elevations),

$$\frac{Q_1}{Q_2} = \sqrt{\frac{P_1}{P_2}}$$

**8.5.1.5 Nozzle Discharge Formula.** The discharge of a nozzle shall be calculated by the formula,

$$Q=K\sqrt{P}$$

where:

Q = gpm flowing from the nozzle

K = nozzle K-factor

P = total pressure in psi at the flow Q

or in SI units,

$$Q_m = K_m \sqrt{P_m}$$

where:

 $Q_m = \text{flow in L/min}$ 

 $K_m$  = nozzle K-factor (where  $K_m$  equals 14.4 K)

 $P_m$  = total pressure in bars at the flow  $Q_m$ 

**8.5.1.5.1** The normal pressure  $(P_n)$ , calculated by subtracting the velocity pressure  $(P_v)$  from the total pressure  $(P_t)$ , shall be permitted to be used to calculate the nozzle discharge, unless the nozzle is an end nozzle, when total pressure  $(P_t)$  is permitted per 8.1.5.

### 8.5.2 Equivalent Pipe Lengths of Valves and Fittings.

**8.5.2.1** Table 8.5.2.1 shall be used to determine equivalent lengths of valves and fittings, unless the manufacturer's test data indicates that other factors are appropriate.

**Table 8.5.2.1 Equivalent Pipe Length Chart** 

Fittings and Valves					Fittings and V	alves E	Expressed in Eq	uivaleı	nt Meter (Feet)
	3/4 in.		1 in.		1¼ in.	_	1½ in.		2 in.
	n ft		n ft		n ft	_	n ft		n ft
45° Elbow	0.3	1	0.3	1	0.3	1	0.6	2	0.6
90° Standard elbow	0.6	2	0.6	2	0.9	3	1.2	4	1.5
90° Long turn elbow	0.3	1	0.6	2	0.6	2	0.6	2	0.9
Tee or cross (Flow	1.2	4	1.5	5	1.8	6	2.4	8	3.1
turned 90°)									
Gate valve		_	_		_				0.3
Butterfly valve									1.8
Swing check*	1.2	4	1.5	5	2.1	7	2.7	9	3.4

	Fittings and Valves Expressed in Equivalent Meter (Feet) of Pipe										
Fittings and Valves	3½ in. n ft		<u>4 in.</u> n ft		5 in. n ft		6 in.	8 in. n ft			
							n ft				
45° Elbow	0.9	3	1.2	4	1.5	5	2.1	7	2.7		
90° Standard elbow	2.4	8	3.1	10	3.7	12	4.3	14	5.5		
90° Long turn elbow	1.5	5	1.8	6	2.4	8	2.7	9	4.0		
Tee or cross (Flow turned 90°)	5.2	17	6.1	20	7.6	25	9.2	30	10.7		
Gate valve	0.3	1	0.6	2	0.6	2	0.9	3	1.2		
Butterfly valve			3.7	12	2.7	9	3.1	10	3.7		
Swing check*	5.8	19	6.7	22	8.2	27	9.8	32	13.7		

\*Due to the variations in design of swing check valves, the pipe equivalents indicated in this chart a

#### Notes:

- 1. Use the equivalent m (ft) value for the "standard elbow" on any abrupt 90° turn such as the screw-type pattern. Use the equivalent m (ft) value for the "standard elbow" on any abrupt 90° turn such as flanged, welded, or mechanical joint elbow type.
- 2. For internal pipe diameters different from Schedule 40 steel pipe, the equivalent feet shown shall be multiplied by a factor de

$$\left(\frac{\text{actual inside diameter}}{\text{Schedule 40 steel pipe inside diameter}}\right)^{4.87} = \text{factor}$$

**8.5.2.2** Specific friction loss values or equivalent pipe lengths for system actuation valves and other devices shall be made available to the authority having jurisdiction.

**8.5.2.3** Use with Hazen and Williams, C = 120 only. For other values of C, the figures in Table 8.5.2.1 shall be multiplied by the following factors:

Value of C	100	120	130	140	150
	0.713	1.00	1.16	1.33	1.57
lying					
Factor					

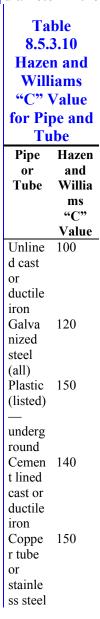
#### Notes:

- 1. This is based upon the friction loss through the fitting being independent of the *C* factor applicable to the piping.
- 2. Specific friction loss values or equivalent pipe lengths for alarm valves, dry-pipe valves, deluge valves, strainers, and other devices or fittings should be made available to the authority having jurisdiction.

#### 8.5.3\* Calculation Procedure.

- **8.5.3.1** Worksheets shall be provided to show the flow and pressure for all nozzles and junction points to the water supply.
- **8.5.3.2** A graph sheet shall be included with the calculations in accordance with 8.3.4.
- **8.5.3.3** The friction loss for all pipes, and devices such as valves, meters, and strainers, shall be included in the calculation.
- **8.5.3.4** A legend of the symbols used for all devices shall be included.
- **8.5.3.5** The loss of all fittings shall be calculated where a change in direction of the flow occurs, as follows:
  - (1) The loss for a tee or a cross shall be calculated where the flow direction change occurs, based upon the equivalent pipe length for the smaller size of the tee or cross in the path of the turn. Loss for that portion of the flow that passes straight through the run of a tee or a cross shall not be included.
  - (2) The loss of reducing elbows shall be calculated based upon the equivalent length value in feet of the smallest outlet.
  - (3) Friction loss shall be excluded for tapered reducers and for the fitting directly supplying the spray nozzle.

- **8.5.3.6** Elevation changes affecting the discharge or the total required pressure, or both, shall be included in the calculations at the point of occurrence.
- **8.5.3.7** The water allowance for hose stream(s), where served from the same supply, shall be added to the system requirement at the system connection to the supply main.
- **8.5.3.8** The total water requirements shall then be calculated to a known water supply reference point.
- **8.5.3.9** Orifice plates shall not be used for balancing the system.
- **8.5.3.10** Pipe friction loss shall be calculated in accordance with the Hazen and Williams formula, using "C" values as shown in Table 8.5.3.10, and using the actual internal pipe diameter in the formula.



```
Note: SI
units: 1
in. =
25.4
mm; 1 ft
= 0.305
m.
```

**8.5.3.11** Different "C" values shall be permitted to be used where required by the authority having jurisdiction.

# **Chapter 9 Water Supplies**

#### 9.1 General.

Every water spray system shall have at least one automatic water supply.

### 9.2 Volume and Pressure.

- **9.2.1** The water supplies shall be capable of providing the required flow and pressure for the required duration, including systems designed to operate simultaneously, as specified in Chapter 7.
- **9.2.2** For water supply distribution systems, an allowance for the flow rate of other fire protection water requirements shall be made in determining the total water supply requirement.

### 9.3 Acceptable Water Supply Systems.

- **9.3.1\*** Water for water spray systems shall be from one or more water supplies, such as the following:
  - (1) Connections to waterworks systems, in accordance with NFPA 24, Standard for the Installation of Private Fire Service Mains and Their Appurtenances
  - (2) Gravity tanks, in accordance with NFPA 22, Standard for Water Tanks for Private Fire Protection
  - (3) Fire pumps with adequate water supply, in accordance with NFPA 20, Standard for the Installation of Stationary Pumps for Fire Protection
  - (4) Pressure tanks, in accordance with NFPA 22, Standard for Water Tanks for Private Fire Protection, and NFPA 13, Standard for the Installation of Sprinkler Systems, sized per the hydraulically calculated method
- **9.3.2** Installation of underground private fire service mains connecting water spray systems to water supplies shall be in conformance with the applicable criteria of NFPA 13, *Standard for the Installation of Sprinkler Systems*.

# **Chapter 10 System Acceptance**

### 10.1\* Certification.

The contractor shall prepare and submit a set of as-built drawings and hydraulic calculations of the system, maintenance and instruction bulletins, and the applicable parts

of the contractor's material and test certificates covering material and tests certifying that the work has been completed and tested in accordance with plans and specifications.

### 10.2 Flushing of Pipe.

**10.2.1\* Supply Piping.** Underground mains and lead-in connections to system risers shall be flushed thoroughly before connection is made to system piping in order to remove foreign materials that might have entered the underground mains or connections during the course of the installation or that might have been present in existing piping. The minimum flow rate shall be at least that necessary to provide a velocity of 3 m/sec (10 ft/sec). (*See Table 10.2.1.*)

Table 10.2.1 Flow Required to Produce a Velocity of 3 m/sec (10 ft/sec) in Pipes

Pipe	Size	Flo	)W
mm	in.	L/min	gpm
100	4	1,476	390
150	6	3,331	880
200	8	5,905	1,560
250	10	9,235	2,440
300	12	13,323	3,520

- **10.2.2** Where the system cannot provide a velocity of 3 m/sec (10 ft/sec), then the supply piping shall be permitted to be flushed at the maximum flow rate available to the system under fire conditions.
- **10.2.3** The flushing operations for all systems shall be continued for a sufficient time to ensure thorough cleaning.
- **10.2.4** All system pipe shall be made free of debris that would inhibit system discharge.
- **10.2.5** Where flushing is not possible, cleanliness shall be determined by internal examination of all sections of pipe not flushed.

### 10.3 Hydrostatic Pressure Tests.

All new system piping shall be hydrostatically tested in accordance with the provisions of NFPA 13, *Standard for the Installation of Sprinkler Systems*.

### 10.4 Operating Tests.

**10.4.1 Performance.** Operation tests shall be conducted to ensure that the water spray system(s) will respond as designed, both automatically and manually.

#### 10.4.2\* Response Time.

- **10.4.2.1** Under test conditions, the heat detection system, where exposed to a heat source or pilot sprinkler line test valve opened, shall operate the system actuation valve within 40 seconds.
- **10.4.2.2** Under test conditions, the flammable gas detection system shall operate within the time frame specified in the system design.
- **10.4.2.3** All test times shall be recorded.

- 10.4.2.4 Response time for ultra high-speed water spray systems shall comply with 12.2.2.
- 10.4.3 Discharge Tests on Systems with Open Nozzles.
- **10.4.3.1** The water discharge patterns from all of the spray nozzles shall be observed to verify the following:
  - (1) Patterns are not impeded by plugging of the nozzles.
  - (2) Nozzles are properly positioned.
  - (3) Nozzle discharge patterns are not obstructed from wetting surfaces to be protected as designed.

### 10.4.3.2\* Pressure Readings.

- **10.4.3.2.1** Pressure readings shall be recorded at the hydraulically most remote nozzle to verify the water flow has not been impeded.
- **10.4.3.2.2** A second pressure reading shall be recorded at the system actuation valve to ensure the water supply is adequate.
- **10.4.3.2.3** Those readings shall be compared to the design criteria to determine that the system is operating as designed.
- **10.4.3.3** The time lapse between operation of the detection systems and water flow at the most remote water spray nozzle shall be recorded.
- 10.4.3.4 The time lapse for ultra high-speed water spray systems shall comply with 12.2.2.
- **10.4.4 Manual Operation.** Each manual actuation device shall be tested.
- **10.4.5 Multiple Systems.** The maximum number of systems that would be expected to operate in case of fire shall be tested simultaneously to determine the adequacy and condition of the water supply.

# **Chapter 11 System Maintenance**

#### 11.1 General.

11.1.1 A water spray system installed in accordance with this standard shall be properly maintained in accordance with NFPA 25, Standard for the Inspection, Testing, and Maintenance of Water-Based Fire Protection Systems, and NFPA 72, National Fire Alarm Code, to provide at least the same level of performance and protection as designed.

**11.1.2** The owner shall be responsible for conducting system maintenance and maintaining the system in operating condition.

# **Chapter 12 Ultra High-Speed Water Spray Systems**

### 12.1\* General.

- **12.1.1\*** Ultra high-speed water spray systems shall operate to be used for the extinguishment or control of deflagrations in open, unconfined areas or within process equipment.
- **12.1.2\*** Ultra high-speed water spray systems shall not be used for the extinguishment or control of detonations, or for the suppression of deflagrations in enclosed or confined vessels for purposes of limiting overpressurization.
- 12.1.3 Ultra high-speed water spray systems shall be permitted to be used to prevent a

deflagration from transitioning to a detonation.

**12.1.4 Design Guides.** Ultra high-speed water spray systems shall conform to the applicable requirements of the standards of the National Fire Protection Association listed in Chapter 2.

### 12.2 Response Time.

- **12.2.1** Response time shall be the time for system operation from the presentation of an energy source to the detector to flow of water from the water spray nozzle being tested.
- **12.2.2** Ultra high-speed water spray systems shall be designed to have a response time of not more than 100 milliseconds.
- **12.2.3** Faster response times than indicated in 12.2.2 shall be provided where required by the properties of the hazard being protected.
- **12.2.4** In order to meet the response time criteria, ultra high-speed water spray systems shall utilize water-filled piping.

### 12.3 Design Considerations.

### 12.3.1 System Types.

- **12.3.1.1\* Ultra High-Speed Local-Application Water Spray System.** Nozzle(s) shall be placed as close to the point of ignition as possible.
- **12.3.1.2\* Ultra High-Speed Area-Application Water Spray System.** Nozzles shall be spaced such that the minimum density is applied uniformly over the entire hazard area.
- **12.3.1.3\* Dual Application System.** A system that uses both the local- and area-application concepts shall be permitted.
- **12.3.1.4\* Personnel Protection.** Where protection of personnel is required, coverage by the ultra high-speed water spray system shall include locations where personnel are expected to be within the hazard area and their immediate means of egress.

### 12.3.2 Flow and Density.

- **12.3.2.1 Local Application.** The design shall produce a flow rate of not less than 95 L/min (25 gpm) per nozzle at the point of water application.
- **12.3.2.2** Where higher nozzle flow rates are required for local application based on test data or field information, the higher rates shall be used.
- **12.3.2.3\* Area Application.** The minimum design density shall be 2 (L/min)/m<sup>2</sup> (0.50 gpm/ft<sup>2</sup>) of area covered by ultra high-speed water spray.
- **12.3.2.4** Where higher nozzle flow rates are required for area applications based on test data or actual field information, the higher rates shall be used.

#### 12.3.3 Design Pressure.

- **12.3.3.1** Operating pressure at the hydraulically most remote nozzle shall be not less than 3.5 bar (50 psi).
- **12.3.3.2** Static pressure maintained on the system prior to system actuation shall be maintained at a pressure no less than 3.5 bar (50 psi).
- **12.3.3.3** For systems utilizing blow-off caps or rupture disks on the nozzles, the system

static pressure shall not exceed 75 percent of the rating of the lowest rated blow-off caps or rupture disks.

- **12.3.4\* System Volume Limitation.** No larger than a 1893 L (500 gal) system capacity shall be controlled by one system actuation valve.
- **12.3.4.1** System capacity shall be permitted to exceed 1893 L (500 gal) if the system design is such that the system response time required by 12.2.2 is met.

#### 12.3.5 Duration.

- **12.3.5.1** Systems shall have a duration of not less than 15 minutes.
- **12.3.5.2** Where the time for safe evacuation of personnel is longer than 15 minutes, the evacuation time shall be the required minimum system duration.
- **12.3.6 Fire Hose Connection.** Hose connections shall not be permitted to be supplied by the ultra high-speed water spray system.
- **12.3.7 System Operation.** Systems shall be designed to operate automatically with supplementary manual actuation means provided.

### 12.3.8 Discharge Delays.

- **12.3.8.1 Timers.** Timers or similar devices to delay system activation shall not be permitted.
- **12.3.8.2\* Water Supply.** The water supply pressure for a properly functioning ultra high-speed water spray system shall be maintained such that it is available at the time a system functions

### 12.3.9 Nozzle Placement.

- **12.3.9.1\*** Nozzles shall be located as close as practicable to the protected area or likely point, or points, of ignition.
- **12.3.9.2** Nozzles shall be positioned to provide complete water spray impingement for the protected area or likely point, or points, of ignition.
- **12.3.9.3** Local application systems requiring two or more nozzles shall have nozzles positioned in a counter-opposed fashion for the most efficient water spray coverage of the hazard and the most efficient distribution of water onto the hazard. (See Figure A.12.3.1.1.)
- **12.3.9.3.1** Nozzles shall be positioned in such a way that burning materials are not propelled toward personnel and so that personnel and material-in-process cannot impede or block water flow.
- **12.3.9.4** Nozzle locations that are subject to mechanical damage shall be suitably protected.

#### 12.3.10\* System Actuation Valves and Accessories.

- **12.3.10.1\*** System actuation valves and accessories shall be placed as close as practical to the water spray nozzles.
- **12.3.10.2** System actuation valves shall be accessible for maintenance and shall be protected from damage.

#### **12.3.11 Piping.**

- **12.3.11.1** Piping used in ultra high-speed water spray systems shall comply with the requirements of Chapter 5.
- **12.3.11.2** High pressure flexible hydraulic hose shall be permitted to be used to connect nozzles on local application systems when approved by the authority having jurisdiction.
- **12.3.11.3\*** All piping including wet pilot lines shall be sloped at a minimum of 25 mm per 3 m (1 in. per 10 ft) of pipe.
- **12.3.11.4** Air bleeder valves shall be placed at all piping high points to bleed air trapped in the system.
- **12.3.11.5** Piping shall be routed as directly as practical from the system actuation valve to the protected area or hazard with the fewest number of fittings and changes of direction.
- **12.3.12\* Pipe Support.** Piping shall be supported in accordance with the requirements of 6.3.2.

#### **12.3.13 Strainers.**

- 12.3.13.1\* Systems utilizing pilot-operated nozzles shall be equipped with strainers in the main waterway.
- **12.3.13.2** Pilot lines shall be equipped with a separate strainer capable of removing particles that are 75 percent of the flow orifice in the solenoid.

#### **12.3.14 Detection.**

- **12.3.14.1 General.** The detection systems shall be in accordance with NFPA 72, *National Fire Alarm Code*.
- **12.3.14.2** Sensing devices shall be as follows:
- (1) Response characteristics:
  - (a) Radiant energy sensing devices capable of sensing the expected wavelength emissions of the materials in combustion.
  - (b) Other types of sensing devices having equivalent response characteristics to radiant energy sensing devices shall be permitted to be used.
- (2) Protected from physical damage
- (3) Suitable for the electrical area classification where they are installed
- (4) Accessible for testing, cleaning, and maintenance
- (5) Aimed and adjusted to minimize false actuation

#### 12.3.14.3 Detection for Local Application.

- **12.3.14.3.1** One or more detectors shall be placed as close as physically possible to sources of ignition.
- **12.3.14.3.2** Detectors shall provide complete detection coverage for the likely point, or points, of ignition and shall not be blocked by shielding, equipment, or personnel.
- **12.3.14.4 Detection for Area Application.** One or more detectors shall be located to provide general coverage for the area occupied by operating personnel, including egress routes and other possible sources of ignition within the space.

### 12.3.15 Control Panel.

- **12.3.15.1** The control panel shall conform to the requirements of NFPA 72, *National Fire Alarm Code*.
- **12.3.15.2** The control panel shall be located in an area protected from physical injury and from electromagnetic energy emitted from other electrical devices that could induce false actuation.
- **12.3.15.3** Control panel enclosures shall be rated for the ambient environment where they are located.
- **12.3.16 Wiring.** Wiring shall be in compliance with NFPA 70, *National Electrical Code*, and NFPA 72, *National Fire Alarm Code*, in addition to the following requirements:
  - (1) Circuits between initiating or actuating devices and their controllers shall be shielded.
  - (2) All wiring between the initiating or actuating devices and the control panel shall be continuous with no splices.

### 12.4\* System Acceptance.

The performance of the system shall be tested to verify that the response time criteria in Section 12.2 will be met and that each nozzle provides the correct coverage and flow rate.

### 12.5 Testing and Maintenance.

Ultra high-speed water spray systems shall be maintained in accordance with NFPA 25, Standard for the Inspection, Testing, and Maintenance of Water-Based Fire Protection Systems, and NFPA 72, National Fire Alarm Code.

- **12.5.1\*** A maintenance program in addition to the requirements of NFPA 25, *Standard for the Inspection, Testing, and Maintenance of Water-Based Fire Protection Systems*, and NFPA 72, *National Fire Alarm Code*, shall be established.
- **12.5.2** Systems not in use shall not be required to be periodically tested.
- **12.5.3** Systems not in use shall be tested when put back into service.
- **12.5.4** Records of the tests shall be kept on file at the facility.
- **12.5.5** The following tests shall be conducted in addition to the requirements of NFPA 25, Standard for the Inspection, Testing, and Maintenance of Water-Based Fire Protection Systems, and NFPA 72, National Fire Alarm Code.
- **12.5.6** The following shall be completed in addition to any of the requirements of Section 12.5:
  - (1) A full operational flow test shall be conducted at intervals not to exceed 1 year, including measurement of response time. The results of tests shall be retained on file for the life of the system. (See A.12.4 for suggested time testing procedures.)
  - (2) Detectors shall be tested and inspected for physical damage and accumulation of deposits on the lenses at least monthly.
  - (3) Controllers shall be checked at the start of each shift for any faults.
  - (4) Valves on the water supply line shall be checked at the start of each shift to ensure they are open.

- (5) Valves secured in the open position with a locking device or monitored by a signaling device that will sound a trouble signal at the deluge system control panel or other central location shall not be required to be checked.
- **12.5.7** Response time testing shall be conducted where required by other sections of this standard.

# **Annex A Explanatory Material**

Annex A is not a part of the requirements of this NFPA document but is included for informational purposes only. This annex contains explanatory material, numbered to correspond with the applicable text paragraphs.

**A.1.1.2** Waterspray systems can be independent of, or supplementary to, other forms of protection.

The design of specific systems can vary considerably, depending on the nature of the hazard and the basic purposes of protection. Because of these variations and the wide choice in the characteristics of spray nozzles, these systems shall be competently designed, installed, and maintained. It shall be essential that their limitations as well as their capabilities be thoroughly understood by the designer.

**A.1.1.3** For information on these applications refer to the following:

NFPA 13, Standard for the Installation of Sprinkler Systems

NFPA 14, Standard for the Installation of Standpipe, Private Hydrant, and Hose Systems

NFPA 69, Standard on Explosion Prevention Systems

NFPA 750, Standard on Water Mist Fire Protection Systems

NFPA 1964, Standard for Spray Nozzles (Shutoff and Tip)

**A.3.2.1 Approved.** The National Fire Protection Association does not approve, inspect, or certify any installations, procedures, equipment, or materials; nor does it approve or evaluate testing laboratories. In determining the acceptability of installations, procedures, equipment, or materials, the authority having jurisdiction may base acceptance on compliance with NFPA or other appropriate standards. In the absence of such standards, said authority may require evidence of proper installation, procedure, or use. The authority having jurisdiction may also refer to the listings or labeling practices of an organization that is concerned with product evaluations and is thus in a position to determine compliance with appropriate standards for the current production of listed items.

**A.3.2.2 Authority Having Jurisdiction.** The phrase "authority having jurisdiction" is used in NFPA documents in a broad manner, since jurisdictions and approval agencies vary, as do their responsibilities. Where public safety is primary, the authority having jurisdiction may be a federal, state, local, or other regional department or individual such as a fire chief; fire marshal; chief of a fire prevention bureau, labor department, or health department; building official; electrical inspector; or others having statutory authority. For insurance purposes, an insurance inspection department, rating bureau, or other insurance company representative may be the authority having jurisdiction. In many circumstances, the property owner or his or her designated agent assumes the role of the authority having

jurisdiction; at government installations, the commanding officer or departmental official may be the authority having jurisdiction.

**A.3.2.3 Listed.** The means for identifying listed equipment may vary for each organization concerned with product evaluation; some organizations do not recognize equipment as listed unless it is also labeled. The authority having jurisdiction should utilize the system employed by the listing organization to identify a listed product.

**A.3.3.10 Fire Area.** The physical separations also include diking and special drainage systems.

#### **A.3.3.13.1 Insulated.**

- (1) Noncombustible materials affording 2-hour fire ratings under NFPA 251, Standard Methods of Tests of Fire Endurance of Building Construction and Materials, will usually satisfy the requirements of Chapter 3 when properly fastened and weather protected.
- (2) For equipment, structures, and vessels of nonferrous metals, somewhat lower temperature limits than indicated in Chapter 3 may be required, based upon reliable metallurgical data.
- **A.3.3.15 Nonabsorbing Ground.** Most soils are not considered sufficiently permeable or absorbent to be considered absorbing ground. Paving, such as concrete or asphalt, is considered nonabsorbing.
- **A.3.3.21.2 Open Water Spray Nozzle.** A water spray nozzle is usually a discharge device with an open waterway. However, it is possible for nozzles to be equipped with operating elements such as fusible links or glass bulbs for special applications.
- **A.3.3.22 Water Spray System.** Automatic systems can be actuated by separate detection equipment installed in the same area as the water spray nozzles or by the water spray nozzles using an operating element. In some cases the automatic detection can also be located in another area.
- **A.3.3.23 Water Wastage.** Some causes of wastage are wind velocity and sometimes the overcarry of discharge pattern beyond the targeted surface.
- **A.4.1** The design objectives are as follows:
- (1) Extinguishment of fire by water spray is accomplished by cooling, smothering from produced steam, emulsification of some liquids, dilution in some cases, or a combination of these factors.
- (2) Control of fires is accomplished by an application of water spray to the burning materials producing controlled burning. The principle of control may be applied where combustible materials are not susceptible to complete extinguishment by water spray or where complete extinguishment is not considered desirable.
- (3) Effective exposure protection is accomplished by application of water spray directly to the exposed structures or equipment to remove or reduce the heat transferred to them from the exposing fire. Water spray curtains are less effective than direct application but can, under favorable conditions, provide some protection against fire exposure through subdivision of fire areas. Unfavorable conditions can include such factors as windage, thermal updrafts, and inadequate drainage.

(4) Start of fire is prevented by the use of water sprays to dissolve, dilute, disperse, or cool flammable materials or to reduce flammable vapor concentrations below the lower flammable limit (LFL).

**A.4.2.3** See NFPA 49, *Hazardous Chemicals Data*, and NFPA 325, *Guide to Fire Hazard Properties of Flammable Liquids, Gases, and Volatile Solids*. (Note: Although NFPA 49, 325, and 491 have been officially withdrawn from the *National Fire Codes*®, the information is still available in NFPA's *Fire Protection Guide to Hazardous Materials*.) **A.4.2.5** *Water Reactive Materials*. In special cases, where adequate safeguards have been provided, water spray systems for the protection of structures, equipment, or personnel in the presence of such materials as described in 4.2.5 might be acceptable.

**A.4.3** Water spray system installation is a specialized field that is a trade in itself.

**A.4.4.1** The rapid removal of spills and fire protection water from the area protected by a water spray system can greatly reduce the amount of fuel involved in a fire. In addition, if water discharge is not controlled, hydrocarbons or other liquid fuels may spread into adjacent areas and increase the size of the fire, exposing additional property and making the fire more difficult to control or extinguish.

An example of a protected hazard that may not require a system for controlling or containing water spray discharge would be a rubber belt conveyor located in an aboveground conveyor housing.

**A.4.4.3** Each of the methods listed has advantages and disadvantages. In most cases, a combination of methods should be used in designing an effective control or containment system.

The characteristics of any hazardous materials in the protected area should be considered in the design of a control or containment system, including volume, solubility in water, flammability, reactivity, environmental concerns (e.g., toxicity), and vapor pressure at ambient and normal processing conditions. For example, particular attention should be given to the removal of burning flammable liquids away from process vessels containing reactive materials sensitive to heat.

Curbing, along with appropriate grading, can be of significant benefit in preventing water or burning liquid from spreading horizontally into adjacent areas. Grading should ideally be sloped at a pitch not less than one percent away from critical equipment and toward drains, trenches, ditches, or other safe area. Concrete surfacing is most desirable, but other hard surfacing or crushed rock or equivalent is suitable.

Process areas and buildings handling hydrocarbons or hazardous chemicals normally have a closed drain system to capture leaks, spills, normal drainage, wash down, and so forth. In some cases, it may not be practical to design the closed drain system to accommodate the full flow from the fire protection systems. Additionally, even where designed with adequate capacity, floor drains will often become clogged with debris during a fire. The excess that cannot be carried off by the closed drain system will then overflow to the surface drainage systems, which might include storm sewers, open ditches, streets, or similar features. The proper design of area drainage should anticipate where the excess will flow so that it may be safely routed and controlled.

See NFPA 30, *Flammable and Combustible Liquids Code*, for diking requirements for the tank storage of flammable and combustible liquids.

Diking is not a desirable means of containing water spray discharge where buildings, process structures, or important equipment are being protected from exposure to flammable or combustible liquids.

**A.4.4.4** Underground or enclosed drains are preferred over open trenches since enclosed drains provide a method of removing spilled liquids from the area without exposing equipment to burning liquids. Further, trenches can act as collection points for heavier-than-air vapors. If used, trenches should be routed in a way that will not carry fire protection water and burning liquids through another fire area. If unavoidable, fire stops (weirs) should be provided in the trench system between the fire areas. Trenches should be twice as wide as deep, and in no case should the depth exceed the width. Trenches should be provided with covers that are one-third open grating and two-

thirds solid plate or concrete. (See Figure A.4.4.4.)

Steel plate spot welded to grating

x" 2x"

Drainage trench with steel plate and grating cover

FIGURE A.4.4.4 Drainage trench detail.

Drains should be in sufficient number such that the required runoff is handled without formation of significant pools.

**A.4.4.7(1)** The actual flow rate may be determined by plotting the demand curve (fixed water supply systems) and the water supply curve on semi-exponential (N<sup>1.85</sup>) graph paper. The intersection of the demand curve and the supply curve provides a realistic estimate of the actual flow rate that would be anticipated.

**A.4.4.7(5)** Judgment should be used in determining the chance of having a major fire simultaneous with a heavy rainfall. For areas experiencing little rainfall, drainage calculations can ignore rainfall. For areas experiencing frequent rainfall, a flow rate from rainfall may or may not be warranted, depending on the hazards being protected and other factors. If included, a rainfall rate less than the highest anticipated would ordinarily be used, as it is not likely that the maximum fire and rainfall demands would occur simultaneously. The effect of rainfall on the size of any areas designed to contain runoff should also be considered.

**A.4.4.8** It is desirable to contain runoff for the anticipated duration of any fire. However, in large chemical or petrochemical facilities, a major fire can last for 8 hours or more, resulting in extremely large holding basins or retention ponds. Where the anticipated incident duration results in retention basins that are of impractical size, methods to limit the duration of runoff may be required.

When an extended duration is anticipated, a duration of 4 hours is usually considered the practical maximum. During that time it is often possible to isolate equipment and reduce the flow rate of water and other materials so that the continuous discharge flow rate is less than the initial flow rate. If a significant amount of flammable materials can be removed from the protected area, it may be possible to shut down water spray systems and manually fight the fire, greatly reducing the amount of material that needs to be contained.

Smaller facilities with limited holdups may not require as long a duration. For example, if the exposing fire is caused by a spill of 1893 L (500 gal) or less, with good drainage and containment systems, the anticipated duration may be as little as 30 minutes to 1 hour. In special circumstances (e.g., involving prompt manual response), an anticipated duration less than 30 minutes would be acceptable.

Finally, other standards and regulations may dictate the amount of containment required. For example, NFPA 30, *Flammable and Combustible Liquids Code*, contains requirements for warehouses and other areas containing flammable liquids. Also, local environmental regulations and building codes might contain criteria for duration and amount of material to be collected.

**A.5.2.3.3** Painting of spray nozzles can retard the thermal response of the heat-responsive element, can interfere with the free movement of parts, and can render the spray nozzle inoperative. Moreover, painting can invite the application of subsequent coatings, thus increasing the possibility of altering the discharge pattern for all types of nozzles.

**A.5.2.5** The stock of spare automatic water spray nozzles and pilot sprinklers should take into consideration the intended system performance, the criticality of the operations, and the down time associated with system impairment after damage or fire. Automatic water spray nozzles could have long lead times, delaying replacement of large numbers of nozzles for several weeks.

**A.5.3.2** See Table A.5.3.2.

**Table A.5.3.2 Steel Pipe Dimensions** 

		Table 14.5.0.2 Seed Tipe Difficultions												
Nominal Pipe Size (in.)			Schedule 10 <sup>1</sup>						Schedule 30					
Outside Diameter				Inside Diameter		Wall Thickness		Inside Diameter		Wall Thickne ss				
mm	in.	_	n	in.		n	in.		m	in.	-	n	in.	-
			m			m			m			n		
1	33.4	1.315		27.9	1.097		2.8	0.109					_	
1 1/4	42.2	1.660		36.6	1.442		2.8	0.109					_	
1 ½	48.3	1.900		42.7	1.682		2.8	0.109					_	
2	60.3	2.375		54.8	2.157		2.8	0.109					_	
2 ½	73.0	2.875		66.9	2.635		3.0	0.120						
3	88.9	3.500		82.8	3.260		3.0	0.120						
3 ½	101.6	4.000		95.5	3.760		3.0	0.120					_	
4	114.3	4.500		108.2	4.260		3.0	0.120						
5	141.3	5.563		134.5	5.295		3.4	0.134						
6	168.3	6.625		161.5	6.357		3.4	$0.134^{2}$		_				
8	219.1	8.625		209.5	8.249		4.8	$0.188^{2}$		205.0	8.071		7.0	0.277
10	273.1	10.75		263.4	10.37		4.8	$0.188^{2}$		257.6	10.14		7.8	0.307

<sup>1</sup>Schedule 10 defined to 127 mm (5 in.) nominal pipe size by ASTM A 135, *Standard Specification for Electric*<sup>2</sup>Wall thickness specified in 5.3.2.

**A.5.3.5** Other types of pipe and tube that have been investigated and listed for water spray applications include lightweight steel pipe. While these products can offer advantages, such as ease of handling and installation, cost-effectiveness, and reduction of friction losses, it is

important to recognize that they also have limitations that are to be considered by those contemplating their use or acceptance.

Corrosion studies for lightweight steel pipe have shown that, in comparison to Schedule 40 pipe, its effective life might be reduced, with the level of reduction being related to its wall thickness. Further information with respect to corrosion resistance is contained in the individual listings of such products.

The investigation of pipe and tube other than described in Table 5.3.1 should involve consideration of many factors, including the following:

- (1) Pressure rating
- (2) Beam strength (hangers and spacing)
- (3) Unsupported vertical stability
- (4) Movement during system operation (affecting water distribution)
- (5) Corrosion (internal and external), chemical and electrolytic
- (6) Resistance to failure where exposed to elevated temperatures
- (7) Methods of joining (strength, permanence, fire hazard)
- (8) Physical characteristics related to integrity during earthquakes
- (9) Resistance to mechanical and, where applicable, explosion damage
- (10) Susceptibility to degradation due to environmental exposure (i.e., ultraviolet degradation and low temperatures, etc.)

**A.5.4.10** Rubber-gasketed pipe fittings and couplings should not be installed where ambient temperatures can be expected to exceed 66°C (150°F) unless listed for this service. If the manufacturer further limits a given gasket compound, those recommendations should be followed.

**A.5.5.1.2** Some steel piping material having lesser wall thickness than specified in 5.5.1.2 has been listed for use in water spray systems when joined with threaded connections. The service life of such products can be significantly less than that of Schedule 40 steel pipe, and it should be determined if this service life will be sufficient for the application intended.

All such threads should be checked by the installer using working ring gauges conforming to the Table 8, Basic Dimensions of Ring Gauges for USA (American) Standard Taper Pipe Threads, NPT, in accordance with ANSI/ASME B1.20.1, *Pipe Threads, General Purpose*, 1983.

**A.5.5.2** See Figure A.5.5.2(a) and Figure A.5.5.2(b).

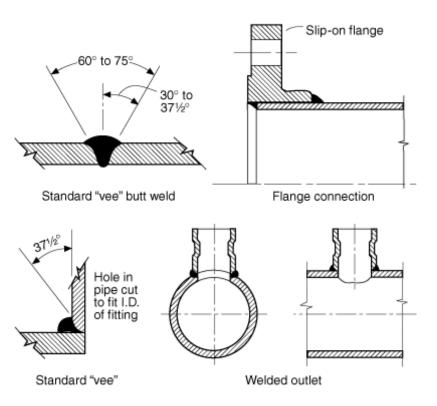


FIGURE A.5.5.2(a) Acceptable weld joints.

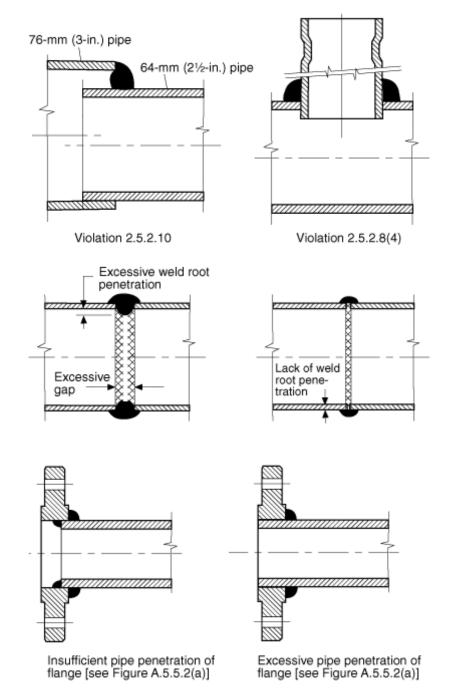


FIGURE A.5.5.2(b) Unacceptable weld joints.

A.5.5.2.8(1) Listed, shaped, contoured nipples meet the definition of fabricated fittings.

**A.5.5.4** The fire hazard of the brazing process should be suitably safeguarded.

**A.5.7.2.1** These valves include, but are not limited to, deluge valves, alarm check valves, preaction valves, and high-speed valves.

**A.5.7.2.2** Accessories can include any one of or a combination of the following:

(1) Manual emergency stations

- (2) Flammable gas detectors
- (3) Smoke detectors
- (4) Heat detectors
- (5) Fire detectors
- (6) Control panels

Where installing wet pilot systems, special attention should be given to height limitations above the system actuation valve due to concern of water column. Refer to manufacturer's information and listing.

**A.5.7.2.3** Manual means of actuation can include pneumatic, hydraulic, electrical, mechanical, or any combination thereof.

**A.5.9.1** The strainer should be capable of continued operation without serious increase in head loss for a period estimated to be ample when considering the type of protection provided, the condition of the water, and similar local circumstances.

**A.5.11.3** All alarm apparatus should be located and installed such that all parts are accessible for inspection, removal, and repair and should be adequately supported.

**A.6.1.2** The minimum clearances listed in Table 6.1.2.2 are for the purpose of electrical clearance under normal conditions; they are not intended for use as "safe" distances during fixed water spray system operation.

The clearances are based upon minimum general practices related to design basic insulation level (BIL) values. To coordinate the required clearance with the electrical design, the design BIL of the equipment being protected should be used as a basis, although this is not material at nominal line voltages of 161 kV or less.

Up to electrical system voltages of 161 kV, the design BIL kV and corresponding minimum clearances, phase to ground, have been established through long usage.

At voltages higher than 161 kV, uniformity in the relationship between design BIL kV and the various electrical system voltages has not been established in practice. For these higher system voltages, it has become common practice to use BIL levels dependent on the degree of protection that is to be obtained. For example, in 230 kV systems, BILs of 1050, 900, 825, 750, and 650 kV have been utilized.

Required clearance to ground may also be affected by switching surge duty, a power system design factor that along with BIL should correlate with selected minimum clearances. Electrical design engineers may be able to furnish clearances dictated by switching surge duty. Table 6.1.2.2 deals only with clearances required by design BIL. The selected clearance to ground should satisfy the greater of switching surge or BIL duty, rather than to be based upon nominal voltage.

Possible design variations in the clearance required at higher voltages are evident in the table, where a range of BIL values is indicated opposite the various voltages in the high voltage portion of the table. However, the clearance between uninsulated energized parts of the electrical system equipment and any portion of the water spray system should not be

less than the minimum clearance provided elsewhere for electrical system insulation on any individual component.

**A.6.2.1** Water spray systems are usually applied to special fire protection problems beyond the capability of a standard sprinkler system. They are specifically designed for fire control, extinguishment, prevention, or exposure protection. These systems typically require that the water be applied rapidly to all protected surfaces at the same time, an objective that may not be possible with closed nozzles. In addition, to protect specific surfaces, the use of special nozzles with directional discharge is employed. The placement of these nozzles to provide proper coverage is often in conflict with the required placement to ensure prompt operation where automatic nozzles are used. Thus, the standard contemplates that open nozzles will normally be employed and that a separate detection system will be used to actuate the system.

There are cases, however, where it is desirable to use closed nozzles to limit the discharge of water to prevent equipment damage (such as when water spray is used to protect turbine bearings), or there are environmental concerns. Automatic nozzles should only be used where open nozzles present such problems and the position of the nozzles can meet both the coverage and response time design objectives.

A.6.3.2.2.1 See Figure A.6.3.2.2.1.

TYPICAL ARRANGEMENT OF SUPPORT LEGS

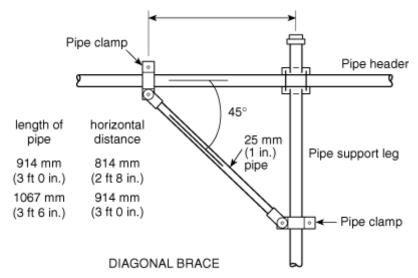
Note: Avoid obstructing door swing when locating support legs.

4.6 m (15 ft)

Maximum

Supply

FIGURE A.6.3.2.2.1 Typical arrangement of support legs for pipe stands. A.6.3.2.2.2 See Figure A.6.3.2.2.2.



Note: When using diagonal braces as supports, the maximum dimension between support legs can be exceeded by one-half the total horizontal distance of the diagonal braces.

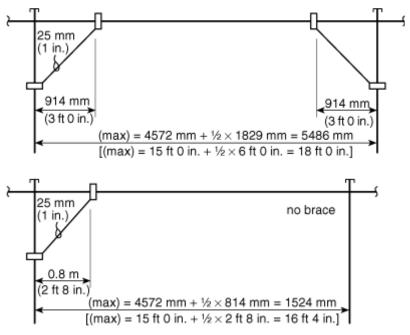
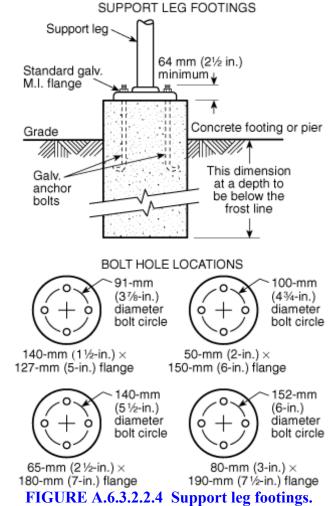
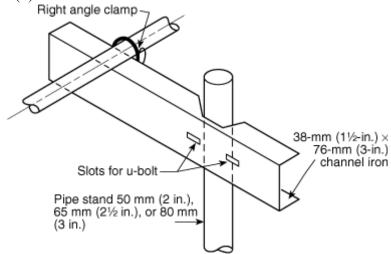


FIGURE A.6.3.2.2.2 Sway/support brace.

**A.6.3.2.2.4** See Figure A.6.3.2.2.4.

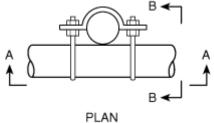


**A.6.3.2.2.5** See Figure A.6.3.2.2.5(a), Figure A.6.3.2.2.5(b), Figure A.6.3.2.2.5(c), and Figure A.6.3.2.2.5(d).



Note: Pipe stand brackets are now replacing the old style pipe stand without the bracket. The bracket makes installation easier and allows for adjustment horizontally and vertically. The standard bracket is made to fit 50-mm (2-in.), 65-mm (2½-in.), or 80-mm (3-in.) pipe stands.

# FIGURE A.6.3.2.2.5(a) Typical pipe stand bracket.



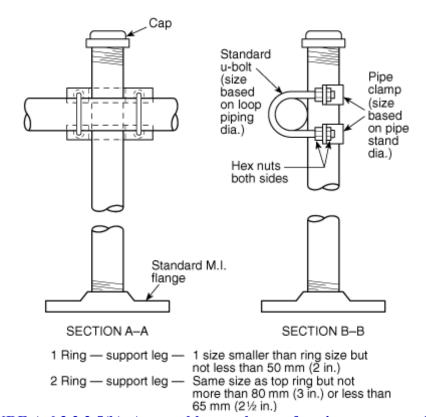


FIGURE A.6.3.2.2.5(b) Acceptable attachment for pipe to support legs.

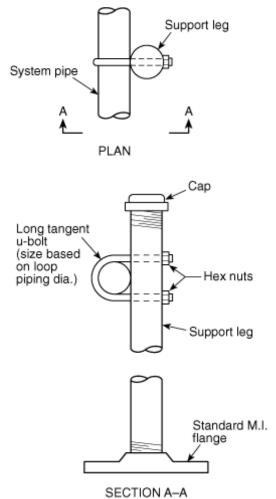


FIGURE A.6.3.2.2.5(c) Acceptable attachment for pipe to support legs.

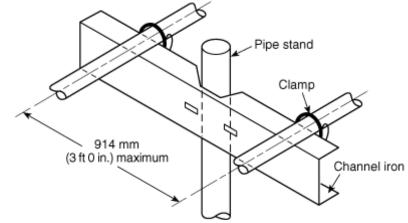


FIGURE A.6.3.2.2.5(d) Multiple pipes supported by one pipe stand.

**A.6.3.2.6** In cases where the piping cannot be supported by structural members, piping arrangements that are essentially self-supporting are often employed together with such hangers as are necessary.

**A.6.3.2.7** The performance of piping support systems should consider expansion and contraction due to temperature change, expansion due to internal water pressure (thrust),

restrained and/or unrestrained joints or pipe runs, heavy point loads (e.g., valves), and pipe deflection (span/support spacing). Manufacturer's installation instructions and engineering design guides should be consulted.

**A.6.3.3.6** See Figure A.6.3.3.6.

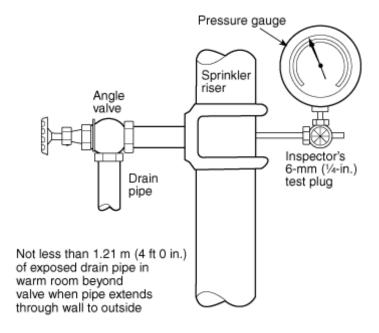


FIGURE A.6.3.3.6 Drain connection for system riser.

**A.6.3.6** Areas considered to have an explosion potential may include those having the following characteristics:

- (1) Highly exothermic reactions that are relatively difficult to control, such as nitration, oxidation, halogenation, hydrogenation, alkylation, or polymerization
- (2) Flammable liquids or gases where a flammable vapor or release of more than 10 tons in a 5-minute time period is possible
- (3) Other particularly hazardous operations where an explosion hazard may exist To limit the potential for explosion damage, the following guidelines should be used:
  - (1) System actuation valves should be remotely located [at least 15.2 m (50 ft)] from the area to be protected, housed within a blast resistant valve house or behind a blast wall designed for at least a gauge pressure of 20.7 kPa (3 psi) static overpressure.
  - (2) Piping should be located underground wherever possible. Risers should rise aboveground behind a protecting steel column or other structural element. Other piping should be located behind structural elements providing shielding from explosion overpressures and flying debris.
  - (3) The number of system actuation valves manifolded together should be limited to no more than three.
  - (4) Fire water mains should be buried, and accessible post indicator isolation valves

should be provided.

(5) All water spray piping 63 mm ( $2\frac{1}{2}$  in.) or larger should be of the welded-flanged type and as shown in Figure A.6.3.6.

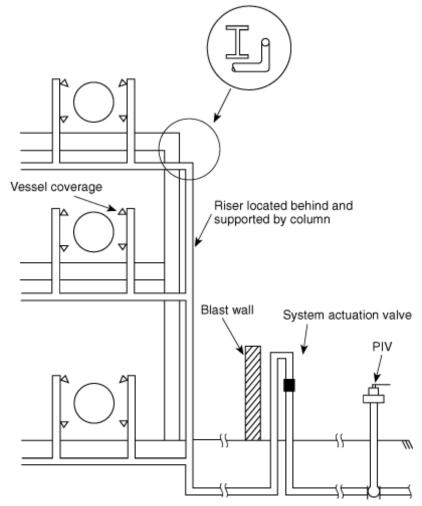


FIGURE A.6.3.6 Explosion protection of water spray or piping (elevation).

**A.6.4.3** Fire Department Connections. Suitable suction provisions can entail the following:

- (1) Suitable suction hydrants accessible to apparatus on primary or auxiliary supplies, or both
- (2) Suitable all-weather landings or locations where pumper apparatus can take suction at surface water supplies

**A.6.4.3.1** Fire department connections should be located and arranged so that hose lines can be readily and conveniently attached without interference from nearby objects including buildings, fences, posts, or other fire department connections. Where a hydrant is not available, other water supply sources such as a natural body of water, a tank, or a reservoir should be utilized. The water authority should be consulted when a nonpotable water supply is proposed as a suction source for the fire department.

See Figure A.6.4.3.1.

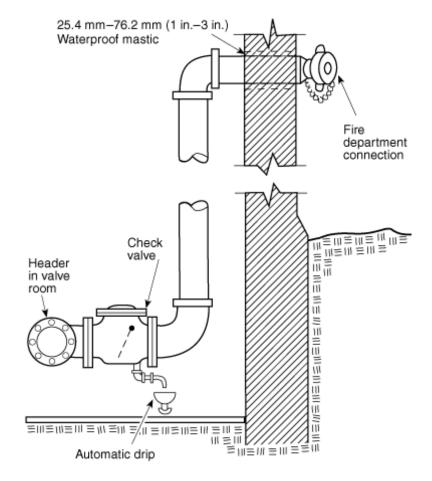


FIGURE A.6.4.3.1 Fire department connection.

**A.6.4.6.1** Care should be taken in the selection of strainers, particularly where nozzle waterways are less than 6.5 mm (½ in.) in dimension. Consideration should be given to the size of screen perforation, the volume available for accumulation without excessive friction loss, and the facility for inspection and cleaning.

**A.6.5.1.3** Consideration should be given to the protection of the detection system in areas subject to earthquake damage.

**A.6.5.2.3** Where detectors are located outdoors or without a ceiling over them to trap the heat, their spacing should be reduced if prompt detection is to be achieved. In general, thermal detectors are to be located within the hot air currents created by the fire if they are to operate. A 50-percent reduction in the spacing between detectors is required in the absence of test data on a particular detector and fire size. Some guidance might be available from the manufacturer. The sensitivity of other detectors (e.g., flammable gas detectors) can also be adversely affected by wind or the lack of walls or ceilings surrounding the hazard.

Heat collectors located above the pilot sprinklers or other thermal detectors for the sole purpose of trapping heat are not recommended, they are considered protected canopies (*see* 6.5.1.2). They can provide some benefit if they are of sufficient size [457 mm  $\times$  457 mm (18 in.  $\times$  18 in.), or larger] to trap heat. Smaller collectors can reduce sensitivity by causing a "dead" air space. However, shields or canopies needed to protect the detector from the

weather should not be eliminated because of concerns they might reduce detector sensitivity.

Other types of detectors such as UV detectors that do not rely on air currents to detect a fire or hazardous condition might not require a reduced spacing when used outdoors.

**A.6.5.2.7** Use of flammable gas detectors should consider the following:

- (1) *Calibration*. Automatic flammable gas detection equipment should be calibrated for the specific flammable gas to be detected.
- (2) Operation Alarms. Flammable gas detectors typically are equipped with two independently adjustable alarms for detection of flammable gas. Each unit should be equipped with a visual indication of alarm points, unit malfunction, and normal operation. Typically, the first alarm point is set between 10 percent and 25 percent of the LFL, and the second alarm point trips the water spray system between 25 percent and 65 percent of the LFL. Where the analyzers alarm in a continuously manned location, remote manual operation of the water spray system from a continuously manned location is sometimes utilized with the flammable gas analyzers alarming only in lieu of the automatic trip arrangement.
- (3) *Inadvertent Activation*. A reduction in the potential to inadvertently activate a system can be attained by designing cross-zone activation into the system. With a cross-zone activation scheme, the activation of a water spray system is triggered by the "high" alarm condition of any two or more detectors comprising the system.
- (4) Wiring. Flammable gas detectors should not be wired in series.
- (5) *Multiple Channel Systems*. Where a multiple channel flammable gas detector system is utilized, continuous, instantaneous analysis should be provided on all channels and an alarm or trip should be indicated immediately at the analyzer. No more than one water spray system should be actuated by a single multiple channel analyzer.
- **A.7.1.6** Prompt operation of the water spray system is needed to meet the design objectives. In most installations, the delivery of effective water spray from all open nozzles should take place within 30 seconds after detection. This may be accomplished by the remote starting of fire pumps. The use of devices such as timers would delay system actuation and negatively affect the system's intended performance.
- **A.7.1.10.1** Single systems should be designed to limit flow rates as small as practicable, with consideration given to the water supplies and other factors affecting reliability of the protection. Large system size may decrease system reliability and increase transfer time, water wastage, and environmental impact. Large systems should generally be limited to a discharge rate of 2500 gpm to 3000 gpm (9463 L/min to 11,355 L/min).
- **A.7.1.10.2** *Volume and Pressure.* For large areas protected by many adjacent systems, it may not be necessary to base the design flow rate on all systems operating simultaneously. Provided that floor drainage is sloped and sectionalized to reduce the flow of flammables to adjacent areas and assuming that detection systems are carefully designed, the maximum design flow rate could be determined by adding the flow rate for any system to the flow

rates for all immediately adjacent systems. (See example in Table A.7.1.10.2(a) and Table A.7.1.10.2(b).) The largest sum determined from considering all logical combinations should be used. This maximum anticipated flow rate basis is valid when the systems selected are judged to represent the worst case situation. Assuming that the above conditions are met, some fires involving several adjacent water spray systems could be adequately controlled with fewer systems operating. Careful engineering judgment should be used in the determination and calculation of the actuation, capacity, and duration of adjacent water spray systems.

Table A.7.1.10.2(a) Determining Design Flow Rate for Multiple Water Spray

_		System 1		System 2		System 3	_	System 4	_	Sy
	Flow	1800	6813	2100	7949	1950	7381	2300	8706	
		gpm	L/min	gpm	L/min	gpm	L/min	gpm	L/min	
	Pressure	80 psi	3.8 kPa	95 psi	4.6 kPa	105 psi	5.0 kPa	100 psi	4.8 kPa	

Note: Flow and pressure are required at the point of supply (other common hydraulic p

Table A.7.1.10.2(b) Determining Design Flow Rate for Combined System, Flow Balance

	Flow			Flow			Flow		
System	stem L/min gpm		System	L/min gpm		System	L/min	gpm	
1	7805	2062	2	8357	2208	3	7381	1950	
2	8357	2208	3	7381	1950	4	8921	2357	
3	7381	1950	4	8921	2357	5	9811	2592	
Total	23,542	6220	Total	24,659	6515	Total	26,113	6899	

Notes:

- 1. The combination of Systems 3, 4, and 5 creates the largest flow at the highest pressure at the point of supply (or other comm flow rate for this installation is selected as 6899 gpm at 105 psi (26,113 L/min at 5.0 kPa). Total water demand would be 689 hose stream application.
- 2. Systems shall be permitted to be combined in a logical manner such that systems that can be expected to be involved in the s simultaneously are combined to determine the design flow rate.

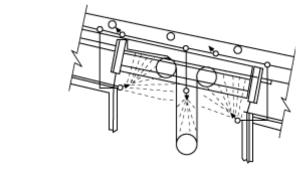
#### **A.7.2.1.2** The following are extinguishment methods:

- (1) Surface Cooling. Where extinguishment by surface cooling is contemplated, the design provides for complete water spray coverage over the entire surface. Surface cooling is not effective on gaseous products or flammable liquids and is not generally satisfactory for combustible liquids having flash points below 60°C (140°F).
- (2) Smothering by Steam Produced. Where this effect is contemplated, the intensity of the expected fire should be sufficient to generate adequate steam from the applied water spray and conditions should be otherwise favorable for the smothering effect. The water spray is to be applied to essentially all the areas of expected fire. This effect should not be contemplated where the material protected could generate oxygen when heated.
- (3) *Emulsification*. This effect should be contemplated only for liquids not miscible with water. The water spray should be applied over the entire area of flammable liquids. For those liquids having low viscosities, the coverage should be uniform

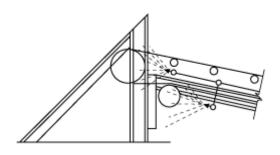
- and the minimum rate required should be applied with the nozzle pressure not less than the minimum on which approval is based. For more viscous materials, the coverage should be complete but need not be so uniform and the unit rate of application may be lower. A water additive that reduces the surface tension of water may be considered where the effect of emulsification is contemplated.
- (4) *Dilution*. Where extinguishment by dilution is contemplated, the material should be miscible with water. The application rate should be adequate to effect extinguishment within the required period of time based upon the expected volume of material and the percentage of dilution necessary to render the liquid nonflammable, but not less than that required for control and cooling purposes.
- (5) Other Factors. The system design may contemplate other extinguishing factors, such as a continuous film of water over the surface where the material is not miscible with water and has a density much greater than 1.0 (such as asphalt, tar, carbon disulfide, and some nitrocellulose solutions). Water spray may also be used on some materials to produce extinguishment as a result of rapid cooling below the temperature at which the material will decompose chemically at a self-sustaining rate.

For further information on the effect of droplet size, refer to *Engineering Criteria for Water Mist Fire Suppression Systems*, J. R. Mawhinney, P.E., presented at the Water Mist Fire Suppression Workshop at NIST.

- **A.7.2.1.3** *Design Density*. Limited test data exists that documents the minimum water application rates needed for extinguishment of certain combustibles or flammables. Much additional test work is needed before minimum rates can be established for all materials.
- **A.7.2.2.1** For this example it is intended that the insulation or tubing is subject to ignition and propagation of fire.
- **A.7.2.2.3** Interlocks should be provided between the fire detection system and the electrical systems to de-energize all power circuits that are not connected to critical processes.
- **A.7.2.3.2** For further information on conveyor belt roller protection, see Figure A.7.2.3.2.



Elevation of typical take-up roller protection



Elevation of typical end roller protection

FIGURE A.7.2.3.2 Typical roller protection.

**A.7.2.3.3.1** For further information on typical conveyor belt protection, including return belt, see Figure A.7.2.3.3.1(a) and Figure A.7.2.3.3.1(b).

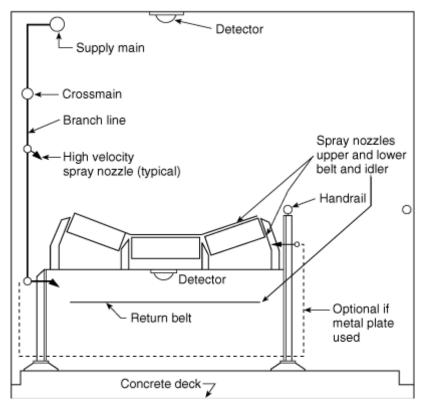


FIGURE A.7.2.3.3.1(a) Typical conveyor belt protection.

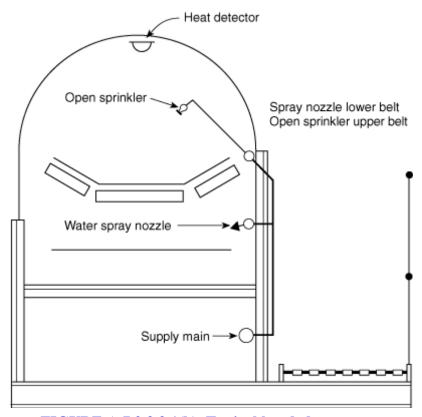


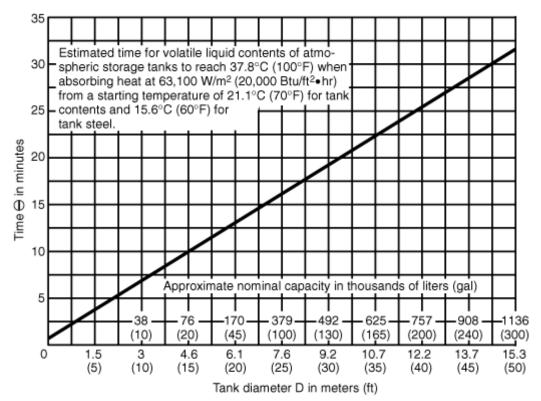
FIGURE A.7.2.3.3.1(b) Typical hooded conveyor.

- **A.7.3.1.1** System operation for a duration of several hours may be necessary before the required activities are completed.
- **A.7.3.2** Control of burning by directional water spray is not intended to preclude the installation of exposure protection for pump and compressor connections, exposed piping, compressor casings, drivers, lubrication systems, and related equipment.
- **A.7.4.1** Exposure Protection General. Generally, the upper portions of equipment and the upper levels of supporting structures are less severely exposed by fire than are the lower portions or levels, due to the accumulation at grade level of fuel from spillage or equipment rupture. Consideration may thus be given to reducing the degree of (or eliminating) water spray protection for the upper portions of high equipment or levels of structures, provided a serious accumulation of fuel or torch action from broken process piping or equipment cannot occur at these elevations and serious fire exposure does not exist. Examples are certain types of distillation columns [above the 9.2-m or 12.2-m (30-ft or 40-ft)] level and above the third or fourth level of multi-level open structures.

The densities specified for exposure protection include a safety factor of 2.0 (L/min)/m<sup>2</sup> (0.05 gpm/ft<sup>2</sup>) to compensate for unanticipated wastage.

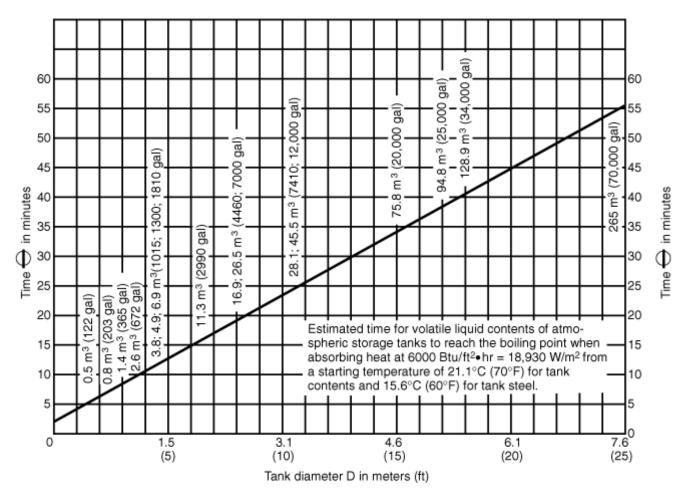
- **A.7.4.1.1** In determining the duration of the exposing fire, consideration should be given to the properties and quantities of the exposing combustibles and the anticipated effect of available manual fire fighting. System operation for several hours may be required.
- **A.7.4.2** Exposure Protection Vessels. It has been established that uninsulated vessels, under average plant conditions, enveloped with flame can be expected to absorb heat at a rate of at least 63,100 W/m² (20,000 Btu/hr/ft²) of exposed surface wetted by the contents. Unwetted, uninsulated steel equipment absorbs heat rapidly, and failure occurs from overpressure or overheating, or both, when such equipment is exposed to fire. Figure A.7.4.2(a) is a time-temperature curve showing the lengths of time required for vessels of different sizes containing volatile materials to have their contents heated to 38°C (100°F) from a starting temperature of 21°C (70°F) for tank contents and 16°C (60°F) for the tank steel. (See Requirements for Relief of Overpressure in Vessels Exposed to Fire; Transactions of the ASME, January, 1944, 1–53; "Venting of Tanks Exposed to Fire"; and Heat Input to Vessels.)

The application of water spray to a vessel enveloped by fire will reduce the heat input rate to a value on the order of 18,930 W/m² (6000 Btu/hr/ft²) of exposed surface wetted by the contents where the unit rate of water application is 8.2 (L/min)/m² (0.20 gpm/ft²) of exposed surface. The 18,930 W/m² (6000 Btu/hr/ft²) rate was also established in Rubber Reserve Company Memorandum 123, *Protection of Vessels Exposed to Fire*. Figure A.7.4.2(b) shows the estimated time for volatile liquid contents of atmospheric storage tanks to reach the boiling point where absorbing heat at 18,930 W/m² (6000 Btu/hr/ft²). This may be compared with Figure A.7.4.2(a) to show the benefits derived from water spray systems.



Note: For SI units, 1 Btu/ft<sup>2</sup>• hr = 3.155 W/m<sup>2</sup>; °C =  $\frac{5}{9}$  (°F - 32); 1 gal = 0.003 79 m<sup>3</sup> = 3.785 L; 1 ft = 0.305 m.

FIGURE A.7.4.2(a) Time-temperature curve.



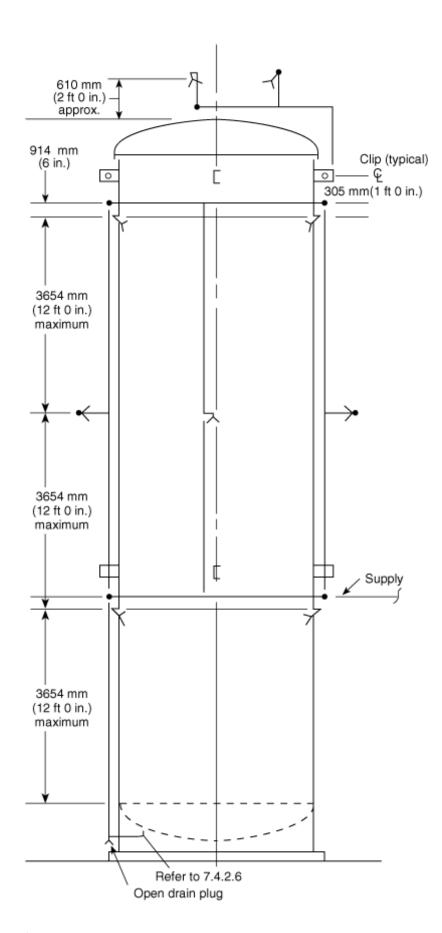
Note: For SI units, 1 Btu/ft²•hr = 3.155 W/m²; 1 gal = 0.003 79 m³ = 3.785 L;  $^{\circ}$ C =  $^{\circ}$ 4 ( $^{\circ}$ F - 32).

#### FIGURE A.7.4.2(b) Time-temperature curve.

Where the temperature of a vessel or its contents should be limited, higher densities than specified in 7.4.2.1 may be required.

Internally insulated or lined vessels require special consideration to determine necessary water spray requirements.

**A.7.4.2.2** See Figure A.7.4.2.2.



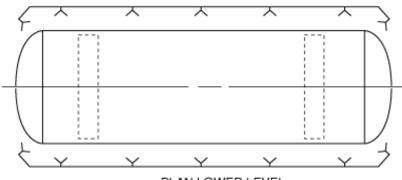
## FIGURE A.7.4.2.2 Typical vertical tank with skirt protection.

**Horizontal Tanks** 

## **A.7.4.2.3** See Figure A.7.4.2.3.

# 1829 mm To 2137 mm (6 ft 0 in.) approx. (7 ft 0 in.)

PLAN UPPER LEVEL



PLAN LOWER LEVEL

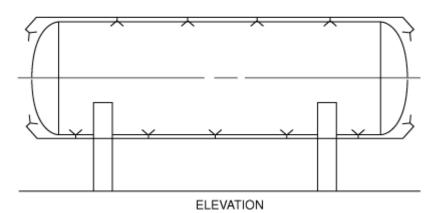


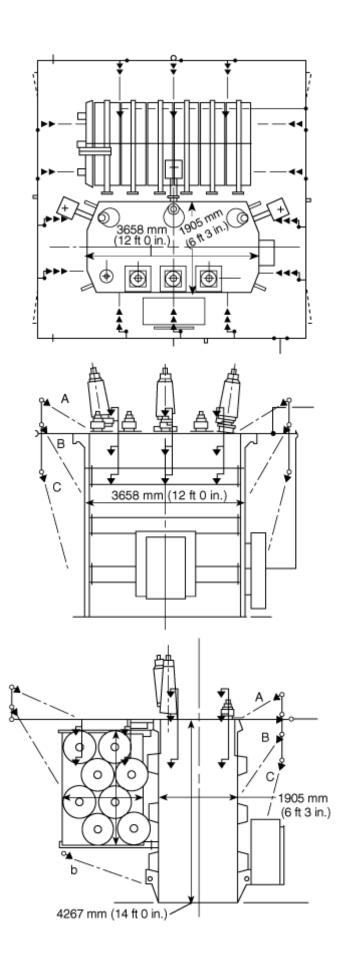
FIGURE A.7.4.2.3 Typical horizontal tank protection.

**A.7.4.3.1** The locations of nozzles should preferably be on alternate sides of the horizontal structural steel.

The wetted surface of a structural member (a beam or column) is defined as one side of the web and the inside surface of one side of the flanges.

**A.7.4.3.4** The locations of nozzles should preferably be on alternate sides of the vertical structural steel.

**A.7.4.4.1** See Figure A.7.4.4.1.



#### FIGURE A.7.4.4.1 Typical transformer layout.

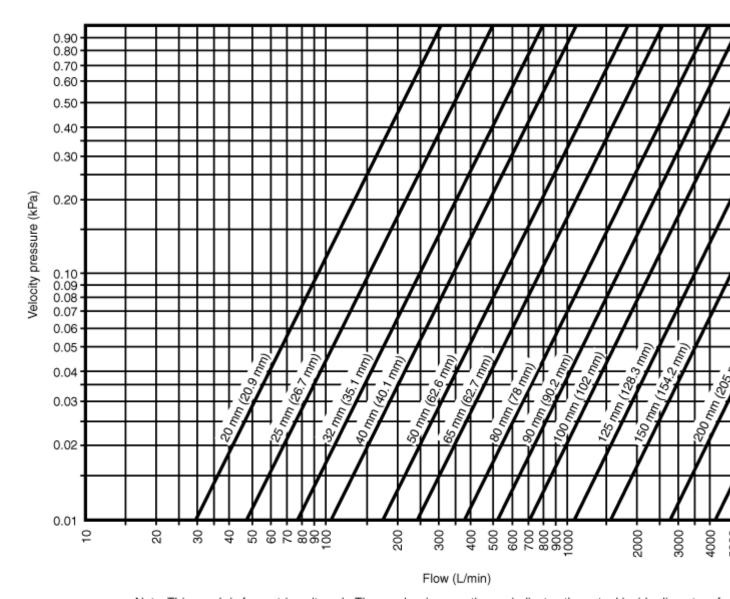
- **A.7.5** Water spray systems designed for extinguishment, exposure protection, or control of burning can disperse flammable gases for fire prevention. When designing water spray systems primarily for dispersion of flammable gases (for fire prevention), the following should be considered:
  - (1) Spray nozzles should be of the size and type to discharge a dense spray into the area of possible flammable vapor release at sufficient velocity to rapidly dilute the flammable vapors to a level below the lower flammable limit.
  - (2) Spray nozzles should be positioned to provide coverage of potential leak sources such as flanges, flexible connections, pumps, valves, vessels, containers, and so forth.
- **A.7.6.1** Examples of combined systems include the following:
  - (1) Open nozzle water spray protection for a vessel combined with area protection provided by a deluge system
  - (2) Automatic nozzle water spray protection for cable trays combined with area protection provided by a wet pipe system
- **A.7.6.2** Generally, the water spray component of a combined system is intended to supplement the protection provided by the sprinkler or deluge portion. The water spray usually is intended to cover a specific hazard or to cover specific areas or equipment items that cannot be otherwise adequately covered. Therefore, the required density from the sprinkler system should not be reduced when supplemental water spray is provided.

However, it would be acceptable to adjust the extent of water spray coverage when a portion of the coverage is provided by the sprinkler deluge portion of a combined system. For example, pressure vessels within the process structure protected by area deluge are typically provided with supplemental water spray on the bottom surfaces where the top surfaces are adequately covered by the deluge system above.

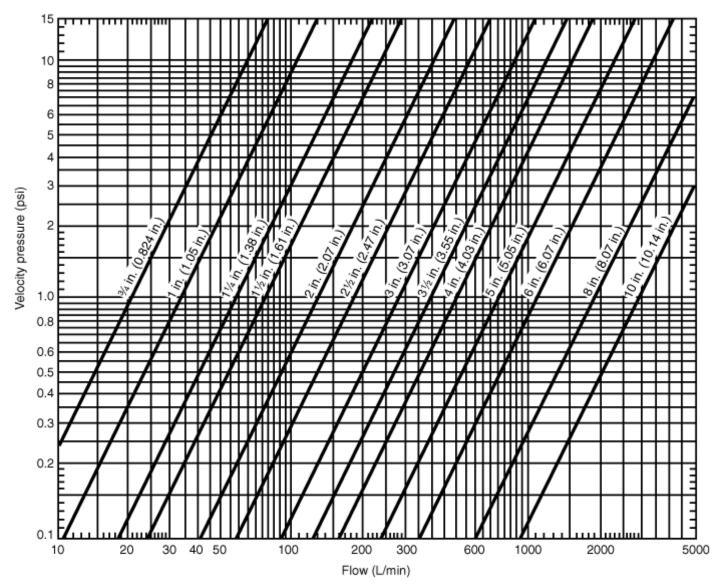
- **A.7.7.1** Different arrangements from those required for other types of detection systems may be required. In particular, it should be remembered that most listed detection devices are tested in an indoor, ceiling-mounted environment, while many water spray systems are installed outdoors. This can affect the type of detector chosen and its installed spacing.
- **A.7.7.3** Selection. Installations with temperature fluctuations include transformer protection involving heat exchangers having automatic fans and installations involving industrial ovens and furnaces. Additionally, protection of machinery involving movement of a hazardous material such as a belt conveyor would require a detection system having a faster response time than normal and appropriate interlocks to stop drive units, and so forth.
- **A.7.7.4** *Response Time.* Though not an aspect that can be designed prior to installation, the response time goal for the detection system is generally 40 seconds from exposure to initiation of the system actuation valve. The intent of the paragraph is to ensure that artificial delays are not built into the detection (initiating device) system.
- **A.8.1.1** See Annex B for Sample Calculations Forms.

- **A.8.1.2** The minimum operating pressure is required for proper pattern development and to overcome the effects of wind. For nozzles with orifices of 9.5 mm ( $^{\frac{3}{8}}$  in.) or less, a minimum pressure of 1.4 kPa (30 psi) is recommended.
- **A.8.1.4** *Sample Calculations.* See Annex B.
- **A.8.3** *Abbreviations and Symbols.* The standard abbreviations and symbols in Figure B.1(d) should be used.
- **A.8.3.2** See Figure B.1(a).
- **A.8.3.3** See Figure B.1(b).
- **A.8.3.4** See Figure B.1(c).
- **A.8.5.1.2** The velocity pressure  $P_v$  is determined by trial and error. It is necessary to estimate the flow, Q, in the pipe on the upstream side of the nozzle, which is used to determine a trial  $P_v$ , a trial q, and a trial Q. After determining the trial Q, use this value to determine a new  $P_v$ . If the new  $P_v$  is approximately equal to the trial  $P_v$ , consider the trial Q to be the actual Q and proceed with calculations. If the  $P_v$  does not check with the trial  $P_v$ , estimate Q again and proceed with successive corrections until an actual  $P_v$  is obtained that checks with a trial  $P_v$ .

The velocity pressure  $P_{\nu}$  is a measure of the energy required to keep the water in a pipe in motion. At the end of the nozzle or end section of a system (when considering the junction of sections of systems) the total pressure available in a pipe at that point should be considered as causing flow. However, at other nozzles or junction points the pressure causing flow will be the normal pressure, which is the total pressure minus the velocity pressure. Figure A.8.5.1.2(a) and Figure A.8.5.1.2(b) may be used for determining velocity pressures, or velocity pressure may be determined by dividing the flow in gpm squared by the proper constant from Table A.8.5.1.2.



Note: This graph is for metric units only. The number in parentheses indicates the actual inside diameter of p FIGURE A.8.5.1.2(a) Metric units. Graph for the determination of velocity pressure.



Note: This graph is for U.S. units only. The number in parentheses indicates the actual inside diameter of pipe. FIGURE A.8.5.1.2(b) U.S. units. Graph for the determination of velocity pressure.

**Table A.8.5.1.2 Constants for Determining Velocity** 

	Pressure									
Pipe Sched ule	Pipe Size (in.)	Constant Based on Actual I.D.								
40	1	1,080								
40	11/4	3,230								
40	$1\frac{1}{2}$	5,980								
40	2	16,200								
40	$2\frac{1}{2}$	33,100								
40	3	78,800								
40	$3\frac{1}{2}$	141,000								
40	4	234,000								

40	5	577,000
40	6	1,204,000
30	8	3,780,000
40	8	3,620,000
	_	

The following assumptions are to be used in applying velocity pressure to the calculations:

- (1) At any nozzle along a pipe, except the end nozzle, only the normal pressure can act on a nozzle. At the end nozzle, the total pressure can act.
- (2) At any nozzle along a pipe, except the end nozzle, the pressure acting to cause flow from the nozzle is equal to the total pressure minus the velocity pressure on the upstream side.
- (3) To find the normal pressure at any nozzle except the end nozzle, assume a flow from the nozzle in question and determine the velocity pressure for the total flow on the upstream side. Because the normal pressure is equal to the total pressure minus the velocity pressure, the value of the normal pressure so found should result in a nozzle flow approximately equal to the assumed flow. If not, a new value should be assumed and the calculations repeated.

Velocity pressure has the effect of reducing the flow from the side outlet of a junction. Ignoring velocity head can introduce a significant error, resulting in an actual nozzle pressure that is less than required. This is especially true where velocities are high (in excess of 20 ft/sec).

The example shown in Figure A.8.5.1.2(b) has been crafted to illustrate situations where a design, if not corrected for an excessive velocity pressure, may yield results that underestimate the required flow and pressure for the system.

**A.8.5.3** Experience has shown that good results are obtained if the calculations are made in accordance with this section. It is recognized that satisfactory results can be obtained by using other methods. However, in order to simplify the checking of calculations and to obtain more consistent correlation between calculated system characteristics and actual system characteristics, it is desirable to use a standard method. The flow from nozzles can be obtained from discharge curves rather than individual calculations at the preference of the calculator. Similarly, flow characteristics of lines or sections of systems can be obtained by plotting results on charts made up to N<sup>1,85</sup> rather than by calculating constants (*K*-values).

**A.9.3.1** A fire department connection should not be considered as a primary source of water supply for a water spray system.

**A.10.1** See NFPA 13, Standard for the Installation of Sprinkler Systems, and NFPA 24, Standard for the Installation of Private Fire Service Mains and Their Appurtenances, for further information on system acceptance.

**A.10.2.1** When planning the flushing operations, consideration should be given to disposal of the water issuing from the test outlets.

**A.10.4.2** *Response Time.* Some detection circuits might be deliberately desensitized in order to override unusual ambient conditions. In such cases, the response in 10.4.2 may be

exceeded.

Testing of integrated tubing systems might be related to this test by means of a standard pressure impulse test specified by the listing laboratory.

One method of testing heat detection uses a radiant heat surface at a temperature of 149°C (300°F) and a capacity of 350 W at a distance of 25 mm (1 in.) but not more than 50 mm (2 in.) from the nearest part of the detector. This method of testing with an electric test set should not be used in hazardous locations. Other test methods can be employed, but the results should be related to the results obtained under these conditions.

**A.10.4.3.2** During the acceptance discharge test, it might be advisable to partially close the system control valve to reduce the system supply pressure to the minimum pressure required by the system calculation. With the gauge at the deluge valve reading the minimum pressure, the test gauges at the most remote nozzle should be read to verify minimum required nozzle pressure. Additionally, pattern and coverage from each open nozzle should be observed to verify adequate operation.

**A.12.1** This standard deals with fixed piped ultra high-speed water spray systems. There are specialized self-contained ultra high-speed deluge systems, which are outside the scope of this standard. The supervised systems may be used alone or with the ultra high-speed deluge systems discussed in this standard. Non-supervised systems should not be used without fixed pipe ultra high-speed backup as described in this standard. The following two small self-contained deluge systems are currently in use [the military ordnance industry (both government and private facilities) is currently the primary user].

- (1) The portable deluge system is a transportable self-contained ultra high-speed deluge system. The system uses multiple optical fire detectors, multiple nozzles, and a pressurized water tank [typically 379 L (100 gal) of water]. Response time does not exceed 100 ms (detection to water at the nozzle). The portable system is intended to protect short-term operations. This system is supervised.
- (2) A fixed pressurized sphere ultra high-speed deluge system is a self-contained system. The system uses one or more optical fire detectors, at least one pressurized [typically 3448 kPa (500 psi)] water sphere (typically 10 to 30 L) with a rupture disc and internal squib), and an electronic controller. Response time is less than 10 ms (detection to water at the nozzle). The sphere discharges water when the squib fires, opening the rupture disc. A screen breaks the water into small-atomized particles and collects the residual squib fragments. This system is not currently supervised.

**A.12.1.1** Extinguishment of fires using ultra high-speed water spray systems is accomplished by surface cooling, by dispersion or dilution of the combustible material, by cooling the expanding flame front, or by a combination of these factors.

Examples of facilities where such systems are advantageous include rocket fuel manufacturing or processing, solid propellant manufacturing or handling, ammunition manufacturing, pyrotechnics manufacturing, and the manufacture or handling of other volatile solids, chemicals, dusts, or gases. Other facilities where the very rapid application of water spray is desirable can be considered. Where used to protect process equipment, these systems will not prevent overpressures. This equipment should be protected in accordance with NFPA 68, *Guide for Venting of Deflagrations*.

**A.12.1.2** For the design of deflagration suppression systems for purposes of limiting overpressure, refer to NFPA 69, *Standard on Explosion Prevention Systems*.

There is no fire protection system that can stop the detonation process when the explosive goes to a high-order state. In many cases, there is a fire or deflagration before the incident progresses to a detonation. An example of high explosives process applications is the extrusion dies for C-4 explosives. In this situation, there is a high probability that there will be deflagration that can be suppressed with an ultra high-speed water spray system before the transition to a detonation.

#### **A.12.3.1.1** See Figure A.12.3.1.1.

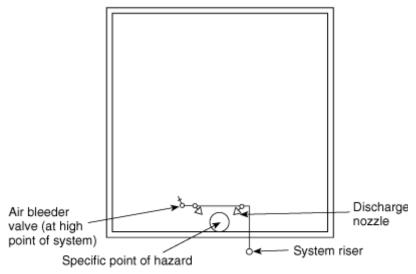
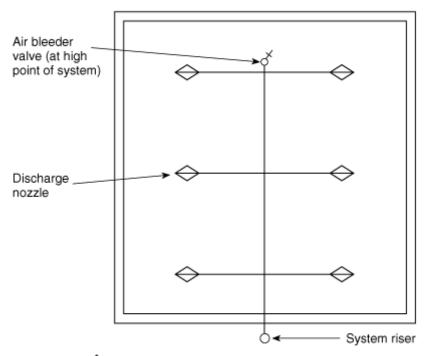
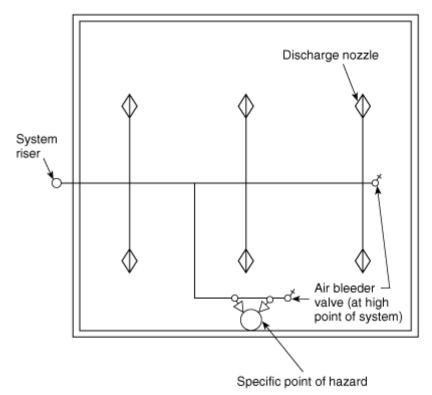


FIGURE A.12.3.1.1 Ultra high-speed local application for a point of hazard. A.12.3.1.2 See Figure A.12.3.1.2.



## FIGURE A.12.3.1.2 Ultra high-speed area application for a small room.

**A.12.3.1.3** An example of a dual application system could be one that protects a specified area from the ceiling and also has nozzles located to protect a specific point or points of likely ignition (see Figure A.12.3.1.3).



Note:  $\Phi$ - High-speed water spray nozzle in the pendant position.

#### FIGURE A.12.3.1.3 Ultra high-speed dual application system.

**A.12.3.1.4** For additional information, refer to U.S. Department of Defense standard DOD 6055.9-STD, *Ammunition and Explosives Safety Standards*. Copies can be purchased from the National Technical Information Service, 5285 Port Royal Road, Springfield, VA 22161.

To protect personnel, the process equipment should be interlocked to shut down upon activation of the ultra high-speed water spray system.

**A.12.3.2.3** A commonly used density for preventing propagation and structural damage is 200 (L/min)/m<sup>2</sup> (0.5 gpm/ft<sup>2</sup>).

Some hazards, particularly the extinguishment of pyrotechnic fires, require significantly higher density rates. These rates may be as high as 11 (L/min)/m² (3.0 gpm/ft²) for area coverage, or 189 L/min (50 gpm) per nozzle for point protection coverage. Tests have shown that fires involving some pyrotechnic materials require a water flow of 757 L/min (200 gpm) or more to extinguish.

**A.12.3.4** As speed is a strong function of volumetric capacity, it is recommended that ultra high-speed water spray systems be kept as small as possible. Tests have shown that systems having a capacity in excess of 1893 L (500 gal) are less likely to be capable of delivering water to the nozzles within 100 milliseconds. The capacities of various sizes of pipe are given in Table A.12.3.4 for convenience in calculating system capacity.

Table A.12.3.4 Capacity of One Foot of Pipe (Based on Actual Internal Pipe Diameter)

Nomi nal Diame ter	Gal		Nomi nal Diame ter	Gal	
Sch 40	Sch 10	<b>Sch 40</b>	Sch 10		
3/4 in.	0.028	_	3 in.	0.383	0.433
1 in.	0.045	0.049	$3\frac{1}{2}$ in.	0.513	0.576
11/4 in.	0.078	0.085	4 in.	0.660	0.740
$1\frac{1}{2}$ in.	0.106	0.115	5 in.	1.040	1.144
2 in.	0.174	0.190	6 in.	1.501	1.649a
$2\frac{1}{2}$ in.	0.248	0.283	8 in.	2.66 <sup>c</sup>	2.776 <sup>b</sup>

Note: For SI units, 1 in. = 25.4 mm; 1 ft = 0.3048 m; 1 gal = 3.785 L.

**A.12.3.8.2** Initial pressure to an ultra high-speed water spray system is ordinarily obtained from an elevated tank, a pressure tank, or an excess pressure pump. A fire pump can be used to provide the required flow and pressure after the system has started to operate.

**A.12.3.9.1** The time for the water to travel from the nozzle to the hazard is not currently included in the total response time, but research efforts are under way to determine the impact of water travel.

a0.134 wall pipe

b0.188 wall pipe

<sup>&</sup>lt;sup>c</sup>Schedule 30

**A.12.3.10** System actuation valves commonly in use are the squib-operated valve [see Figure A.12.3.10(a)] and the solenoid-operated valve [see Figure A.12.3.10(b)].

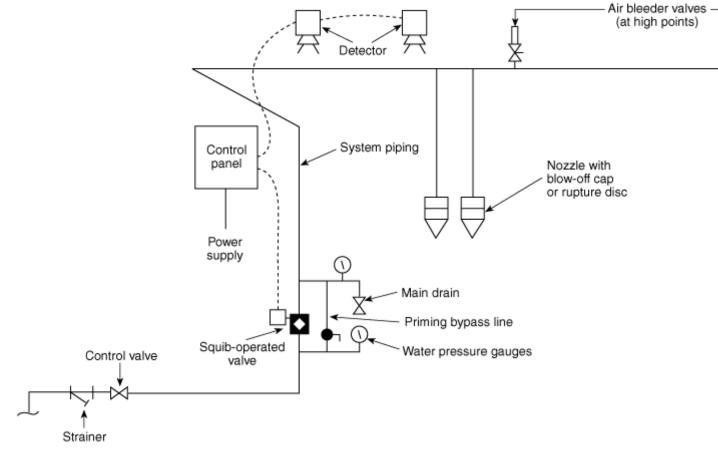


FIGURE A.12.3.10(a) Ultra high-speed system using squib-actuated valve.

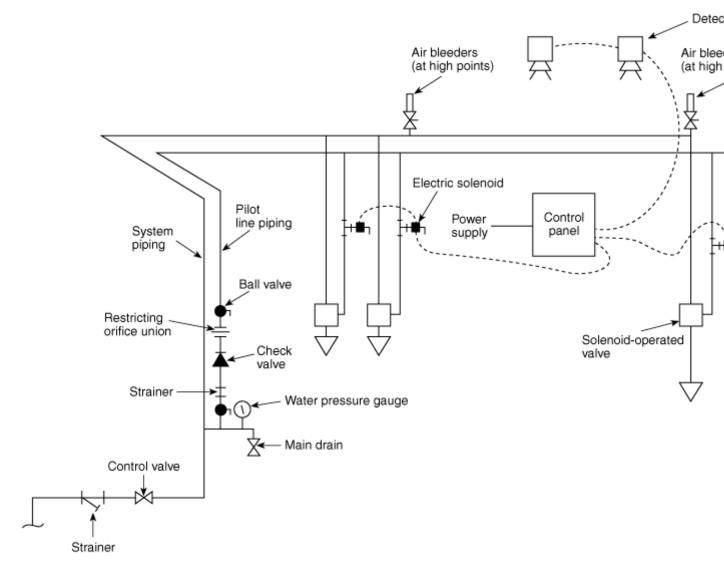


FIGURE A.12.3.10(b) Ultra high-speed system using solenoid-operated valves.

**A.12.3.10.1** Consideration should be given to personnel, operations, and maintenance of protected equipment.

**A.12.3.11.3** Trapped air in an ultra high-speed water spray system dramatically increases system response time. Piping systems must be sufficiently sloped to allow removal of all trapped air.

**A.12.3.12** Pipe movement can be caused by system activation or from the force of a deflagration.

**A.12.3.13.1** Strainers minimize sediment from interfering with the proper seating of the poppet.

**A.12.4** Response time is commonly measured by placing a water flow detector on the nozzle and measuring the time from presentation of an energy source to the sensing device and commencement of water flow at the nozzle.

The following two methods are commonly used to measure response time:

- (1) *Digital Timer*. A millisecond digital timer is started when a saturating energy source is presented to the sensing device and stopped by the actuation of a water flow switch at the nozzle.
- (2) *High-Speed Video Recording System*. A high-speed video camera and recorder (at least 120 frames/second) can be used to provide a very accurate measurement. It can also be used to measure the water travel time from the nozzle to the hazard.

**A.12.5.1** A good preventive maintenance program is needed to keep systems operational and reduce false activations. Experience has shown that increasing the time period beyond 6 weeks results in a significant increase of false activations and other system problems. The following items should be considered when establishing maintenance procedures:

- (1) System checks.
  - (a) Measure all voltages.
  - (b) Put all controllers in bypass, and check for loose wires and/or relays.
  - (c) Clean all dirt and debris from control panel.
  - (d) Check all lamps on control panel.
  - (e) Spot check conduit fittings for moisture and/or loose wire nuts.
  - (f) Check squib-operated valve o-rings (damp or wet primers).
  - (g) Check OS&Y valve limit switches on water supply lines.
- (2) Sensing devices.
  - (a) Remove each lens and clean.
  - (b) Remove each barrel, and check grounding springs, when used.
  - (c) Tighten each terminal screw in sensing devices.
  - (d) Clean and inspect all optical integrity rings, when used.
  - (e) Check for moisture and/or corrosion inside sensing device housings.
  - (f) Check each detector for proper alignment.
  - (g) Check housing for continuity.
  - (h) Reactivate system, and check for problems.
- (3) Flow tests should be conducted.
  - (a) Annually for active systems.
  - (b) After major maintenance or modification.
  - (c) After reactivating an inactive system.
- (4) Priming water squib-operated system.
  - (a) Check weekly.

- (b) Open vent.
- (c) Crack priming valve.
- (d) Allow water to flow for a few minutes, close priming valve, then the vent valve.
- (5) Squib-operated valve.
  - (a) Trip system at least annually by firing primers.
  - (b) Replace primers at least annually.
- (6) Solenoid-operated valves.
  - (a) Trip system at least annually.
  - (b) Check solenoid valve for leaks.

# **Annex B Hydraulic Calculations**

# **B.1** Forms for Hydraulic Calculations.

See Figure B.1(a) through Figure B.1(d).

Name	·	HYDF	RAULIC DESIGN	INFORMATION	SHEET Date
Locat	ion				
Buildi	ng				System No
Contr	actor_				Contract No.
Calcu	lated I	by			Drawing No
	tructio			ombustible	Ceiling Height
			_		
sign		NFPA 13	pecify)		Curv
System Design	Dens Area Hose Hose	per sprinkler allowance L/min (gpm): Inside allowance L/min (gpm): Outside	Siz	e	System Type  Dry Deluge  Sprinkler or Nozzle  Model —  K-Factor —
	ulation	System L/min (gpm) required  "C" factor used:  Total L/min (gpm) required	Overhead		Underground _
Water Supply	Stat Res L/m	Water Flow Test  e & time tic kPa (psi) idual kPa (psi) in (gpm) flowing vation	Rated capacity	mp Data	Tank or Res Capacity  Elevation  Well  Proof flow
>		tion ce of information			
зде	Stora	modity age height age method: Solid piled % Plastics	Area % Palletized		Aisle width
Commodity Storage	ķ		entional pallet pallet	Automatic storag Solid shelving Open	ge Encapsulate  Nonencapsu
ŏ	Rack	Flue Spacing in me Longitudinal Transvers		1	ce from Top of Storage to
	ΙI	Horizontal barriers provided			

# FIGURE B.1(a) Sample summary sheet.

# HYDRAULIC CALCULATIONS

Contract No.	Sheet No
Name and Location	

Reference	Nozzle Ident. & Location	Flow in L/min (gpm)	Pipe Size mm (in.)	Pipe Fittings & Devices m (ft)	Equiv. Pipe Length m (ft)	Friction Loss bar/m (psi/ft)	Req. bar (psi)	Normal Pressure bar (psi)	
		q			Lgth.		Pt	Pt	Ţ
		Q	1		j Fig.		Pf	Pv	1
					Tot.		Pe Pt	Pn Pt	╀
		۹	]		Lgth	1	Pf ———	Pt	ł
		Q			I IOI.	1	Pe	Pn	1
		q			Lath.		Pt	Pt	İ
		-	1		j Fig.	]	Pf	Pv	]
		Q			I IOt.		Pe	Pn	╀
		q			Lgth.	-	Pt	Pt	1
		Q	1		Ftg Tot.	1	Pe —	Pn	ł
		q			Lgth.		Pt	Pt	t
			-		Ftg.	1	Pf	Pv	1
		Q			TOT.	1	Pe	Pn	1
		q			Lgth.		Pt	Pt	1
		a	1		Ftg Tot.	-	Pf Pe	Pv Pn	┨
		_			Lgth.		Pt	Pt	t
		9			Ftg.	1	Pf ——	TPV	1
		Q			l lot.	1	Pe	Pn	1
		q			Lgth.		Pt	Pt	Г
		Q	1		Į Ftg.		Pf	Pv	1
					1101.		Pe	Pn	╀
		q			Lgth.	-	Pt	Pt	1
		Q			Ftg Tot.	1	Pe ——	Pn	1
		q			Lgth.		Pt	Pt	t
			ł		Ftg.	]	Pf	Pv	1
		Q			l lot.		Pe	Pn	ļ
		q			Lgth.	1	Pt	Pt Pv	1
		a	1		Ftg Tot.	1	Pf	Pn	┨
		q			Lgth.		Pt	Pt	t
		· —	-		Ftg.	1	Pf	Pv	1
		Q			Tot.	1	Pe	Pn	1
		q			Lgth.		Pt	Pt	1
		a	1		Ftg Tot.	-	Pf Pe	Pv Pn	1
		_			Lgth.		Pt	Pt	+
		۹			Ftg.	1	Pf ———	Fv	1
		Q			Tot.		Pe	Pn	1
		q			Lgth.		Pt	Pt	Γ
		\ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \	1		Ftg		Pf	Pv	1
		_			Tot.		Pe	Pn	+
		q	]	<u> </u>	Lgth Ftg.	1	Pt	Pt	+
		Q			Tot.	1	Pe —	Fv	+

FIGURE B.1(b) Sample worksheet.

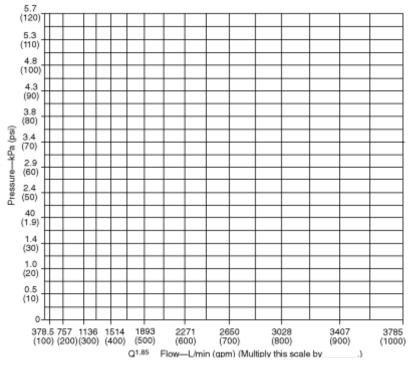


FIGURE B.1(c) Sample graph sheet.

Symbols or Abbreviations	Item	Symbols or Abbreviations	Item
P	Pressure in psig	GV	Gate valve
$P_m$	Pressure in bars	Del V	Deluge valve
gpm	Flow rate in U.S. gallon per minute	DPV	Dry-pipe valve
q	Flow increment in gpm to be added at a specific	AL V	Alarm valve
	location	CV	Swing check valve
$q_m$	Flow increment in liters per minute (L/min) to be added at a specific location	St	Strainer
Q	Summation of flow in gpm at a specific location	psig	Pounds per square inch
$Q_m$	Summation of flow in L/min at a specific location	V	Velocity of water in pipe
$P_t$	Total pressure at a point in a pipe	v <sub>m</sub>	Velocity of water in pipe
$P_f^t$	Pressure loss due to friction between points indicated in location column	g	Acceleration due to grav (generally 32.0 or 32.1
$P_{\theta}$	Pressure due to elevation difference between indicated points. This can be a plus value or a	$g_m$	Acceleration die to gravit per second
	minus value. Where minus the symbol (–) shall	K	A constant
	be used; where plus, no sign need be indicated.	$\kappa_m$	A constant (SI)
$P_{\nu}$	Velocity pressure at a point in a pipe	C	Hazen and Williams frict
P <sub>μ</sub> E	Normal pressure at a point in a pipe	p	Frictional resistance per
É	90° elbow	·	per foot
EE	45° elbow	$p_m$	Frictional resistance per
Lt E	Long turn elbow		per meter
Cr	Cross	d	Actual internal diameter
T	Tee, flow turned 90°	$d_m$	Actual internal diameter

FIGURE B.1(d) Abbreviations and symbols for hydraulic calculations.

#### **B.2 Sample Calculations.**

Figure B.2(a) shows a hypothetical water spray system layout. Figure B.2(e) through Figure B.2(h) show a sample calculation for this system, using pipe sizing and nozzles with constants such that the velocity pressures generally exceed 5 percent of the total pressures, and the designer elected to include velocity pressures. Figure B.2(i) through Figure B.2(l) show a sample calculation for this system, using pipe sizing and nozzles with constants such that velocity pressures are less than 5 percent of the total pressures, and the velocity pressures were not included in the calculation. Figure B.2(c) and Figure B.2(d) show a graphical representation of the results of hydraulic calculations shown in Figure B.2(i) through Figure B.2(l), assuming 946 L/min (250 gpm) outside hydrant flow requirements and 0.28 bar (4.0 psi) of underground friction loss.

Calculations for the system in Figure B.2(b) are fairly straightforward until one attempts to balance at junction point "C." The side outlet of the tee at "C" only sees the normal pressure. In this example, due to the high velocity through "C", the normal pressure available to "B" is less than that required to satisfy the individual nozzle demand. This requires actually increasing the total pressure coming into "C" to satisfy the rule for both velocity head correction and for pressure balance. If not, the nozzles fed by line "C-B" will be denied adequate flow. [Refer to Figure B.2(b).] The 28.2 psi pressure at "C" from the side outlet is used as a minimum normal pressure starting point, to which the assumed velocity pressure of 13.6 psi is added, to get a new total pressure of 41.8 psi. The flow straight through the tee at point "C" is then increased by the ratio of (41.8/29.7)<sup>1/2</sup>.

Figure B.2(m) and Figure B.2(n) present calculations in which velocity pressure is ignored. For the example system shown, correcting the velocity pressure indicates that the system would require 12.1% more flow (785.2 gpm vs. 700.5 gpm) and 26.9% more pressure (120.2 psi vs. 94.7 psi).

The alternatives for correcting the system to a more balanced configuration include increasing the pipe size to reduce the effect of velocity pressure (though this may result in an alteration of the specified nozzle's spray pattern) and modifying the piping arrangement (for example, using bull-headed tees at critical junctions). Whether or not a correction is made, the velocity pressure at each side outlet should be examined to determine if corrective action is desired.

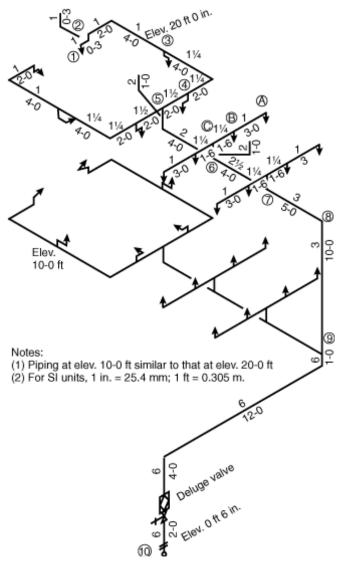
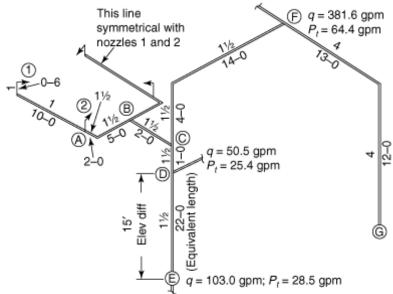


FIGURE B.2(a) Drawing of water spray system used for sample calculations shown in Figures B.2(e) through B.2(l).



Note: For SI units; 1 gpm = 3.78 L/min (flow); 1 ft = 0.3048 m (length); 1 in. = 25 mm: 1½ in. = 40 mm: 4 in. = 100 mm (pipe).

FIGURE B.2(b) Drawing of water spray system used for sample calculations shown in Figure B.2(m) and Figure B.2(n).

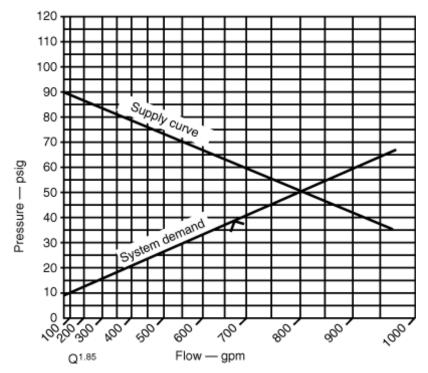


FIGURE B.2(c) English. Sample graph sheet.

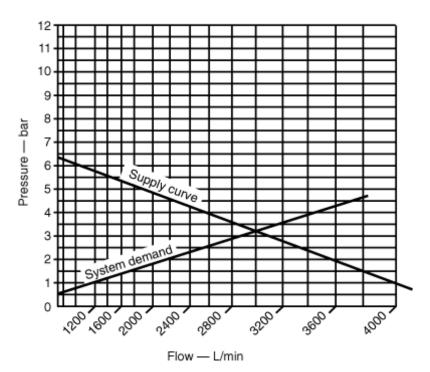


FIGURE B.2(d) Metric. Sample graph sheet.

# HYDRAULIC CALCULATIONS

For	System Shown on Fig. B.2(a)	Sheet No.	1
	All Nozzles Type N 90	Ву	J.E.
	(Nozzle Discharge Constant 9.0)	Date	12 - 3 -
		Job No	1571

Nozzle	Flow	Pipe	Pipe	Fa	uiv.	Friction		Τ.	lormal		
Ident. & Location	in gpm	Size (in.)	Fittings & Devices (ft)	ΡÌ	pe th (ft)	Loss (psi/ft)	Pressure Summary		ressure (psi)	Nozzle Elev.	
1-N9O	9 40.2		E = 2.0	Lgth	0.5		Pt20.0	Pt .		21.0'	
<u>(1)</u>	Q 40.2	1 1		Ftg Tot.	2.0 2.5	0.47	Pe Pf 1.2	Pv :			$q_1 = 9$
	q _		2E = 4.0	Lgth.	6.0		Pt 21.2	Pt			
	-	1		Ftg.	4.0	0.47	Pe -	Pv			]
2	Q 40.2		5 70	Tot.	10.0		Pf 4.7	Ph	05.0		
1-N90	q 40.6	ate	E = 3.0	Lgth Ftg.	6.0 3.0	0.46	Pt <u>25.9</u> Pe -	Pt Pv	25.9 2.0		$q_3 = \varepsilon$
3	Q 80.8	11/4		Tot.	9.0	0.40	Pf 4.1	Ph	23.9		For K <sub>3</sub>
1-N9O	q 43.5		T = 8.0	Lgth	2.0		Pt30.0	Pt .	30.0		
(4)	Q 124.3	11/2		Ftg Tot.	8.0	0.48	Pe	Pv.	2.6		$q_4 = \varepsilon$
		_	E = 5.0	Lgth.	10.0 5.0		Pf 4.8 Pt 34.8	Ph	27.4		-
3-N90	q <u>124.3</u>	2	L = 3.0	Ftg.	5.0	0.50	Pe 0.4	Pv			1
	Q 248.6	_		Tot.	10.0		Pf 5.0	Ph			1
4-N90	q 180.0			Lgth	4.0		Pt	Pt.	40.2	20.0'	$q_G = 3$
6	Q 428.6	21/2		Ftg Tot.	4.0	0.58	Pe Pf 2.3	Pv .	5.5 34.7		For K
4-N90	q 188.0		E = 7.0	Lgth.	5.0		Pt 42.5	Pt	42.5		
		3		Ftg.	7.0	0.40	Pe	Pv	4.8		$q_7 = 3$
<u> </u>	Q 616.6			Tot.	12.0		Pf 4.8	Ph	37.7		ļ
	9	3		Lgth Ftg.	10.0	0.40	Pt 47.3 Pe 4.3	Pt Pv			1
<b>B</b>	Q 616.6	5		Tot.	10.0	0.40	Pf 4.0	Ph.			1
14-N90	9 640.0		2E = 28.0	Lgth	19.0		Pt _ 55.6	Pt .	55.6	10.0'	q <sub>9</sub> = 8
9	Q 1256.6	6	Del V. = 10.0	Ftg	41.0	0.054	Pe <u>4.1</u> Pf <u>3.2</u>	Pv .	1.3		For K <sub>g</sub>
		_	G.V. = 3.0	Tot. Lgth.	60.0		Pf 3.2 Pt 62.9 /	Pt	54.3	0.5'	9
	9			Ftg.			Pe	Pv.		0.0	1
	Q 1256.6	/		Tot.			Pf	Ph			1
	q			Lgth			Pt	Pt Pv			Note: F
	a	1		Ftg Tot.			Pe	Ph.			y. 9
	q			Lgth.			Pt	Pt			Residu
	<u> </u>	1		Ftg.			Pe	Pv :			Flow: 13
	Q			Tot.			Pf	Ph			~230
	۹			Lgth Ftg.			Pt Pe	Pv.			@ 62.5
	Q			Tot.			Pf	Ph			1
	q			Lgth.			Pt	Pt			
	a	1		Ftg			Pe	Pv :			-
				Tot. Lgth.			Pt	Pt			_
	9	1		Ftg.			Pe	Pv.			1
	Q			Tot.			Pf	Ph '			1
	q			Lgth			Pt	Pt .			-
	Q	1		Ftg Tot.			Pe Pf	Pv . Ph			-

FIGURE B.2(e) English. Calculation of system shown in Figure B.2(a) with velocity pressure included.							

	HTDRAULIC CALCUL	AHONS	
For _	System Shown on Fig. B.2(a)	Sheet No	2
	All Nozzles Type N 90	Ву	J.E.
	(Nozzle Discharge Constant 3.0)	Date	12 - 3
		Job No.	1571

Job No. \_

Nozzle Ident. & Location	Flow in gpm	Pipe Size (in.)	Pipe Fittings & Devices (ft)	Equiv. Pipe Length (ft)	Friction Loss (psi/ft)	Pressure Summary	Normal Pressure (psi)	Nozzle Elev.	
1-N9O	9 40.2		E=2.0	Lgth. 0.5		Pt 20.0	Pt		
(1)	Q 40.2	1	T=5.0	Ftg. 7.0	0.47	Pe	Pv		K <sub>3</sub>
				Tot. 7.5 Lgth.		Pf 3.5 Pt 23.5	Ph Pt		
	٩			Ftg.	1	Pe	Pv		1
	Q			Tot.		Pf	Ph		
	q			Lgth.		Pt	Pt		
<b>*</b>	a			Ftg Tot.	-	Pe	Pv		-
1-N90	q 40.2			Lgth. 3.0		Pt 20.0	Pt	21.0'	
		1		Ftg. –	0.47	Pe	Pv		]
(A)	Q 40.2		T. C.O.	Tot. 3.0		Pf 1.4	Ph Of 4		
1-N9O	9 <i>39.6</i>	ate	T=6.0	Lgth. <u>1.5</u> Ftg. 6.0	0.44	Pt <u>21.4</u> Pe –	Pt 21.4 Pv 2.0		-
B	Q 79.8	11/4		Tot. 7.5	0.44	Pf 3.3	Ph 19.4		1
2-N90	q 79.8		T=10.0	Lgth. 1.0		Pt 24.7	Pt		
©	Q 159.6	2		Ftg. 10.0	0.23	Pe <u>0.4</u>	Pv		K
				Tot. 11.0		Pf 2.5 Pt 27.6	Ph Pt	20.0'	
	۹			Lgth Ftg.	1	Pt <u>27.6</u> Pe	Pv	20.0	1
	Q			Tot.	1	Pf	Ph —		1
Lower Pipe Level	q			Lgth.		Pt	Pt		
3	Q			Ftg. Tot.		Pe	Pv Ph		
			T=15.0	Lgth. 5.0		Pt 42.5	Pt		
14-N90	۹	3	7=10.0	Ftg. 15.0	0.40	Pe 8.0	Pv		Kg
<u> </u>	Q 616.6			Tot. 20,0	00	Pf 50.5	Ph		Ľ
	q			Lgth.		Pt	Pt		
	a		<u> </u>	Ftg. Tot.	-	Pe Pf	Pv Ph		-
	q			Lgth.		Pt	Pt		
	-			Ftg.	]	Pe	Pv		]
	Q			Tot.		Pf	Ph		
	q			Lgth Ftg.		Pt Pe	Pt Pv		-
	Q			Tot.	1	Pf	Ph		1
	q			Lgth.		Pt	Pt		
	\[ \]			Ftg.	]	Pe	Pv		
				Tot.		Pf	Ph Pt		
	۹			Lgth Ftg.	1	Pt Pe	Pv		
	Q			Tot.		Pf	Ph		
	q			Lgth.		Pt	Pt		
	a			Ftg Tot.		Pe Pf	Pv Ph		
	_			Lgth.		Pt	Pt		
	٩			Ftg.	1	Pe —	Pv		
	Q			Tot.	1	Pf	Ph		1

Note: The velocity pressure  $P_v$  is determined by trial. It is necessary to estimate the flow Q in the pipe on the upsteam side of determine a trial  $P_v$ , which is used to determine a trial Q, and a trial Q. After determining the trial Q, use this value Q. If the new Q is approximately equal to the trial Q, consider the trial Q to be the actual Q and proceed with the calculation

FIGURE B.2(f) English. Calculation of system shown in Figure B.2(a) with velocity pressure included.

a <sub>1</sub> = 129.6		Pre (	mmary (m)		Friction Loss (bar/m)	ipe ngth m)	Lei	Fittings & Devices (m)	Pipe Size (mm)	Flow in L/min	Nozzle Ident. & Location
-		Pt _ Pv	1.38	Pt _ Pe	0.11	0.2 0.6	Lgth. <sub>-</sub> Ftg.	E = 0.6	25	q <u>152</u>	1-N90
-		Pn <sup>-</sup>	0.08	Pf	0,,,,	0.8	Tot.			Q 152	1
		Pt Pv	1.46	Pt _ Pe	0.44	1.8 1.2	Lgth.	2E = 1.2		q –	
-		Pn -	0.33	Pf -	0.11	3.0	Ftg. Tot.		25	Q 152	2
q <sub>3</sub> = 119.5	1.79	Pt _	1.79	Pt _		1.8	Lgth.	E = 0.9		q 154	1-N90
For K <sub>3</sub> Cald	0.14 1.65	Pv _ Pn	0.28	Pe _ Pf	0.10	0.9 2.7	Ftg. Tot.		32	Q 306	3
	2.07	Pt	2.07	Pt		0.6	Lgth.	T = 2.4		q 165	1-N90
q <sub>4</sub> = 119.5	0.18	Pv _	-	Pe	0.11	2.4	Ftg.		40		
<del>                                     </del>	1.89	Pn Pt	0.33 2.40	Pf Pt		3.0 1.5	Tot. Lgth.	E = 1.5			4)
-		Pv -	0.03	Pe -	0.11	1.5	Ftg.	E = 1,0	50	q <u>471</u>	3-N90
1		Pn -	0.34	Pf	0	3.0	Tot.			Q 941	6
q <sub>6</sub> = 437√	2.77	Pt Pv	2.77	Pt _	0.47	1.2	Lgth.			q 681	4-N90
46=4071	0.38 2.39	Pn -	0.16	Pe _ Pf	0.13	1.2	Ftg Tot.		65	Q 1622	6
	2.93	Pt _	2.93	Pt _		1.5	Lgth.	E = 2.1		q 712	4-N90
q <sub>7</sub> = 437√.	0.32	Pv _	-	Pe_	0.09	2.1	Ftg.		80	Q 2334	7
+	2.61	Pn Pt	0.33 3.26	Pf Pt		3.6 3.0	Tot. Lgth.				
1		Pv =	0.30	Pe -	0.09	-	Ftg.		80	q	
<del>1</del>		Pn	0.27	Pf		3.0	Tot.			Q 2334	<u>B</u>
q <sub>9</sub> = 1250	3.83 0.08	Pt Pv	3.83 0.28	Pt _ Pe	0.01	5.8 12.5	Lgth. <sub>-</sub> Ftg.	2E = 8.6 Del V. = 3.0	150	q 2442	14-N90
19-1200	3.75	Pn -	0.23	Pf -	0.01	18.3	Tot.	G.V. = 0.9	100	Q 4756	9
		Pt _	4.34	Pt _			Lgth.			q _	
-		Pv – Pn –		Pe _ Pf			Ftg. Tot.			Q 4756	10
		Pt		Pt			Lgth.			q	
]		Pv _		Pe _			Ftg.		[	ā —	
+		Pn Pt		Pf Pt			Tot. Lgth.				
1		Pv -		Pe -			Ftg.			q	
1		Pn -		Pf			Tot.			Q	
-		Pt Pv		Pt _ Pe			Lgth. <sub>-</sub> Ftg.			q	
-		Pn -		Pf -			Tot.			Q	
		Pt _		Pt _			Lgth.			q	
-		Pv - Pn -		Pe _ Pf			Ftg. Tot.			a ——	
		Pt		Pt			Lgth.			q	
1		Pv <sup>-</sup>		Pe			Ftg.				
		Pn -		Pf			Tot.			Q	
-		Pt Pv		Pt _ Pe			Lgth Ftg.			q	
1		Pn		Pf			Tot.		l	Q	

FIGURE B.2(g) Metric. Calculation of system shown in Figure B.2(a) with velocity pressure included. Nozzle constant =  $K_{\rm m}$  = 129.6.

	Normal Pressure (bar)	Pressure Summary (bar)	Friction Loss (bar/m)	Equiv. Pipe Length (m)	Pipe Fittings & Devices (m)	Pipe Size (mm)	Flow in L/min	Nozzle Ident. & Location
L 15	Pt	Pt		Lgth	E=0.6	25	q 152	1-N9O
$K_3 = \frac{15}{\sqrt{1.6}}$	Pv Pn	Pe Pf	0.11	Ftg. 2.1 Tot. 2.3	T=1,5	25	Q 152	1)
	Pt	Pt 1.62		Lgth.			q	
	Pv Pn	Pe		Ftg Tot.			a —	
	Pt	Pt		Lgth.			q	
1	Pv	Pe		Ftg.				<u> </u>
	Pn Pt	Pf 170		Tot.			Q	<b>②</b>
1	Pt	Pt <u>1.38</u> Pe –	0.11	Lgth. <u>0.9</u> Ftg. –		25	9 <u>152</u>	1-N90
	Pn	Pf 0.10	0.11	Tot. 0.9		20	Q 152	4>
	Pt 1.48 Pv 0.14	Pt	0.10	Lgth. <u>0.5</u>	T=1.8	32	9 150	3-N90
-	Pv <u>0.14</u> Pn <u>1.34</u>	Pe Pf	0.10	Ftg. 1.8 Tot. 2.3			Q 302	(B)
- 6	Pt	Pt 1.71		Lgth. 0.3	T=3.0		9 302	2-N90
K <sub>6</sub> = 4	Pv	Pe 0.03	0.05	Ftg. 3.0		50	Q 604	©
,	Pn Pt	Pf 0.17 Pt 1.91		Tot. 3.3 Lgth.				
	Pv	Pe		Ftg.			q	
	Pn	Pf		Tot.			Q	
-	Pt Pv	Pt Pe		Lgth Ftg.			۹	ower Pipe Level
1	Pn —	Pf		Tot.			Q	3
v 2	Pt	Pt 2.93		Lgth 1.5	T=4.6	20	q	14-N90
$K_g = \frac{2}{\sqrt{3}}$	Pv Pn	Pe <u>0.55</u> Pf <u>3.48</u>	0.09	Ftg. 4.6 Tot. 6.1		80	Q 2334	9
	Pt	Pt S.440		Lgth.			q	
1	Pv	Pe		Ftg.			· —	
	Pn Pt	Pf		Tot.			Q	
-	Pt ———	Pt Pe		Lgth Ftg.			q	
	Pn	Pf		Tot.			Q	
	Pt	Pt		Lgth.			q	
-	Pv	Pe Pf		Ftg Tot.			a	
	Pt	Pt		Lgth.			q	
	Pv	Pe		Ftg.			Q	
	Pn Pt	Pf Pt		Tot. Lgth.				
1	Pv	Pe		Ftg.			q	
1	Pn	Pf		Tot.			Q	
-	Pt Pv	Pt Pe		Lgth Ftg.			q	
1	Pn —	Pf		Tot.			a	
	Pt	Pt		Lgth.			q	
-	Pv	Pe		Ftg			Q	
l	Pn	Pf Pt		101.			~	

FIGURE B.2(h) Metric. Calculation of system shown in Figure B.2(a) with velocity pressure included. Nozzle constant =  $K_{\rm m}$  = 129.6.

## HYDRAULIC CALCULATIONS

For _	System Shown on Fig. B.2(a)	Sheet No.	1
	All Nozzles Type N-30	Ву	J.E.C.
	(Nozzle Discharge Constant 3.0)	Date	12 - 3 - 6
		Job No	1572

Nozzle Ident. & Location	Flow in gpm	Pipe Size (in.)	Pipe Fittings & Devices (ft)	P	juiv. ipe jth (ft)	Friction Loss (psi/ft)	Pressure Summary (psi)	Normal Pressure (psi)	Nozzie Elev.	
1-N30	q 13.4		1E = 2.0	Lgth.	0.5		Pt20.1	Pt	20.0'	
1	Q 13.4	1		Ftg. Tot.	2.0 2.5	0.06	Pe Pf	Pv		9,:
	q –		2E = 4.0	Lgth.	6.0		Pt 20.3	Pt		$\vdash$
_	l . ——	1		Ftg.	4.0	0.06	Pe	Pv		]
2	Q 13.4		# 7.0	Tot.	10.0		Pf 0.6	Ph		<u> </u>
1-N30	q <u>13.5</u>	417	1E = 3.0	Lgth Ftg.	6.0 3.0	0.06	Pt <u>20.9</u> Pe -	Pt		93
3	Q 26.9	11/4		Tot.	9.0	0.00	Pf 0.5	Ph		For
1-N90	q 19.6	414	1T = 8.0	Lgth.	2.0		Pt 21.4	Pt		
(4)	Q 40.5	11/2		Ftg. Tot.	8.0 10.0	0.06	Pe Pf	Pv		94
3-N30	q 40.5		1E = 5.0	Lgth.	5.0		Pt 22.0	Pt		
5	· —	2		Ftg.	5.0	0.06	Pe 0.4	Pv		]
				Tot. Lgth.	10.0 4.0		Pf 0.6 Pt 23.0	Ph Pt	19.0'	-
4-N30	q <u>56.1</u>	21/2		Ftg.	-	0.07	Pe -	Pv	10.0	q <sub>6</sub> For
6	Q 137.1	2,2		Tot.	4.0	0.07	Pf 0.3	Ph		For
4-N30	q 56.5	_	1E = 7.0	Lgth.	5.0		Pt23.3	Pt		
7	Q 193.6	3		Ftg. Tot.	7.0 12.0	0.05	Pe Pf	Pv Ph		97
	q –			Lgth.	10.0		Pt 23.9	Pt		$\vdash$
(a)	H . ——	3		Ftg.	-	0.05	Pe 4.3	Pv		1
8	Q 193.6		25 24 2	Tot.	10.0		Pf 0.5	Ph Pt	9.0'	-
14-N30	9 <u>211.0</u>	6	2E = 28.0 Del V. = 10.0	Lgth Ftg.	19.0 41.0	0.007	Pt <u>28.7</u> Pe 4.1	Pv	9,0	q <sub>9</sub>
9	Q 404.6		G.V. = 3.0	Tot.	60.0	0.007	Pf 0.4	Ph		For
	q –			Lgth.			Pt33.3 /	Pt	0.5'	
10	Q 404.6	1/		Ftg. Tot.		-	Pe	Pv		$\{$
	q			Lgth.			Pt	Pt		Not
	\[ \]	+		Ftg.			Pe	Pv		
				Tot. Lgth.			Pf Pt	Ph Pt		
	q 250	1		Ftg.		1	Pe	Pv		hosi
	Q			Tot.			Pf	Ph		1
	q			Lgth.			Pt	Pt		
	a	1		Ftg Tot.		-	Pe	Pv		ł
	q			Lgth.			Pt	Pt		
	· —	1		Ftg.		]	Pe	Pv		]
	Q	_		Tot.			Pf Pt	Ph Pt		<del>                                     </del>
	۹	1		Lgth Ftg.		-	Pt Pe	Pv ———		1
	Q			Tot.			Pf	Ph		1
	q			Lgth.			Pt	Pt		
	Q 654.6	1		Ftg. Tot.		-	Pe	Pv Ph		1

FIGURE B.2(i)	English. Calculation of system shown in Figure B.2(a) with velocity
	pressure not included.

## HYDRAULIC CALCULATIONS

For	System Shown on Fig. B.2(a)	Sheet No	2
	All Nozzles Type N-30	Bv	J.E.C
	(Nozzle Discharge Constant 3.0)	Date	12 - 3 -
		Job No	1572

Nozzle Ident. & Location	Flow in gpm	Pipe Size (in.)	Pipe Fittings & Devices (ft)	Equiv. Pipe Length (ft)	Friction Loss (psi/ft)	Pressure Summary (psi)	Normal Pressure (psi)	Nozzle Elev.	
1-N30	q 13.4		1E=2.0	Lgth0.5		Pt <u>20.1</u>	Pt		_
1	Q 13.4	1	1T=5.0	Ftg. 7.0 Tot. 7.5	0.06	Pe Pf	Pv		K <sub>3</sub>
				Lgth.		Pf 0.5 Pt 20.6	Pt		$\vdash$
	9			Ftg.		Pe	Pv —		
	Q			Tot.		Pf	Ph		
	q			Lgth.		Pt	Pt		
(2)	Q			Ftg. Tot.		Pe	Pv		
1-N3O	q 13.4			Lgth. 3.0		Pt 20.1	Pt		
		1		Ftg. –	0.06	Pe	Pv		
(A)	Q 13.4			Tot. 3.0		Pf 0.2	Ph		$\vdash$
1-N30	9 <u>13.5</u>	414.	T=6.0	Lgth. <u>1.5</u> Ftg. 6.0	0.06	Pt <u>20.3</u> Pe	Pt		
(B)	Q 26.9	11/4		Tot. 7.5	0.00	Pf 0.5	Ph		
2-N30	q 26.9		T=10.0	Lgth. 1.0		Pt 20.8	Pt		$\vdash$
		2		Ftg. 10.0	0.03	Pe 0.4	Pv		l K <sub>e</sub>
	Q 53.8	_		Tot. 11.0		Pf 0.3	Ph		
	q			Lgth.		Pt21.5	Pt		
	a			Ftg Tot.		Pe Pf	Ph		
Lower Pipe Level	q			Lgth.		Pt	Pt		$\vdash$
				Ftg.		Pe	Pv		
3	Q			Tot.		Pf	Ph		
14-N30	q	_	T=15.0	Lgth. 5.0	2.05	Pt 23.3	Pt		l K
	Q 193.6	3		Ftg. 15.0 Tot. 20.0	0.05	Pe Pf 1.0	Pv		, r
	q			Lgth.		Pt 24.3	Pt		$\vdash$
	· ——			Ftg.		Pe	Pv		
	Q			Tot.		Pf	Ph		
	q			Lgth.		Pt	Pt		
	a —			Ftg Tot.		Pe Pf	Pv		
				Lgth.		Pt	Pt		$\vdash$
	q			Ftg.		Pe	Pv		
	Q			Tot.		Pf	Ph		
	q			Lgth.		Pt	Pt		
	a —			Ftg. Tot.		Pe Pf	Pv		
				Lgth.		Pt	Pt		<del></del>
	q			Ftg.		Pe ———	Pv —		
	Q			Tot.		Pf	Ph		
	q			Lgth.		Pt	Pt		
	Q		<u> </u>	Ftg. Tot.		Pe	Pv		
				Lgth.		Pt	Pt		$\vdash$
	٩			Ftg.		Pe ———	Pv		
	Q			Tot.	1	Pf	Ph		

Note: The flow from nozzles may be obtained from discharge curves rather than individual calculations at the preference of Similarly, flow characteristics of lines or sections of systems may be obtained by plotting results on charts made up to n<sup>1.85</sup> of by calculating constants (K – values)

FIGURE B.2(j)	English. Calculation of system shown in Figure B.2(a) with velocity
	pressure not included.

	Normal Pressure (bar)	essure mmary (bar)	Sur	Friction Loss (bar/m)	uiv. ipe ngth m)	Pi Ler	Pipe Fittings & Devices (m)	Pipe Size (mm)	Flow in L/min	Nozzle Ident. & Location
/	Pt	1.39	Pt _		0.2	Lgth.	1E = 0.6		9 <i>50.7</i>	1-N30
q <sub>1</sub> = 43.2√	Pv Pn	0.01	Pe _ Pf	0.014	0.6 0.8	Ftg Tot.		25	Q 50.7	(1)
	Pt	1.40	Pt		1.8	Lgth.	2E = 1.2		g _	
	Pv	-	Pe _	0.014	1.2	Ftg.		25	l · ——	
	Pn	0.04	Pf		3.0	Tot.			Q 50.7	2
q3 = 42.57	Pt Pv	1.44	Pt _ Pe	0.014	1.8 0.9	Lgth Ftg.	1E = 0.9	70	q 51.1	1-N30
For K <sub>3</sub> Calc,	Pn —	0.04	Pf -	0.014	2.7	Tot.		32	Q 101.8	(3)
$q_4 = 42.5\sqrt{1}.$ $q_6 = 168\sqrt{1}.$ For $K_6$ Calc,	Pt	1.48	Pt		0.6	Lgth.	17 = 2.4		q 51.5	1-N30
	Pv	-	Pe _	0.014	2.4	Ftg.		40	Q 153.3	
	Pn	0.04	Pf -		3.0	Tot.	4F 46			4
	Pt Pv	1.52 0.03	Pt _ Pe	0.014	1.5 1.5	Lgth Ftg.	1E = 1.5		9 153.3	3-N30
	Pn —	0.04	Pf -	0.014	3.0	Tot.		50	Q 306.6	⑤
	Pt	1.59	Pt _		1.2	Lgth.			q 212.3	4-N30
	Pv	-	Pe_	0.016	-	Ftg.		65	Q 518.9	6
	Pn Pt	0.02 1.61	Pf Pt		1.2 1.5	Tot. Lgth.	1E = 2.1			
$q_7 = 168\sqrt{1.6}$ $q_9 = 566\sqrt{1}.$ For $K_9$ Calc,	Pv —	- 1.01	Pe -	0.011	2.1	Ftg.	1E = 2.1	80	q 213.9	4-N30
	Pn	0.04	Pf -	0.011	3.6	Tot.			Q 732.8	7
	Pt	1.65	Pt _		3.0	Lgth.		80	q –	
	Pv Pn	0.30	Pe_	0.011		Ftg			Q 732.8	(B)
	Pt	0.03 1.98	Pf Pt		3.0	Tot. Lgth.				
		0.28	Pe -	0.002		Ftg.		150	9 <u>798.6</u>	14-N30
	Pn	0.03	Pf	0.00		Tot.		100	Q 1531.4	9
	Pt	2.29	Pt _		5.8	Lgth.	2E = 8.6		q _	
	Pv Pn		Pe _ Pf		12.5 18.3	Ftg Tot.	Del. V = 3.0 GV = 0.9		Q 1531.4	10
Note: See Fig supply inform	Pt		Pt		10.0	Lgth.	07 = 0.0		q	
	Pv		Pe			Ftg.			l  ———	
эарру то	Pn		Pf			Tot.			Q	10
	Pt Pv		Pt _ Pe _			Lgth Ftg			q	
	Pn —		Pf -			Tot.			Q	
	Pt		Pt			Lgth.			q	
	Pv		Pe _			Ftg.			. —	
	Pn		Pf			Tot.			Q	
	Pt Pv		Pt _ Pe			Lgth Ftg.			q	
	Pn —		Pf -			Tot.			Q	
	Pt		Pt _			Lgth.			q	
	Pv		Pe_			Ftg.			[ -	
	Pn		Pf			Tot.				
	Pt		Pt _ Pe			Lgth Ftg.			۹	
	Pn —		Pf -			Tot.			Q	
			Pt							

FIGURE B.2(k) Metric. Calculation of system shown in Figure B.2(a) with velocity pressure not included.  $K_{\rm m}=43.2$ .

	Normal Pressure (bar)	Pressure Summary (bar)	Friction Loss (bar/m)	Equiv. Pipe Length (m)	Pipe Fittings & Devices (m)	Pipe Size (mm)	Flow in L/min	Nozzle Ident. & Location
. 5	Pt	Pt <u>1.39</u>		Lgth	1E=0.6		9 50.7	1-N30
$K_3 = \frac{50}{\sqrt{1.4}}$	Pv Pn	Pe Pf	0.014	Ftg. 2.1 Tot. 2.3	1T=1.5	25	Q 50.7	⟨ĵ⟩
	Pt	Pf 0.03 Pt 1.42		Tot. 2.3 Lgth				
	Pv —	Pe 7.42		Ftg.		- 1	q	
	Pn	Pf		Tot.			Q	
	Pt	Pt		Lgth			q	
	Pv	Pe		Ftg			a —	<b>②</b>
	Pn	Pf		Tot.				·
	Pt Pv	Pt <u>1.39</u> Pe –	0.014	Lgth Ftg		25	9 50.7	1-N30
	Pn —	Pf 0.01	0.014	Tot. 0.9		20	Q 50.7	$\otimes$
	Pt	Pt 1.40		Lgth. 0.5	1T=1.8			1-N30
	Pv	Pe –	0.014	Ftg. 1.8	11-110	32		
	Pn	Pf 0.03	0.014	Tot. 2.13			Q 101.8	₿
<sub>ν</sub> 2	Pt	Pt <u>1.43</u>		Lgth	1T=3.0		q 101.8	2-N30
$K_{\Theta} = \frac{2O}{\sqrt{1}}$	Pv	Pe 0.02	0.007	Ftg. 3.0		50	Q 203.6	0
	Pn Pt	Pf 0.02 Pt 1.47		Tot. 3.3				0
	Pv —	Pt <u>1.47</u> Pe		Lgth Ftg.		-	q	
	Pn —	Pf		Tot.			Q	
	Pt	Pt		Lgth.			q	wer Pipe Level
	Pv	Pe		Ftg.				
	Pn	Pf		Tot.			Q	3>
$K_g = \frac{732}{\sqrt{1.6}}$	Pt	Pt1.61		Lgth	1T=4.6		q	14-N30
	Pv Pn	Pe Pf	0.011	Ftg. <u>4.6</u> Tot. 6.1		80	Q 732.8	
	Pt	Pt 1.68		Lgth.				
	Pv —	Pe 7.00		Ftg.			q	
	Pn	Pf		Tot.			Q	
	Pt	Pt		Lgth.			q	
	Pv	Pe		Ftg.			<u>a</u> —	
	Pn	Pf		Tot.				
	Pt	Pt		Lgth Ftg		-	q	
	Pn —	Pf		Tot.			Q	
	Pt	Pt		Lgth.			q	
	Pv	Pe		Ftg.				
	Pn	Pf		Tot.			Q	
	Pt	Pt		Lgth.			q	
	Pv Pn	Pe		Ftg Tot.			a T	
	Pt	Pt		Lgth.				
	Pv	Pe		Ftg.		ŀ	q	
	Pn —	Pf		Tot.			Q	
	Pt	Pt		Lgth.			q	
	Pv	Pe		Ftg.				
	Pn	Pf Pt		Tot.			Q	

# FIGURE B.2(1) Metric. Calculation of system shown in Figure B.2(a) with velocity pressure not included. Nozzle constant = $K_{\rm m}$ = 43.2.

## HYDRAULIC CALCULATION WORKSHEET

For all nozzles shown, k = 5.56; each nozzle covers 100.8 ft<sup>2</sup> at 0.25 gpm/ft<sup>2</sup> = 25.2 gpm minimum

25.2 25.2 25.2 25.2 26.1 25.2	1 1	Ftg. Tot. Lgth Ftg. Tot.	2.0 12.5 1	0.200	Pt 20.5 Pe +0.2 Pf 2.5 Pt 23.2 Pe Pf	Pt Pv Pn Pt Pv Pn	C = 120 Pt = (25.2/5.56) <sup>2</sup> = 20.5 psi at A
25.2 25.2 26.1 25.2 11		Lgth Ftg. Tot.  Lgth Ftg. Tot. Tot.	i. <u>0.5</u> 5.0		Pt <u>23.2</u> Pe Pf	Pt Pv	
25.2 25.2 26.1 26.1 25.2 11		Lgth Ftg. Tot.	5.0				1
26.1 9 25.2 <sub>1</sub> 1		Lgth	5.5	0.200	Pt 20.5 Pe +0.2 Pf 1.1	Pt Pv Pn	K = 25.2√21.7 = 5.41
25.2		Ftg. Tot.	١.		Pt21.7 Pe Pf	Pt Pv Pn	-
51.3	/2		12.0 19.0	0.092	Pt 23.2 Pe - Pf 1.7	Pt O.4 Pn	q <sub>2</sub> = 5.41/√23.2 P <sub>V</sub> < 5% of Pt, no
51.3 102.6	/2	Lgth Ftg. Tot.		0.333	Pt 24.9 Pe - Pf 3.3	Pt Pv Pn	-
ā —		Lgth Ftg. Tot.			Pt <u>28.2</u> Pe Pf	Pt Pv Pn	at C
Q 103.0 11	/2	Lgth Ftg. Tot.	22.0	0.335	Pt 28.5 Pe -6.5 Pf 7.4	Pt Pv Pn	-
50.6 153.6	//2	Lgth Ftg. Tot.	1.0 - 1.0	0.702	Pt 29.4 Pe -0.4 Pf 0.7	Pt 29.4 Pv 3.9 Pn 25.5	q = 50.5(25.5/25) $P_V$ into "D" from the
2 -		Lgth Ftg. Tot.			Pt <u>29.7</u> Pe <u>Pf</u>	Pt Pv Pn	-
185.7 102.6 288.3			12.0	2.250	Pt 43.4 Pe -1.7 Pf 67.5	Pt 43.4 Pv 15.2 Pn 28.2	q from D = 153.6( = 185.7 (
496.9 785.2		E Lgth Ftg. Tot.		0.165	Pt 109.2 Pe +5.2 Pf 5.8	Pt ~2.9 Pn	q = 381.6(109.2/64 P <sub>V</sub> < 5% of Pt, no c
2		Lgth Ftg. Tot.			Pt 120.2 Pe Pf	Pt Pv Pn	at G
2 —		Lgth Ftg. Tot.	-		Pt Pe Pf	Pt Pv Pn	-
ā —		Lgth Ftg. Tot.			Pt Pe Pf	Pt Pv Pn	-
2		Ftg.			Pt Pe Pf	Pt Pv Pn	
편 <u> </u>	103.0 50.6 153.6 185.7 102.6 288.3 496.9 785.2	103.0 50.6 153.6 185.7 102.6 288.3 11/2 1	103.0   Tot.   Lgth   Ftg.   Tot.   Lgth   Lgth   Tot.   Lgth   Lgth	Tot.   22.0   1.	Tot.   22.0   1.	Tot.   22.0   Pf   7.4   7.4   7.4   7.4   7.4   7.4   7.4   7.4   7.4   7.4   7.4   7.4   7.4   7.4   7.4   7.4   7.4   7.5	Tot.   22.0   Pf   7.4   Pn

FIGURE B.2(m)	English. Calculation of system shown in Figure B.2(l) with velocity pressure included.

## HYDRAULIC CALCULATION WORKSHEET

For all nozzles shown, k = 5.56; each nozzle covers 100.8 ft<sup>2</sup> at 0.25 gpm/ft<sup>2</sup> = 25.2 gpm minimum

	Normal Pressure (psi)	Pressure Summary (psi)	Friction Loss (psi/ft)	Equiv. Pipe Length (ft)	Pipe Fittings & Devices (ft)	Pipe Size (in.)	Flow in gpm	Nozzle Ident. & Location
C = 120 Pt = (25.2/ = 20.5 p	Pt Pv Pn	Pt 20.5 Pe +0.2 Pf 2.5	0.200	Lgth. 10.5 Ftg. 2.0 Tot. 12.5	1E	1	q Q 25.2	1
at A	Pt Pv Pn	Pt 23.2 Pe		Lgth Ftg Tot.			а	
K = 25.2/√2 = 5.41	Pt Pv Pn	Pt 20.5 Pe +0.2 Pf 1.1	0.200	Lgth. 0.5 Ftg. 5.0 Tot. 5.5	1T	1	q Q 25.2	2
	Pt Pv Pn	Pt 21.7 Pe Pf		Lgth Ftg Tot.			σ Q	
a <sub>2</sub> = 5.41/√	Pt Pv Pn	Pt 23.2 Pe – Pf 1.7	0.092	Lgth. 7.0 Ftg. 12.0 Tot. 19.0	1E 1T	11/2	26.1 <b>q</b> 25.2 <b>Q</b> 51.3	A
	Pt Pv Pn	Pt <u>24.9</u> Pe <u>-</u> Pf 3.3	0.333	Lgth. 2.0 Ftg. 8.0 Tot. 10.0	1T	11/2	9 <u>51.3</u> Q 102.6	В
at C	Pt Pv Pn	Pt <u>28.2</u> Pe Pf		Lgth Ftg Tot.			q	
	Pt Pv Pn	Pt 28.5 Pe -6.5 Pf 7.4	0.335	Lgth. 22.0 Ftg. 22.0		11/2	q Q 103.0	E
q = 50.5(29 = 54.3	Pt Pv Pn	Pt 29.4 Pe -0.4 Pf 0.7	0.734	Lgth. 1.0 Ftg. – Tot. 1.0		11/2	q <u>54.3</u> Q 157.3	D
q from B = 1 = 1	Pt Pv Pn	Pt 29.7 Pe -1.7 Pf 56.8	1.893	Lgth. 18.0 Ftg. 12.0 Tot. 30.0	1T 1E	11/2	q <u>105.3</u> Q 262.6	С
q = 381.6(84 = 437.9	Pt Pv Pn	Pt 84.8 Pe +5.2 Pf 4.7	0.134	Lgth. 25.0 Ftg. 10.0 Tot. 35.0	1E	4	q <u>437.9</u> Q 700.5	F
at G	Pt Pv Pn	Pt <u>94.7</u> Pe Pf		Lgth Ftg Tot.			q Q	
	Pt Pv Pn	Pt Pe Pf		Lgth Ftg Tot.			q	
	Pt Pv Pn Pt	Pt Pe Pf		Lgth Ftg Tot.			q Q	
	Pv Pn	Pt Pe Pf		Lgth Ftg Tot.			q Q	
	Pt Pv Pn	Pt Pe Pf Pt		Lgth Ftg Tot.			q Q	

## FIGURE B.2(n) English. Calculation of system shown in Figure B.2(l) with velocity pressure not included.

#### **Annex C Informational References**

#### C.1 Referenced Publications.

The following documents or portions thereof are referenced within this standard for informational purposes only and are thus not part of the requirements of this document unless also listed in Chapter 2.

**C.1.1 NFPA Publications.** National Fire Protection Association, 1 Batterymarch Park, P.O. Box 9101, Quincy, MA 02269-9101.

NFPA 13, Standard for the Installation of Sprinkler Systems, 1999 edition.

NFPA 14, Standard for the Installation of Standpipe, Private Hydrant, and Hose Systems, 2000 edition.

NFPA 24, Standard for the Installation of Private Fire Service Mains and Their Appurtenances, 1995 edition.

NFPA 30, Flammable and Combustible Liquids Code, 1996 edition.

NFPA 68, Guide for Venting of Deflagrations, 1994 edition.

NFPA 69, Standard on Explosion Prevention Systems, 1992 edition.

NFPA 80A, Recommended Practice for Protection of Buildings from Exterior Fire Exposures, 1996 edition.

NFPA 251, Standard Methods of Tests of Fire Endurance of Building Construction and Materials, 1995 edition.

NFPA 750, Standard on Water Mist Fire Protection Systems, 2000 edition.

NFPA 1964, Standard for Spray Nozzles (Shutoff and Tip), 1998 edition.

Fire Protection Guide to Hazardous Materials, 1997 edition.

"Venting of Tanks Exposed to Fire," NFPA Quarterly, October 1943.

#### **C.1.2 Other Publications.**

**C.1.2.1 ANSI Publication.** American National Standards Institute, Inc., 11 West 42nd Street, New York, NY 10036.

ANSI/ASME B1.20.1, Pipe Threads, General Purpose, 1983.

**C.1.2.2 ASME Publication.** American Society of Mechanical Engineers, Three Park Avenue, New York, NY 10016-5990.

ASME *Boiler and Pressure Vessel Code*, Section IX, Qualification Standard for Welding and Brazing Procedures, Welders, Brazers and Welding and Brazing Operators, 1985 edition.

ASME B.1.20.1, Pipe Threads, General Purpose, 1983.

**C.1.2.3 ASTM Publications.** American Society for Testing and Materials, 100 Barr Harbor Drive, West Conshohocken, PA 19420-2959.

ASTM A 135, Standard Specification for Electric-Resistance-Welded Steel Pipe, 1993.

ASTM E 380, Standard Practice for Use of the International System of Units (SI), 1993.

C.1.2.4 National Technical Information Service. 5285 Port Royal Road, Springfield, VA 22161.

U.S. Department of Defense standard DOD 6055.9-STD, *Ammunition and Explosives Safety Standards*.

#### C.1.2.5 Other Publications.

C.1.2.5.1 Department of the Army, Ammunition and Explosives Safety Standards, Headquarters Department of the Army, Washington D.C. Pamphlet 385-64, 28 November 1997.

C.1.2.5.2 Sprinkler Hydraulics And What It's All About, Harold S. Wass, Jr., Society of Fire Protection Engineers, April 2000.

**C.1.2.5.3** Rubber Reserve Company Memorandum 123, *Protection of Vessels Exposed to Fire.* 

#### C.2 Informational References.

The following documents or portions thereof are listed here as informational resources only. They are not a part of the requirements of this document.

Engineering Criteria for Water Mist Fire Suppression Systems, J. R. Mawhinney, P.E., presented at the Water Mist Fire Suppression Workshop at NIST, March 1–2, 1993.

Requirements for Relief of Overpressure in Vessels Exposed to Fire, J. J. Duggan, C. H. Gilmour, P. F. Fisher.

Rubber Reserve Company Memorandum 89, Heat Input to Vessels, November 19, 1944.

Transactions of the ASME, January 1944, 1–53. Requirements for relief of pressure in vessels exposed to fire & venting of tanks exposed to fire; heat input to vessels.

## **Formal Interpretation**

## NFPA 15

## Water Spray Fixed Systems for Fire Protection

#### 2001 Edition

Reference: 4-3.3.3.1

F.I. 79-1

Question: Is it the intent of 4-3.3.3.1 that 0.25 gpm per square foot (10.2 (L/min)/m<sup>2</sup>) be the rate of water application for each level of spray nozzles of a belt conveyor system requiring three levels of nozzles?

Answer: The 0.25 gpm per square foot [10.2 (L/min)/m<sup>2</sup>] is required for the top and bottom belt area, the structural parts and idler-rolls supporting the belt. This is independent of the size, number or levels of spray nozzles required for the installation.

Issue Edition: 1979 Reference: 4-4.3.5(b) Date: April 1982

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